

MANUFACTURER'S DATA BOOK

KBR	
ACCEPTANCE FOR ENGINEERING USE	
THIS DOCUMENT IS:	
ACCEPTED	(Code 1) _____
ACCEPTED WITH COMMENTS	(Code 2) _____
NOT ACCEPTED	(Code 3) _____
NOT REVIEWED	(Code 4) <u> X </u>
ACCEPTANCE DOES NOT RELIEVE SUPPLIER FROM FURNISHING MATERIAL IN CONFORMANCE WITH ORDER. REFER TO SDR-1 FOR FULL DEFINITION OF ACCEPTANCE CONDITIONS.	
DISCIPLINE	EXCH BY MW
	DATE <u>26JUL12</u>

MISSISSIPPI POWER

DEKALB, MISSISSIPPI

KEMPER COUNTY 1 – IGCC PROJECT

P.O. NO: 17496-0001

REQ. NO: MC202

ITEM NO: HX1027

PROCESS CONDENSATE TRIM HEATER

1 – 20" x 216" NEU EXCHANGER

ENERGY JOB NO: X-7930 A



Energy Exchanger Company

Energy Industrial Park
1844 North Garnett Road/Tulsa, OK 74116-1612
(918) 437-3000/FAX (918) 437-7144

Southern Company Generation Kemper County
MM187157 0 Unit 1

ENERGY EXCHANGER COMPANY PO: MPC17496-0001
X7930-A-MDB Rev: 0
IGCC - GASIFIER - MULTIPAGE - SHELL AND TUBE HEAT EXCHANGER - MAN

Mississippi Power
Kemper County 1 – IGCC Project
P.O. No: 17496-0001
Req. No: MC202
Item No: HX1027
Energy Job No: X-7930 A

MANUFACTURER'S DATA BOOK

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SECTION 1

**I.Q.S. Work Order 556
Inspection Shipping Release Notice 08-BB**

Client: SOUTHERN CO. Purchase Order #: MPC-17645; MPC17496 & MPC- 17497

EWO: MPC9117.T61401 Supplier: ENERGY EXCHANGERS

Shop Order # SO # 7930 A/B Location: TULSA, OK

Project: KEMPER COUNTY IGCC UNIT Supplier Ref. #:

Item #	Description	Qty Ordered	Qty Released	Balance
	21-216-NEU exchangers Tag # HX1027/HX2027--SO# 7930 A/B	2	2	0
	THE UNITS & FINAL DOCUMENTATION ARE COMPLETE			

This (is not) a complete shipping release.

This does not relieve the Vendor of any responsibility to ensure that the material or equipment meets all contractual requirements. This notice is issued according to IQS' best knowledge, experience, codes and specifications available to us during this inspection. Neither IQS nor any member of its inspection force is to be held liable for the acceptance of or payment for released items, or the default or negligence on the part of the vendors' obligation to supply quality equipment and materials or breach the conditions of his contract with the purchaser. Actual acceptance of equipment/material is predicated on the purchaser's site inspection, operational integrity and the fulfillment of all contractual warranties connected thereto.

Date: 6/29/12

Bill Bronaugh
IQS

SECTION 2

REV L N #

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Energy Exchanger Company



HEAT EXCHANGER SPECIFICATION SHEET

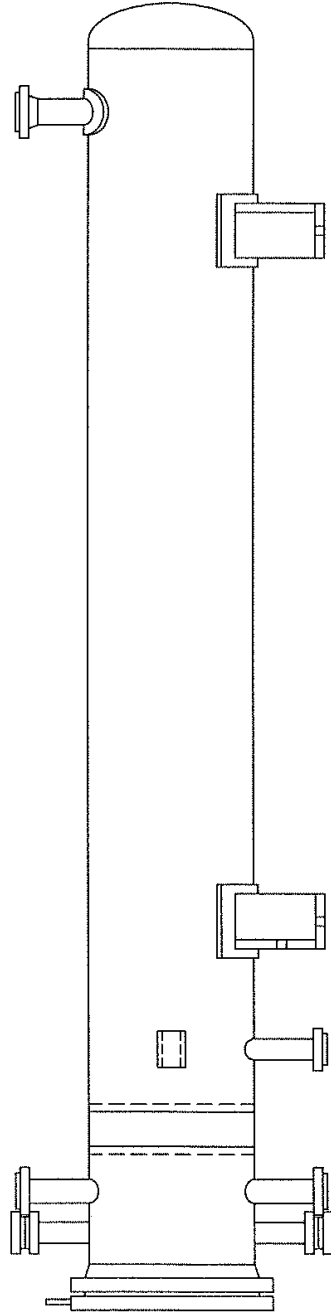
P.O. No.: 17496-0001

REV. 0 AS PURCHASED

Customer	SOUTHERN COMPANY SERVICES		Job No.:	X-7930 "AS BUILT"	
Address	BIRMINGHAM, AL		Rev.:	2	Date: 5/31/2012
Plant Location	KEMPER COUNTY, MS		File:	10-7309	
Service of Unit	PROCESS CONDENSATE TRIM HEATER		Item:	HX1027/2027	
Size	20-216	Type	NEU	Horizontal	Connected In 1 Parallel 1 Series
Surf./Unit	Gross ☒ Eff ☐	959.77 ft ²	Shells/Unit 1	Surf./Shell ☐ Gross ☒ Eff ☐	959.77 ft ²
PERFORMANCE OF ONE UNIT					
Fluid Allocation	Shell Side		Tube Side		
Fluid Name	LP STEAM		CONDENSATE		
Fluid Quantity, Total	lb/hr	5528 X 1.1	108315 X 1.1		
Vapor (In/Out)			29 X 1.1 (2)		
Liquid			108315 X 1.1		
Steam		5528 X 1.1	108286 X 1.1		
Water		5528 X 1.1			
Noncondensable					
Temperature (In/Out)	°F	281.		215.1	261.
Density (Vapor/Liquid)	Lb/Ft ³			60.44	2.6
Viscosity	cP			0.29	0.0200
Molecular Weight					0.22
Molecular Weight, Noncondensable					
Specific Heat	Btu/lb-F			0.9510	0.2940
Thermal Conductivity	Btu/hr-ft-F			0.3050	0.0250
Latent Heat	Btu/lb				0.2590
Inlet Pressure	psia	40.		628.5	
Velocity	ft/sec	21.13		4.72	
Pressure Drop, Allow./Calc.	psi	2.00 /	0.20	7.00 /	7.00
Fouling Resistance (Min.)	Hr-Ft ² -°F/Btu	0.0005		0.001	
Heat Exchanged	5204000 X 1.1		Btu/hr; M.T.D. (Corrected)	20.12 °F	
Transfer Rate, Service	296.43		Btu/hr-ft ² -F; Clean	776.67	Btu/hr-ft ² -F
CONSTRUCTION OF ONE SHELL			Sketch (Bundle/Nozzle Orientation)		
Design/Test Pressure	psig	85/FV/280	Tube Side	790 / 1030 (6)	
Design Temperature (Max/Min)	°F	350/10		285/10	
No. Passes Per Shell		1		4	
Corrosion Allowance	inch	0.125		0.125	
Connections	In	1 - 6" 150RF	Out	1 - 4" 600RF	
Size & Rating	Intermediate	1 - 2" 150RF		1 - 4" 600RF	
Tube No.	133 U'S	OD 0.75 In; Thk. ☒ Min	Avg 0.083 In; Length 18. ft; Pitch 1 in 30°		
Tube Type	BARE		Material SA-179		
Shell	SA-106B	☒ ID ☐ OD 21.25	In ; Shell Cover SA-516-70	☒ Integ. ☐ Remov.	
Channel or Bonnet	SA-516-70N (PWHT)		Channel Cover SA-266-2or4N	☐ Integ. ☒ Remov.	
Tubesheet-Stationary	SA-266-2or4N		Tubesheet - Floating		
Floating Head Cover			Impingement Protection	DEFLECTOR BEYOND BENDS (SA-36)	
Baffles-Cross	14 - SA-36	Type V D-SEG	% Cut (☒ Dia ☐ Area)	25. Spacing c/c 15.0	Inlet in
Baffles-Long			Seal Type		
Supports - Tube		U-Bend	Type		
Bypass Seal Arrangement			Tube-Tubesheet Joint	FULL STRENGTH WELD PER UW-20 (5)	
Expansion Joint			Type		
pv ² - Inlet Nozzle		Bundle Entrance	Bundle Exit		
Gaskets - Shell Side			Tube Side	321 SS GMGC	
- Floating Head					
Code Requirements	ASME SECTION VIII, DIV. 1 (STAMP: YES)		TEMA Class	R	
Weight/Shell	8250	Filled With Water	11500	Bundle	---

REMARKS

- 1) THERE ARE TWO TRAINS AND EACH TRAIN HAS ONE EXCHANGER (HX1027 & HX2027). FLOW RATE AND DUTY ARE FOR ONE TRAIN.
- 2) FLASHING IS DUE TO DISSOLVED GAS.
- 3) BAFFLE AT U-BEND IS FULL CIRCLE BAFFLE WITH WINDOW CUT-OUT AT CENTER (WxH = 7.125" x 5.5")
- 4) APPLY NACE FOR WET H2S SERVICE ON TUBE SIDE.
- 5) PER FIG UW-20.1 (c) or (d).
- 6) TUBESIDE IS SUBJECT TO STEAM OUT OF 15 PSIG @ 250°F (BOTH BELOW THE DESIGN PRES./TEMP)

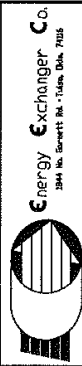


▲ COATING DATA SHEET - SYSTEM 6 APPLIES.
 ABRASIVE BLAST PER SSPC-SP10 WITH AN ANCHOR PROFILE OF 2 TO 3 MILS.
 FIRST COAT WITH CARBOLINE THERMALINE 450 NOVOLAC (4.0-5.0 MILS DFT)
 SECOND COAT WITH CARBOLINE THERMALINE 450 NOVOLAC (4.0-5.0 MILS DFT)
 (8-10 MILS TOTAL DFT) (COLOR: MFR STD GREY)

CERTIFIED AS-BUILT

CUSTOMER: MISSISSIPPI POWER
 / SOUTHERN COMPANY SERVICES
 P.D. NO: 17496-0001 REQ NO: MC202
 SERVICE: PROCESS CONDENSATE TRIM HEATER
 ITEM NO: HX1027/2027

NOTES:		PAINT MAP	
1. A DAILY INSPECTION REPORT SHALL BE MAINTAINED.		DOWN BY: DMORRISON	
2. PAINT SPECIFICATION V42-ITS AND APPLICABLE COATING DATA SHEET SHALL BE FURNISHED TO THE PAINTER.		DATE: 3-11-11	
1. DATA SHEET SHALL BE FURNISHED TO THE PAINTER.		CKD. BY: SM	
REVISED PER CUSTOMER MD/SG		DWG. NO: X-7930-AA	
NO. DATE		REV 1	



Energy Exchange Co.
 384 N. BENTLEY BL. - 11th. Bldg. 7005



QTY SHOWN FOR ONE
TWO REQ'D- UNITS "A" & "B"

SUPPORT DETAILS



Energy Exchanger Co.
1844 No. Cornett Rd. • Tulsa, Okla. 74116

NOTE:
SEE DWG. X-7930-R
FOR JOB NOTES.

DWG. NO.

X-7930-D

CKD. BY

SM

MD/SG

ER COSI

REVISION

REVISED	
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NO.	DATE
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FOR JOB NOT

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-7930-R

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SEE DWG.

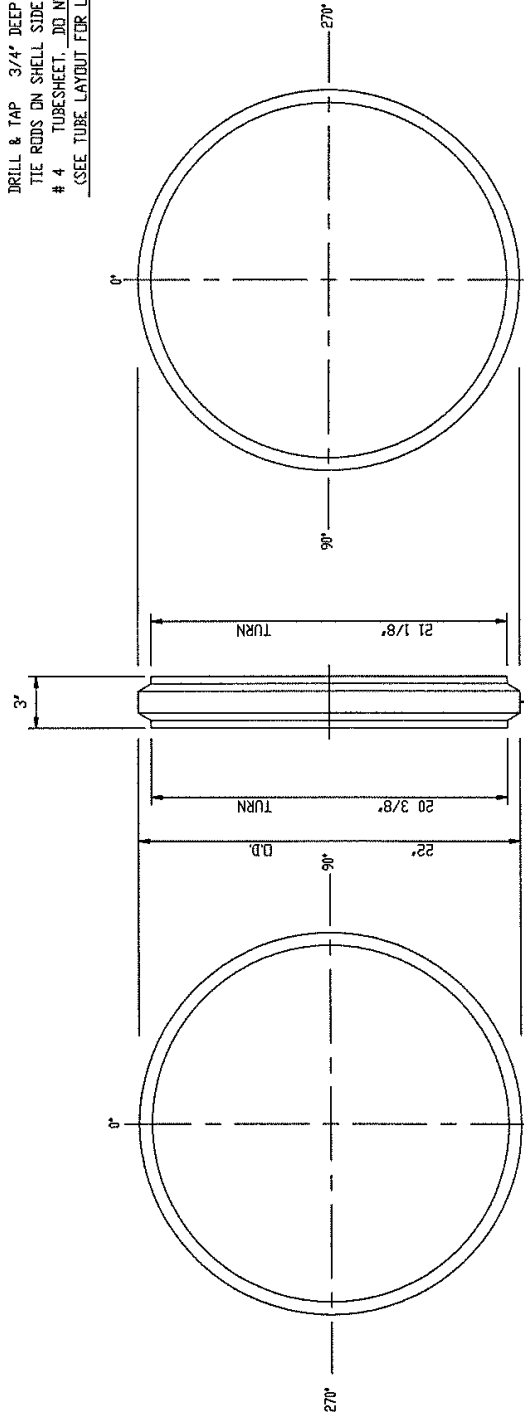
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MM187157

DRILL & TAP 3/4" DEEP FOR
TIE RODS ON SHELL SIDE OF
4 TUBESHEET. DO NOT DRILL THRU!!
(SEE TUBE LAYOUT FOR LOCATIONS.)

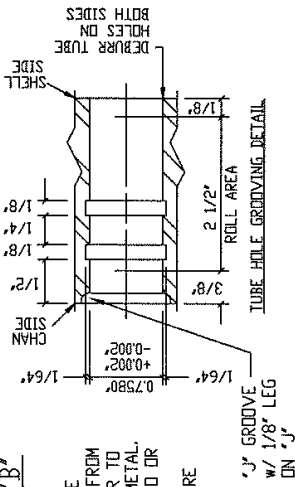


NOTES:

- 1) MACHINE ALL SURFACES TO 250 Ra EXCEPT GASKET FACE TO BE 125 Ra.
- 2) REAM & RING-GROOVE TUBE HOLES BEFORE POST-WELD HEAT TREAT.
- 3) FOR JOB NOTES SEE DWG. X-7930-R

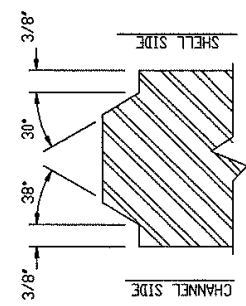


SHELL SIDE



QTY SHOWN FOR ONE
TWO REQ'D- UNITS "A" & "B"

STRENGTH WELD TUBE TO TUBESHEET. REMOVE OIL AND GREASE OR OTHER FOREIGN MATTER FROM TUBESHEET, TUBEHOLES AND TUBE ENDS PRIOR TO WELDING OF TUBES. HELI-ARC WITH FILLER METAL. WELD EACH TUBE INDIVIDUALLY WITH (2) TWO OR MORE PASSES. WELD PROCEDURE = SW-1. DYE CHECK TUBE TO TUBESHEET WELDS BEFORE AND AFTER TUBE ROLLING. PREHEAT TO 200 deg F. PRIOR TO WELDING. FINAL TUBE ROLLING AFTER HEAT TREAT. BUBBLE TEST AT 15 PSIG. PRIOR TO ROLLING



CUSTOMER: MISSISSIPPI POWER
/ SOUTHERN COMPANY SERVICES
P.O. NO: 17496-0001 REQ NO: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER
ITEM NO: HX1027/2027

TUBESHEET DETAILS



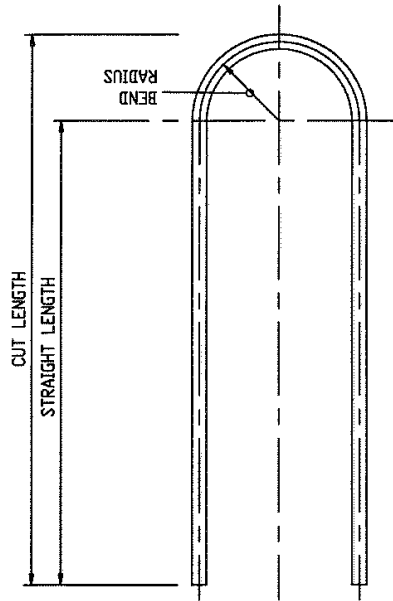
DWN. BY	D.MORRISON
DATE	3-11-11
CKD. BY	SM
REV	1
DWG. NO.	X-7930-F

CERTIFIED AS-BUILT

TUBESHEET DETAIL

NO.	DATE	REVISED NOTE	2/ECC	MD/SG	REVISIONS
1	8/18/11				

ROW	NO. OF TUBES	BEND RADIUS	BEND DIAMETER	BEND LENGTH	STRAIGHT LENGTH	CUT LENGTH	DEVELOPED LENGTH
A	16	1 1/8"	2 1/4"	0'-3 9/16"	18'-0"	18'-1 1/2"	36'-3 9/16"
B	14	2"	4"	0'-6 5/16"	18'-0"	18'-2 3/8"	36'-6 5/16"
C	16	2 7/8"	5 3/4"	0'-9 1/16"	18'-0"	18'-3 1/4"	36'-9 1/16"
D	15	3 3/4"	7 1/2"	0'-11 13/16"	18'-0"	18'-4 1/8"	36'-11 13/16"
E	16	4 5/8"	9 1/4"	1'-2 9/16"	18'-0"	18'-5"	37'-2 9/16"
F	14	5 1/2"	11"	1'-5 5/16"	18'-0"	18'-5 7/8"	37'-5 5/16"
G	14	6 3/8"	12 3/4"	1'-8 1/16"	18'-0"	18'-6 3/4"	37'-8 1/16"
H	12	7 3/16"	14 3/8"	1'-10 5/8"	18'-0"	18'-7 9/16"	37'-10 5/8"
J	10	8 1/16"	16 1/8"	2'-1 3/8"	18'-0"	18'-8 7/16"	38'-1 3/8"
K	6	8 15/16"	17 7/8"	2'-4 1/8"	18'-0"	18'-9 5/16"	38'-4 1/8"



TOTAL NO. REQUIRED: 133
 SIZE: 3/4" O.D. X 0.083" MIN
 MATERIAL: SA-179

MAXIMUM OUT-OF-ROUNDNESS OF TUBES AT
 U-BENDS NOT TO EXCEED 10%.
 MATERIAL HARDNESS SHALL NOT EXCEED 22 HRC
 STRESS RELIEVE U-BENDS PLUS 1'-0" STR. LEN.
 BY ELECTRIC RESISTANCE @ 1150°F ±25°F

QUANTITIES SHOWN ARE FOR
 ONE SET OF U-TUBES,
 2 -SET REQ'D. TOTAL.

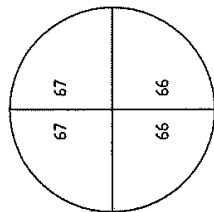
CUSTOMER: MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES
 P.O. NO. 17496-0001 REQ. NO. MC202
 SERVICE: PROCESS CONDENSATE TRIM HEATER
 ITEM NO. HX1027/2027

CERTIFIED AS-BUILT

TUBE BENDING SCHEDULE

DOWN. BY	DN	DATE	1-18-11
REV'D PER CUST.	DN/SG	NO.	2-16-11
REVISIONS	DATE	NO.	1
DWG. NO.	X-7930-G	REV	1





TUBE DISTRIBUTION

NOTES

- 1) DRILL AND REAM TUBE HOLES IN
TUBESHEETS TO 0.758" $\pm$ 0.002" DIA. 
FOR 133 - 3/4" O.D. U-TUBES.
TOTAL HOLES = 266
2) TUBE PITCH = 1' ROT. TRIANGLE. (30°) 
3) NUMBER OF PASSES = 4
4) SEE DRAWING X-7930-F
FOR TUBE GROOVING DETAILS.
5) BAFFLE O.D. = 21 1/16"
6) O.T.L. = 19 13/16"

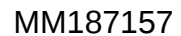
CERTIFIED AS-BUILT

CUSTOMER: MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES
P.O. NO: 17496-0001 REQ NO: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER
ITEM NO: HX1027/2027

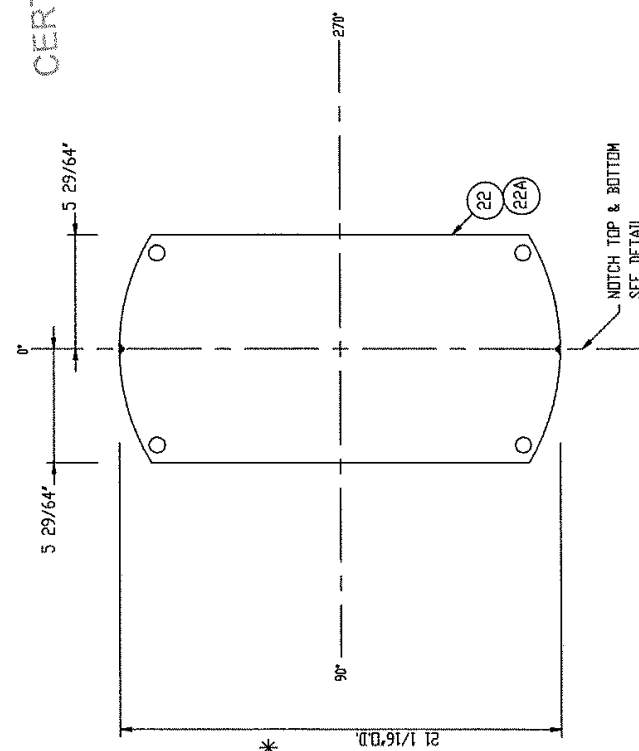
TUBE LAYOUT

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VIEW LOOKING AT SHELL SIDE OF NO. 4 TUBESHEET

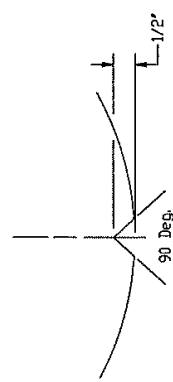


CERTIFIED AS-BUILT

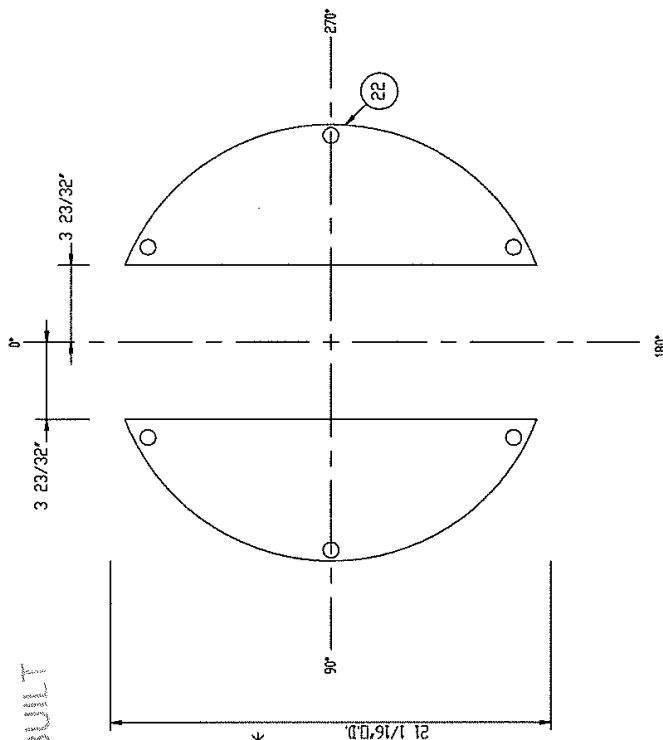


VIEW ZZ OF BAFFLES
6 - REQD. CUT A (1/4\"/>

NOTCH TOP & BOTTOM
SEE DETAIL



QTY SHOWN FOR ONE
TWO REQ'D- UNITS "A" & "B"



VIEW ZZ OF BAFFLES
6 - REQD. CUT B (1/4\"/>

CUSTOMER: MISSISSIPPI POWER
/ SOUTHERN COMPANY SERVICES
P.D. NO: 17496-0001 REQ NO: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER
ITEM NO: HX0027/2027

NOTES:

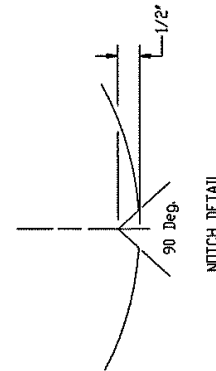
- 1) FOR JOB NOTES SEE DWG. X-7930-R
- 2) DRILL TUBE HOLES IN BAFFLES 25/32\"/>
- 3) DRILL TIE ROD HOLES 9/16\"/>
- 4) RADIUS ALL CORNERS ON BAFFLE CUTS.
- * 5) CHECK SHELL I.D. BEFORE MACHINING BAFFLE O.D.
- 6) MACHINE O.D. OF BAFFLES TO 250 Ra.
- 7) SEE TUBE LAYOUT (DWG. X-7930-H) FOR BAFFLE CUT LOCATIONS.

BAFFLE DETAILS			
	DWN. BY	D. MORRISON	
	DATE	3-11-11	
	CKD. BY	SM	
	REVISED PER CUSTOMER	MD/SG	
	DATE	5/12/11	
	NO.		
REVISIONS			
	DWG. NO.	X-7930-J1	REV 1



QTY SHOWN FOR ONE
TWO REQ'D- UNITS "A" & "B"

- 1) FOR JOB NOTES SEE DWG. X-7930-R
- 2) DRILL TUBE HOLES IN BAFFLES .25/32" DIA. & DEBURR.
- 3) DRILL TIE ROD HOLES 9/16" DIA.
SEE TUBE LAYOUT (DWG. X-7930-H) FOR LOCATION.
- 4) RADIUS ALL CORNERS ON BAFFLE CUTS.
- * 5) CHECK SHELL I.D. BEFORE MACHINING BAFFLE O.D.
- 6) MACHINE O.D. OF BAFFLES TO .250 R_o.
- 7) SEE TUBE LAYOUT (DWG. X-7930-H) FOR BAFFLE CUT LOC.



1 1/2" THK
1 -REQD

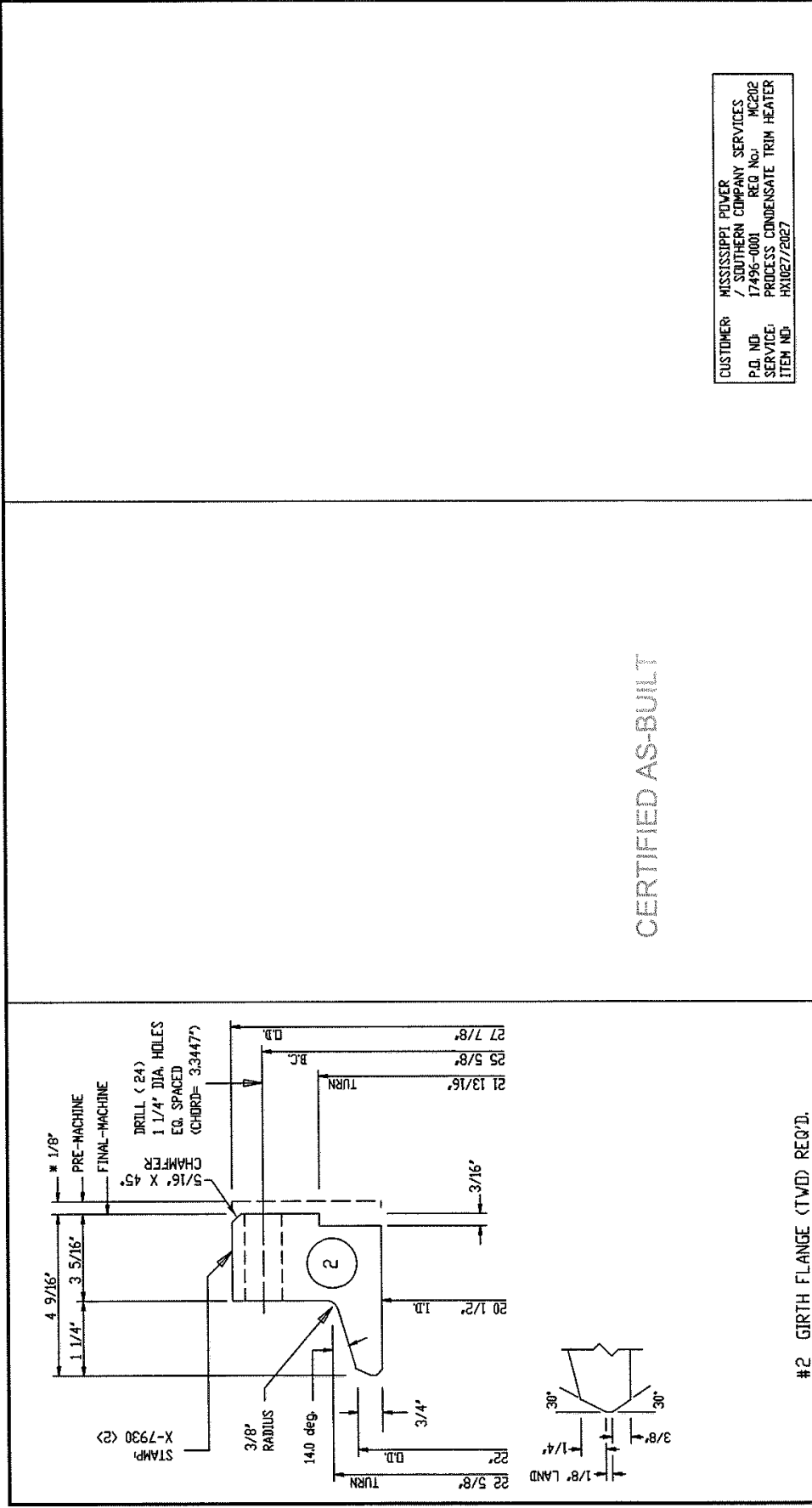
BAFFLE DETAILS

NO.	DATE	REVISED PER	CUSTOMER	MD/SG	VE/DA	DATE	DWN. BY
1	5/12/11					3-11-11	J. MORRISON
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Energy Exchanger Co.
1944 N. Garnett Rd. • Tulsa, Okla. 74126

X-7930-J2	REV 2
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#2 GIRTH FLANGE (TWD) REQ'D.

NOTES:

- 1) SEE DWG. X-7930-R FOR JOB NOTES.
- 2) MACHINE ALL SURFACES TO 250 Ra EXCEPT GASKET SURFACES MACHINE TO 125-250 Ra
- 3) * FINAL MACHINE FACING AFTER FINAL WELDING AND POST WELD HEAT TREATMENT.

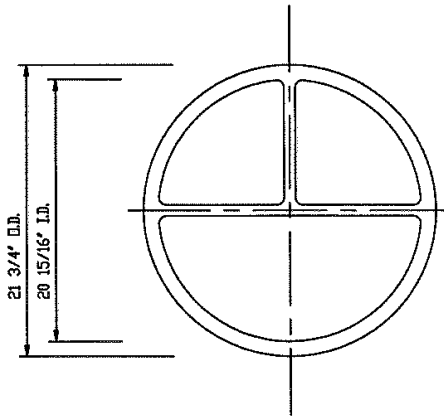
CUSTOMER: MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES
 P.O. NO: 17496-0001 REQ. NO: MC202
 SERVICE: PROCESS CONDENSATE TRIM HEATER
 ITEM NO: HX10272027

GIRTH FLANGES

DRWN. BY	D.MORRISON
DATE	3-11-11
CKD. BY	SM
DWG. NO.	X-7930-K
REV	0



NO.	DATE	REVISIONS



(1)-REQUIRED.
 CHANNEL COVER GASKET
 1/8" THK 321 STN STL GMGC
 RIB WIDTH TO BE 7/16" WIDE.

CERTIFIED AS-BUILT

NOTES:
 1) QUANTITIES SHOWN FOR ONE SET
 (4)-SETS REQUIRED TOTAL.
 ONE SET OF GASKETS TO BE USED IN EACH EXCH. AND
 (2) SETS TO BE BOXED, MARKED WITH
 P.D. & ITEM NO. & SHIPPED WITH EXCHANGER.
 2) ALL RADII TO BE 1/4"

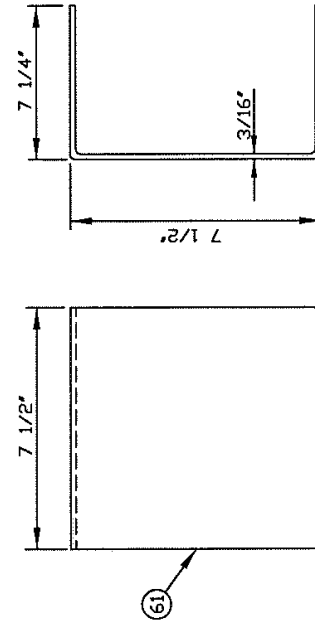
CUSTOMER:	MISSISSIPPI POWER
P.D. NO:	/ SOUTHERN COMPANY SERVICES
SERVICE:	17496-0001 REC NO: MC202
ITEM NO:	PROCESS CONDENSATE TRIM HEATER
	HX1027/2027

GASKET DETAILS	
DOWN BY	D.MORRISON
DATE	3-9-11
EXD BY	<i>DM</i>
DWG. NO.	X-7930-D
REV	0



SHOP TO ASSIGN AT COMPLETION OF FABRICATION

CERTIFIED BY		Energy Exchanger Company		TULSA, OKLAHOMA	
MAVP SHELL	215	P.S.I.	350	*F	280
MAVEP	15.0	P.S.I.	350	*F	
MAVP TUBE	792	P.S.I.	285	*F	1030
MAVEP	---	P.S.I.	---	*F	
MIN. DESIGN METAL TEMP.		SHELL	10	*F	215
		TUBE	10	*F	792
SERIAL NO.		1	YEAR BUILT		
P.O. NO.		17496-0001			
SERVICE		PROCESS CONDENSATE TRIM COOLER			
ITEM	2	SIZE	20-216	TYPE	NEU
DESIGN PRESSURE: SHELL=85 PSIJ TUBE=790 PSI					



NAME PLATE BRACKET DETAIL

TWO - REQ'D.

- 1 X-7930 A
X-7930 B

- 2 HX1027
HX2027

CLIP CORNERS & SEAL WELD TO NAME PLATE BRACKET

NAME PLATE DETAIL

TWO - REQ'D.

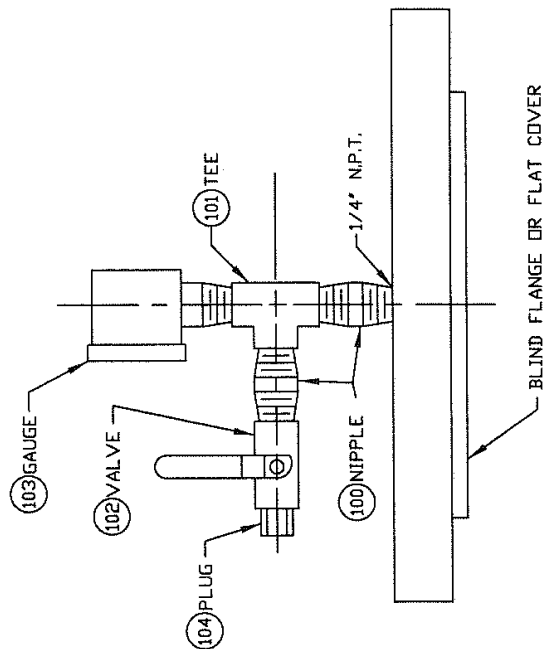
CERTIFIED AS-BUILT

CUSTOMER: MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES
P.O. NO: 17496-0001 REQ. NO: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER
ITEM NO: HX1027/2027

NAME PLATE DETAILS	
DWN. BY D.MORRISON	REV. 0
DATE 3-11-11	
CHKD. BY JMM	
DWG. NO. X-7930-Q	

BOTH SIDES SHALL BE THOROUGHLY DRAINED AND DRIED AFTER HYDROTEST. REMOVE MOISTURE BY BLOWING HOT AIR (150°F., MAXIMUM).

- 2) A) SEAL ALL EXTERNAL OPENINGS WITH A 1/8" THK. RUBBER-GASKETED BLIND FLANGE OR FLAT COVER.
- B) INSTALL A CONNECTION WITH A VALVE AND PRESSURE GAUGE.
- C) PRESSURE TO 15 PSIG AND DEPRESSURIZE TWICE, REPRESSURE TO 15 PSIG WITH DRY NITROGEN.
- 3) STENCIL BY EACH NOZZLE: 'CONTENTS UNDER N2 PRESSURE) DO NOT OPEN WITHOUT PURCHASER'S APPROVAL'.
- 4) TACKWELD A PIECE OF PIPE TO EACH COVER EQUIPPED WITH THE FITTING AND GAUGE ASSEMBLY, FOR PROTECTION DURING SHIPMENT.



ONLY ONE BLIND FLANGE OR COVER SHALL BE TAPPED FOR CHANNEL SIDE, AND ONE FOR SHELL SIDE.

PROVIDE 1/4" N.P.T. WITH PLUG ON BOTTOM COVERS FOR DRAINING PURPOSES.

2025 RELEASE UNDER E.O. 14176

CUSTOMER:	MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES
P.O. NO:	17496-0001
SERVICE:	PROCESS CONDENSATE TRIM HEATER
ITEM NO:	HX1027/2027

	NITROGEN PURGE DETAILS						
✓	DWN. BY	D MORRISON					
✓	DATE	6/25/12					
✓	CKD. BY	(n)					
✓	REV NO.	X-7930-X					
✓	REVISIONS	0					
✓	DATE						

BILL OF MATERIAL

PART NO	TWO REQ'D, DESCRIPTION OF ONE	MATERIAL SPEC.	QTY ONE	TOT QTY	REV	NOTE	PO NO	PROMISED
21	TUBES 3/4" O.D.X 0.083" THK (MIN) PER BEND SCHEDULE	SA-179	133	266	1			*
FORGED RING MATERIAL								
2	FLG 27 7/8" O.D.X 20 1/2" I.D.X 4 9/16" THK	SA-266-2or4N	1	2	1			*
TUBESHEETS & COVERS								
4	TUBESHEET 22" O.D.X 3" THK	SA-266-2or4N	1	2	1			*
1	COVER 27 7/8" O.D.X 3 1/4" THK	SA-266-2or4N	1	2	1			*
BAFFLES								
22	BAFFLES 21 1/16" O.D.X 1/4" THK	SA-36	12	24				*
22A	FIRST & LAST BAFFLES 21 1/16" O.D.X 1/2" THK	SA-36	2	4				*
HEADS								
18	ELLIP HD. 22" O.D.X 5/16" THK(min) W/2" SF	SA-516-70	1	2				*
CYLINDERS								
12	R&W CYL 20 1/2" I.D.X 3/4" THK X 1'-7 7/16" LG.	SA-516-70N	1	2	1			*
	(67" WRAP) X 3/4" THK X 19 11/16" LG.							
15	SHLS PIPE 22" O.D.X(0.3750" SchSTD)X 19'-9 1/16" LG.	SA-106B	1	2				*

MATERIAL MAY NOT ORIGINATE FROM CHINA OR NORTH KOREA
 1) BASE MATERIAL HARDNESS SHALL NOT EXCEED 22 HRC
 2) SA-105N BASE HARDNESS SHALL NOT EXCEED 187 HB

* DENOTES PRELIMINARY ORDER

CERTIFIED AS-BUILT



REQ No.
SERVICE

MC202

PROCESS CONDENSATE TRIM HEATER



Energy Exchanger Co.
 1844 No. Garnett Rd. • Tulsa, Okla. 74116

CUST: MISSISSIPPI POWER CO. c/o SOUTHERN COMPANY SERVICES

P.O. 17496-0001

ITEM: HX1027/2027

NO.	DATE	DESCRIPTION	PB/M	DR: DM	CK: MD	DATE: 1/18/11	DWG. NO.	REV
			PB/M	DR: DM	CK: <i>sm</i>	DATE: 3-11-11	X-7930-1BM	0

[illegible]

BILL OF MATERIAL

PART NO	TWO REQ'D, DESCRIPTION OF ONE	MATERIAL SPEC.	QTY ONE	TOT QTY	REV	NOTE	PO NO	PROMISED
BOLTING & GASKETS								
40	LOT OF GASKETS PER DWG X-7930-D		2	4				
41	1 1/8" ROUND X 8-THREAD STUDS X 9 1/8" LG. 1&2	SA-193B7	24	48				
42	1 1/8" HEAVY HEX NUTS 8-THREAD	SA-194-2H	48	96				
43	5/8" ROUND X 11-THREAD STUDS X 4 3/8" LG. (2'-600# RF)	SA-193B7	16	32				
44	5/8" HEAVY HEX NUTS 11-THREAD (2'-600# RF)	SA-194-2H	32	64				
45	GASKET 0.175" THK 321 STN STL SP. WD FLEXIBLE GRAPHITE FILLED W/ 1/8" THK C'ST OUTER COMPRESSION RING FOR (2'-600# RF)		2	4				
MISC. MATERIAL								
60	STD. NAME PLATE	STN.STL.	1	2				
61	STD. NAME PLATE BRK'T.	SA-516-70	1	2				
62	LIFTING LUGS 3 1/2" X 1/2" THK X 6 7/8" LG	SA-516-70	1	2				
23	FT. 1/2" O.D. TIE RODS	C'STL	107	214				
23A	FT. 3/4" O.D. SPACER TUBING	SA-214	107	214				
23B	1/2" TIE ROD HEX NUTS	C'STL	12	24				
63	DEFLECTOR PLATE 7 1/8" X 3/8" THK X 19 3/4" LG	SA-516-70	1	2	2			
50	PASS PLATES 9 15/16" X 3/8" THK X 24" LG.	SA-516-70N	1	2				
51	PASS PLATES 20 3/8" X 3/8" THK X 24" LG.	SA-516-70N	1	2				
NITROGEN PURGE MATERIAL								
100	1/4" PIPE NIPPLE X 2" LG. (THRD. OUTSIDE EACH END)	C. STL.	4	8	3			
101	1/4" STRAIGHT TEE (THRD. INSIDE EACH END)	C. STL.	2	4	3			
102	1/4" PIPE VALVE (INSIDE THRD.) (#5X713)	BRASS	2	4	3			
103	1/4" PRESSURE GAUGE (#5X939)(P570K-60LM)(0-60 PSIG)		2	4	3			
104	1/4" PIPE PLUG	C. STL.	2	4	3			
SUPPORT MATERIAL								
120	PLATE 10" X 3/8" THK X 26 1/2" LG.	SA-516-70	2	4				
121	PLATE 19" X 1/2" THK X 13" LG.	SA-516-70	2	4				
122	PLATE 6" X 1/2" THK X 19" LG.	SA-516-70	2	4				
123	PLATE 5 1/2" X 1/2" THK X 13" LG.	SA-516-70	4	8				
125	5/8" DIA X 11 THD HEX HD BOLT X 2" LG	C'STL	1	2				

* DENOTES PRELIMINARY ORDER

CERTIFIED AS-BUILT

REQ No: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER

△			Energy Exchanger Co. 1844 No. Garnett Rd. • Tulsa, Okla. 74116		
△					
△					
△					
△	6/25/12	ADD NITROGEN PURGE PER CUST DM/100	CUST: MISSISSIPPI POWER CO. c/o SOUTHERN COMPANY SERVICES		
△	5/31/12	CORRECT P/N 63 THK. / EEC MD/SG	P.O. 17496-0001		ITEM: HX1027/2027
△	5/12/11	REV. PER CUSTOMER MD/SG	PB/M	DR: ----	CK: ----
NO.	DATE	DESCRIPTION	FB/M	DR: DM	CK: SM
			DATE: 3-11-11	DWG. NO. X-7930-3BM	
				REV 3	

X-7930 PACKING LIST

LINE NO	SPARE PARTS LIST	MATERIAL SPEC.	QTY ONE	TOT QTY	REV	NOTE	PO NO	PROMISED
SP1	SPARE GASKETS PER DWG. X-7930-D		1 SET(S)	2 SET(S)				
SP2								
SP3								
SP4								
SP5								
SP6								
SP7								
SP8								
SP9								
SP10								

SPARE PARTS TO BE BOXED & TAGGED WITH P.O. NO., ITEM NO., SHIPPING WT. & "SPARE GASKETS AND PARTS"

LINE NO	STACKING MATERIAL	MATERIAL SPEC.	QTY ONE	TOT QTY	REV	NOTE	PO NO	PROMISED
S1								
S2								
S3								
S4								
S5								
S6								
S7								
S8								
S9								
S10								
S11								
S12								
S13								
S14								
S15								
S16								
S17								
S18								
S19								
S20								
S21								
S22								
S23								
S24								
S25								

* DENOTES PRELIMINARY ORDER

DO NOT ORDER
FROM PACKING LIST

CERTIFIED AS-BUILT

REQ No: MC202
SERVICE: PROCESS CONDENSATE TRIM HEATER

△			 Energy Exchanger Co. 1844 No. Garnett Rd. • Tulsa, Okla. 74116					
△								
△								
△								
△								
△								
CUST: MISSISSIPPI POWER / SOUTHERN COMPANY SERVICES								
P.O. 17496-0001			ITEM: HX1027/2027					
PB/M	DR: ----	CK: ----	DATE: ----	DWG. NO.	REV			
NO.	DATE	DESCRIPTION	FB/M	DR: DM	CK: <i>SM</i>	DATE: 3/14/11	X-7930-PL	0

Energy Exchanger Company



CERTIFIED AS-BUILT
Miles D. Small 5/31/12

DATE: 1/18/2011

PAGE: 1 OF 25



MECHANICAL CALCULATIONS

CUSTOMER: MISSISSIPPI POWER c/o SOUTHERN COMPANY SERVICES

DESTINATION: KEMPER COUNTY, MISSISSIPPI

P.O. No.: 17496-0001



ITEM No.: HX1027/2027

E.E.C. SERIAL No.: X-7930 A/B

SERVICE: PROCESS CONDENSATE TRIM HEATER

REQ No.: MC202



DESIGN DATA		
	SHELL SIDE	TUBE SIDE
DESIGN PRESSURE	85 PSIG / FV	790 PSIG
DESIGN TEMP.	350°F	285°F
M.D.M.T.	10 °F	10 °F
CORR. ALLOW.	1/8"	1/8"
NO. PASSES	ONE	FOUR
M.A.W.P. (H&C)	215 PSIG	792 PSIG
LIMITED BY	150# FLANGE RATING	CHANNEL COVER

NOTE: ALL LOADING CONDITIONS REFERENCED IN
 PARA. UG-22 HAVE BEEN ADDRESSED

- DESIGNED TO ASME SEC VIII, DIV 1, 2007 ED, '09 AD.
- MATERIAL ARE IMPACT TEST EXEMPT PER UG-20(f)

REVISION LOG

DATE	PAGE	REV.	DESCRIPTION
2/16/2011	AS NOTED	1	PER CUSTOMER COMMENTS
4/7/2011	25	2	REV'D ANCHOR BOLT DIAM PER CUSTOMER
6/23/2011	AS NOTED	3	ADDED FV FOR STEAM OUT TUBE SIDE PER CUST.

W.O. No.: X-7930

SHELL SIDE

```

=====
NOM.
SIZE      PRESS.      TEMP.      C.A.      RT      H.T.      TEMA
22.000"   85.0psig      350deg.F  0.1250"   SPOT      0deg.F    R
=====

```

ASME CODE SEC.VIII DIV.I UG-27

[CYLINDER]

=====DESIGN CONDITIONS=====CYLINDER CALCULATIONS ON O.D. FORMULA=====

SHELL CYL

MATERIAL: SA-106B PRESS = 85.0psig TEMP = 350deg.F

O.D. NOM. THK. RW=0/PIPE=1 CORR.ALLOW EFFICIENCY

22.0000" 0.3750" 1 0.1250" 0.85

ATM.STRS DES.STRS STRS/STRS MAWP N-C MAWP CORR.

17100.0psi 17100.0psi 1.000 438.808psig 270.399psig

P*(RO)

----- = 0.06418" + CORR. ALLOW. = 0.18918" + MTOL. = 0.21620"

S*E+(.4*P)

ASME CODE SEC.VIII DIV.I UG-32

[ELLIPTICAL HEAD]

=====DESIGN CONDITIONS=====ELLIPTICAL HEAD CALCULATIONS ON O.D. FORMULA=====

SHELL HEAD

MATERIAL: SA-516-70 PRESS = 85.0psig TEMP = 350deg.F

O.D. (min)THK. CORR.ALLOW EFFICIENCY

22.0000" 0.3125" 0.1250" 0.85

ATM.STRS DES.STRS STRS/STRS MAWP N-C MAWP CORR.

20000.0psi 20000.0psi 1.000 495.627psig 294.287psig

P*(RO)

0.0000

----- = 0.05475" + CORR. ALLOW. = 0.17975" + MTOL. = 0.17975"

S*E+(.9*P)

----- External Pressure Calculations -----		Ellip. Head External pressure calculations:	
Ext Press Chart No.=	1	Ext Press Chart No.=	1
Ext Press Chart....=	CS-2	Ext Press Chart....=	CS-2
OD.....=	22.00000	OD.....=	22.00000
T.....=	0.20313	RO.....=	19.80000
L.....=	240.00000	T.....=	0.18750
Temp.....=	350.00000	Temp.....=	350.00000
Stress from MT.....=	20000.00000	Stress from MT.....=	20000.00000
Yield from MT.....=	33050.00000	Yield from MT.....=	33050.00000
2 x Stress.....=	40000.00000	A.....=	0.00118
B1 from Chart@Right=	0.00000	B.....=	12212.38477
Yield= 2 x B1 x 0.9=	0.00000	PA1.....=	115.64759
S.....=	0.00000	PA2.....=	207.31763
DO/T.....=	108.30502	PA.....=	115.64759
L/DO.....=	10.90909		
A.....=	0.00011		
B.....=	1481.60242		
PA1.....=	0.00000		
PA2.....=	0.00000		
PA.....=	18.23987		

Item No.: HX1027/2027

REV. 1

P.O. No.: 17496-0001

Job No.: X-7930

By: DN/MD

2/16/2011

Page: 2

FRONT CHAN.

```

=====
NOM.
SIZE      PRESS.      TEMP.      C.A.      RT      H.T.      TEMA
20.000"   790.0psig      285deg.F  0.1250"   SPOT    1150deg.F  R
=====
ASME CODE SEC.VIII DIV.I UG-27                      [ CYLINDER ]
=====DESIGN CONDITIONS=====CYLINDER CALCULATIONS ON I.D. FORMULA=====
CHAN. CYL
MATERIAL: SA-516-70N      PRESS = 790.0psig  TEMP = 285deg.F
I.D.      NOM. THK.      RW=0/PIPE=1  CORR.ALLOW  EFFICIENCY
20.5000"   0.7500"             0          0.1250"     0.85
ATM.STRS   DES.STRS   STRS/STRS   MAWP N-C   MAWP CORR.
20000.Cpsi 20000.0psi  1.000      1191.589psig  988.372psig

P* (R+CA)
----- = 0.49596" + CORR. ALLOW. = 0.62096" + MTOL. = 0.62096"
S*E- (.6*P)
*****

```

----- External Pressure Calculations -----

```

Ext Press Chart....= 1 CS-2
Actual Chart Used..= 1 CS-2
Material.....= SA-516-70
OD.....= 22.00000
T.....= 0.62500
L.....= 25.00000
Temp.....= 250.00000
Stress from MT....= 20000.00000
Yield from MT....= 34200.00000
2 x Stress.....= 40000.00000
B1 from Chart@Right= 0.00000
Yield= 2 x B1 x 0.9= 0.00000
S.....= 0.00000
DO/T.....= 35.20000
L/DO.....= 1.13636
A.....= 0.00578
B.....= 17235.64648
PA1.....= 0.00000
PA2.....= 0.00000
PA.....= 652.86536

```



Item No.: HX1027/2027
Job No.: X-7930

REV. 3
By: DN/MD 6/23/2011

P.O. No.: 17496-0001
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Energy Exchanger Co.

Mechanical Calculations

X-7930

NOZZLE REINFORCEMENT CALCULATIONS/ ASME SEC.VIII DIV.I UG-37 & UG-16

NOZ NO= S1 6.00" 150 LB RF WN

{INLET } SHELL SIDE

PRESSURE = 85.0psig TEMP = 350.0deg.F

```

-----CYLINDER-----NOZZLE-----
SA-106B                      SA-106B
OPER STRS= 17100.0 psi      OPER STRS= 17100.0 psi
ATM STRS = 17100.0 psi      ATM STRS = 17100.0 psi
C.A.      = 0.12500"        C.A.      = 0.12500"
I.D.      = 21.34375"       I.D.      = 5.76100"
O.D.      = 22.00000"       O.D.      = 6.62500"
THK.      = 0.32812"        THK.  XH= 0.43200"
T          = 0.20312"        TN       = 0.30700"
TR         = 0.05457"        TRN      = 0.01643"
ET         = 0.14856"        ETN      = 0.29057"

```

MIN STD. WT. PIPE+C.A.= 0.37000" TR+C.A.= 0.17957"

LIMITS= 12.02200"

fr1= 1.0000 fr2= 1.0000 fr3= 1.0000 fr4= 1.0000 F= 1.00000

Min weld sizes: NS= 0.0000 NP= 0.3039 PS= 0.1436 IF= 0.0000"

```

AREA REQD.          A = 0.32802in^2
EXCESS IN CYL.      A1= 0.89296in^2
EXCESS IN NOZ. (OUTSIDE) A2= 0.29511in^2 H = 0.50781"
AREA OF FILLETS     = 0.28125in^2
AREA AVAILABLE      = 1.46932in^2

```

NOZ. NECK WELD= 0.37500" AREA= 0.14062in^2

```

PAD MATL.= SA-516-70      S= 20000.psi
PAD O.D.= 9.62500"        THK.= 0.37500" AREA= 1.12500in^2
PAD TO CYL. WELD= 0.37500" AREA= 0.14062in^2
ARC= 6.729"
PAD RET. DIM.= 9.625" X 9.750"

```

< AREA REQD-AREA AVAILABLE > = -2.26630in^2

MAWP COR= 411.0psig LIMITED BY AR

All Weld Paths are stronger than the required strength / [UG-41 UG-45 UW-15]

EXTERNAL PRESSURE:

```

NOZTYP[ 0.0] X-7930          6.00"- 150# RF WN PRESS= -15 TEMP= 350
<<<<<< CYLINDER >>>>>> <<<<<< NOZZLE >>>>>>
      SA-106B                      SA-106B
OPER STRS=17100.0000 OPER STRS=17100.0000 Area reqd. A= 0.5654
ATM STRS =17100.0000 ATM STRS =17100.0000 Excess in cyl A1= 0.0902
C.A.      = 0.12500 C.A.      = 0.12500 Excess in noz A2= 0.2838 H= 0.5078
I.D.      = 21.34375 I.D.      = 5.76100 Excess in noz A3= 0.0000 H= 0.0000
O.D.      = 22.00000 O.D.      = 6.62500 Area fillets = 0.2812
THK.      = 0.32812 THK.  XH= 0.43200 Area avail. = 0.6552
T          = 0.20312 TN       = 0.30700 Noz neck weld = 0.3750 A= 0.1406
TR         = 0.18813 TRN      = 0.02760 Pad weld = 0.3750 A= 0.1406
ET         = 0.01500 ETN      = 0.27940 Internal weld = 0.0000 A= 0.0000
PIPE F=1.0000 E1=1.0000 SHELL TOL=0.8750 (Min USED) NOZ TOL=0.8750 (Nom USED)
MIN STD. WT. PIPE+C.A.=0.37000 TR[using abs(P)]+C.A.=0.13465 CHORD= 0.0000
LIMITS= 12.02200 fr1= 1.0000 fr2= 1.0000 fr3= 1.0000 fr4= 1.0000
Min weld sizes: NS= 0.0000 NP= 0.3039 PS= 0.1436 IF= 0.0000
PAD MATL.= SA-516-70 O.D.= 9.62500 THK.= 0.37500 AREA= 1.12500 S= 20000.
Area reqd-Area avail =<< -1.21477>>

```

Item No.: HX1027/2027

REV. 1

P.O. No.: 17496-0001

Job No.: X-7930

By: DN/MD

2/16/2011

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MM187157

Energy Exchanger Co.

Mechanical Calculations

X-7930

NOZZLE REINFORCEMENT CALCULATIONS/ ASME SEC.VIII DIV.I UG-37 & UG-16
 NOZ NO= T1 & T2 4.00" 600 LB RF LWN
 [INLET/OUTLET] FRONT CHANNEL SIDE
 PRESSURE = 790.0psig TEMP = 285.0deg.F
 OFFSET VERTICAL NOZZLE: OFFSET = 4.00000"

-----CYLINDER-----		-----NOZZLE-----	
SA-516-70N		SA-105N	
OPER STRS=	20000.0 psi	OPER STRS=	20000.0 psi
ATM STRS =	20000.0 psi	ATM STRS =	20000.0 psi
C.A. =	0.12500"	C.A. =	0.12500"
I.D. =	20.50000"	I.D. =	4.00000"
O.D. =	22.00000"	O.D. =	6.00000"
THK. =	0.75000"	THK. =	1.00000"
T =	0.62500"	TN =	0.87500"
TR =	0.41976"	TRN =	0.08598"
ET =	0.20524"	ETN =	0.78902"

MIN STD. WT. PIPE+C.A.= 0.33237" TR+C.A.= 0.54476"
 LIMITS= 8.50000"
 fr1= 1.0000 fr2= 1.0000 fr3= 0.0000 fr4= 0.0000 F= 1.00000
 Min weld sizes: NS= 0.3536" NP= 0.0000" PS= 0.0000" IF= 0.0000"

AREA REQD. A = 1.78398in²
 EXCESS IN CYL. A1= 0.87227in²
 EXCESS IN NOZ. (OUTSIDE) A2= 2.46570in² H = 1.56250"
 AREA OF FILLETS = 0.14062in²
 AREA AVAILABLE = 3.47859in²

NOZ. NECK WELD= 0.37500" AREA= 0.14062in²

< AREA REQD-AREA AVAILABLE > = -1.69461in²

MAWP COR= 1127.0psig LIMITED BY AR

External pressure for steam out:

NOZTYP[9.0] X-7930 4.00"- 600# RF LWN PRESS= -15 TEMP= 250 INLET
 <<<<<< CYLINDER >>>>>> <<<<<< NOZZLE >>>>>>
 SA-516-70N SA-105N
 OPER STRS=20000.0000 OPER STRS=20000.0000 Area reqd. A= 0.1592
 ATM STRS =20000.0000 ATM STRS =20000.0000 Excess in cyl A1= 2.3379
 C.A. = 0.12500 C.A. = 0.12500 Excess in noz A2= 2.6537 H= 1.5625
 I.D. = 20.50000 I.D. = 4.00000 Excess in noz A3= 0.0000 H= 0.0000
 O.D. = 22.00000 O.D. = 6.00000 Area fillets = 0.1406
 THK. = 0.75000 THK. = 1.00000 Area avail. = 5.1323
 T = 0.62500 TN = 0.87500 Noz neck weld = 0.3750 A= 0.1406
 TR = 0.07490 TRN = 0.02580 Pad weld = 0.0000 A= 0.0000
 ET = 0.55010 ETN = 0.84920 Internal weld = 0.0000 A= 0.0000
 LWN F=1.0000 E1=1.0000 SHELL TOL=0.8750 (Min USED) NOZ TOL=0.8750 (Nom USED)
 MIN STD. WT. PIPE+C.A.=0.33237 TR[using abs(P)]+C.A.=0.13278 CHORD= 4.6240
 LIMITS= 8.50000 fr1= 1.0000 fr2= 1.0000 fr3= 0.0000 fr4= 0.0000
 Min weld sizes: NS= 0.3536 NP= 0.0000 PS= 0.0000 IF= 0.0000
 Area reqd-Area avail =<< -4.97313>>



Item No.: HX1027/2027

REV. 3

P.O. No.: 17496-0001

Job No.: X-7930

By: DN/MD

6/23/2011

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MM187157

ASME SEC.VIII DIV.1 APPENDIX 2			Front Channel to cover flange		
DESIGN CONDITIONS			GASKET and BOLTING CALCULATIONS		TABLE
Design Pres=	790.0 psig		Eff.Gsk OD=	21.6875"	No.Passes= 4
Neg. Pres=	None		Eff.Gsk ID=	20.9375"	N= 0.375"
Design Temp=	285 deg.F		THK=	0.1250"	b= 0.188
Flg Matl=	SA-266-2or4N	Gsk Matl=SS GMGC			y= 10100psi
Bolt Matl=	SA-193B7	Gsk Face=FLAT FACE	w=	0.0000"	m= 4.250
Corr Allow=	0.1250"	Wm2=	194201 #	Am =	16.4378in^2
Flange Desn Sfo	20000.0 psi	Hp =	129115 #	Ab =	17.4720in^2
Atm. Sfa	20000.0 psi	H =	281828 #	W =	423872 #
Bolting Desn Sb	25000.0 psi	Wm1=	410944 #	Wm1=	410944 #
Atm. Sa	25000.0 psi	Gasket Width Check	Nmin =	0.3230"	
CONDITION	LOAD	x	LEVER ARM	=	MOMENT
	HD =	267148 #	hD=	1.96875"	MD= 525948 in#
Operating	HG =	129115 #	hG=	2.15625"	MG= 278405 in#
	HT =	14680 #	hT=	2.29688"	MT= 33718 in#
					Mo= 838072 in#
Gasket					
Seating	HG =	423872 #	hG=	2.15625"	mo= 913974 in#
Allow.Stress-STRESS CALCULATIONS-Operating			SHAPE CONSTANTS		
1.5 Sfo Long Hub,SH	23080.3 psi		K	= 1.3434	h/ho= 0.3471
Sfo Radial Flg,SR	4103.6 psi		T	= 1.7788	F = 0.8718
Sfo Tang Flg,ST	13546.1 psi		Z	= 3.4855	V = 0.3537
Sfo .5(SH+SR)or.5(SH+ST)	18313.2 psi		Y	= 6.7336	f = 1.0168
J(APP.2-14)=	0.6421		U	= 7.3996	e = 0.2421in^-1
Allow.Stress-STRESS CALCULATIONS-Gsk.Seating			gl/go=	1.5000	d = 29.428in^3
1.5 Sfa Long Hub,SH	25170.6 psi		ho	= 3.6012"	
Sfa Radial Flg,SR	4475.2 psi				
Sfa Tang Flg,ST	14772.9 psi		OTHER STRESS FORMULA FACTORS		
Sfa .5(SH+SR)or.5(SH+ST)	19971.7 psi		t	= 3.1250"	
J(APP.2-14)=	0.6757		Alpha	= 1.7565	
			Beta	= 2.0087	
			Gamma	= 0.9875	
			Delta	= 1.0370	
			Lambda	= 2.0245	
			M	= 40389 #	
			m	= 44046 #	
O.D.	= 27.8750"	THK.	= 3.3125"		
I.D.	= 20.5000"	T-Adder	= 0.0000"		
GO	= 0.7500"	G1	= 1.0625"		
HUB O.D.	= 22.6250"	HUB LEN	= 1.2500"		
HUB ANG	= 14.0363deg	RIB LENGTH	= 35.5938"		
G(MEAN)	= 21.3125"	G(CALC)	= 21.3125"		
G(MIN.)	= 21.1250"	G(MAX.)	= 23.5000"		
B.C.	= 25.6250"	B.S.C.F.	= 1.0000		
No. BOLTS	= 24	BOLT DIAMETER	= 1.1250"		
R	= 1.5000"	E	= 1.1250"		
BOLT SPAC	= 3.3447"	TORQUE	= 462ft#		
MIN. SPAC	= 2.5000"	TEMA MAX. SPAC	= 6.1974"		
FLG TURN	= 0.1875"	FACING	= RECESS		
BPRIME	= 0.0000"	BG1	= 0.0000"		
FLG RWT	= 362Lbs	FLG FWT	= 273Lbs		

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///// FRONT COVER CALCULATIONS /////

```

EXCHANGER TYPE...= N E U          MATERIAL.....= SA-266-2or4N
PRESSURE.....= 790.0 psig          CORROSION ALLOWANCE= 0.1250"
TURN LOW.....= 0.1875"             TURN HIGH.....= 0.2500"
S COVER STRESS...= 20000.0 psi      E.....= 1.0
Sb STRESS BOLTS...= 25000.0 psi     Ab.....= 17.4720 in^2
d.....= 21.3125"                   C.....= 0.3000
W.....= 423872 #                   Wml.....= 410944 #
hG (ASME).....= 2.1562"            hG (TEMA).....= 2.1562"
G (TEMA).....= 21.3125"            E (MOD.) x (10)-6...= 28.2 psi
COVER THK SET HOLD= [ NO]

```

[PER ASME SECT.VIII UG-34 USING Wml (OPERATING)]

$$THK = d - \sqrt{\frac{C P}{S E} + \frac{1.9 Wml hG}{S E d^3}} = 3.0549"$$

[PER ASME SECT.VIII UG-34 USING W (GASKET SEATING)]

$$THK = d - \sqrt{\frac{1.9 W hG}{S E d^3}} = 2.0184"$$

[PER TEMA RCB-9.2 FLAT CHANNEL COVER]

MAXIMUM DEFLECTION = 0.0300"
 DEFLECTION at 2.7262" THICK = 0.0300"

$$Y = \frac{G}{E (3.062)^3} \left[0.0435 G^3 P + 0.5 Sb Ab hG \right] = 0.0212"$$

```

[ COV THK Min ] TEMA Deflection      = 2.7262" + 0.1875" = 2.9137"
[ COV THK Min ] CODE Operating       = 3.0549" + 0.1875" = 3.2424"
[ COV THK Min ] CODE Gasket Seating  = 2.0184" + 0.1875" = 2.2059"
ACTUAL COVER THICKNESS USED (SET HOLD[ NO])= 3.2500"

```

MAIN FLG IS FLANGE MARK # 2
 COMP FLG IS FLANGE MARK # 0

/// INDIVIDUAL COMPONENTS ///

MAWP CORR. MAIN FLG = 792.0 Limited by: Flange stress.
 MAWP CORR. COVER = 792.0

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Input Echo, Tubesheet Number 1, Description: X-7930 TS

Shell Design Pressure	Ps	85.00	psig
Shell Thickness	ts	0.3750	in.
Shell Corrosion Allowance	cas	0.1250	in.
Inside Diameter of Shell	Ds	21.250	in.
Shell Temperature for Internal Pressure	Ts	350.00	F
Shell Material		SA-106 B	

*Note: Using 2 * Yield for Discontinuity Stress Allowable (UG-23(e)), Sps.
Make sure that material properties at this temperature are not
time-dependent for Material: SA-106 B*

Shell Material UNS Number		K03006	
Shell Allowable Stress at Temperature	Ss	17100.00	psi
Shell Allowable Stress at Ambient		17100.00	psi

Channel Type:		Cylinder	
Channel Design Pressure	Pt	790.00	psig
Channel Thickness	tc	0.7500	in.
Channel Corrosion Allowance	cac	0.1250	in.
Inside Diameter of Channel	Dc	20.500	in.
Channel Design Temperature	TEMPC	285.00	F
Channel Material		SA-516 70N	

*Note: Using 2 * Yield for Discontinuity Stress Allowable (UG-23(e)), Sps.
Make sure that material properties at this temperature are not
time-dependent for Material: SA-516 70*

Channel Material UNS Number		K02700	
Channel Allowable Stress at Temperature	Sc	20000.00	psi
Channel Allowable Stress at Ambient		20000.00	psi

Number of Tubes Holes	Nt	266	
Tube Wall Thickness	et	0.0830	in.
Tube Outside Diameter	D	0.7500	in.
Total Straight Tube Length	Lt	216.00	in.
Straight Tube Length (bet. inner tubsht faces) L		213.00	in.
Design Temperature of the Tubes		220.00	F
Tube Material		SA-179	
Tube Material UNS Number		K01200	
Is this a Welded Tube		No	
Tube Material Specification used	Smls. tube		
Tube Allowable Stress at Temperature		13400.00	psi
Tube Allowable Stress At Ambient		13400.00	psi
Tube Yield Stress At Operating Temperature	Syt	23640.00	psi
Tube Pitch (Center to Center Spacing)	P	1.0000	in.
Tube Layout Pattern		Triangular	

Fillet Weld Leg	af	0.1250	in.
Groove Weld Leg	ag	0.1250	in.
Tube-Tubesheet Joint Weld Type		Full Strength	
Method for Tube-Tubesheet Jt. Allow.		UW-20	
Tube-Tubesheet Joint Classification		d	

Radius to Outermost Tube Hole Center	ro	9.525	in.
Largest Center-to-Center Tube Distance	U1	1.5000	in.
Length of Expanded Portion of Tube	ltx	2.5000	in.
Tube-side pass partition groove depth	hg	0.0000	in.

Tubesheet TYPE: U-tube, Integral both sides, Conf. a

Tubesheet Design Metal Temperature	T	350.00	F
Tubesheet Material Specification		SA-266 2or4N	

*Note: Using 2 * Yield for Discontinuity Stress Allowable (UG-23(e)), Sps.
Make sure that material properties at this temperature are not
time-dependent for Material: SA-266 2or4N*

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Tubesheet Material UNS Number		K03506
Tubesheet Allowable Stress at Temperature	S	20000.00 psi
Tubesheet Allowable Stress at Ambient	Tt	20000.00 psi
Thickness of Tubesheet	h	3.0000 in.
Tubesheet Corr. Allowance (Shell side)	Cats	0.1250 in.
Tubesheet Corr. Allowance (Channel side)	Catc	0.1250 in.
Tubesheet Outside Diameter	A	22.000 in.
Area of the Untubed Lanes	AL	74.250 in ²
Is Exchanger in Creep range (skip EP, Use 3S for Sps)		NO

Stress Reduction Option	Perform Elastic-Plastic Calculation
Perform Differential Pressure Design	NO
Run Multiple Load Cases	YES
Shell Side Vacuum Pressure	Pexts 15.0000 psig

Tubesheet Integral with	Both
Tubesheet Extended as Flange	No

ASME TubeSheet Results per Part UHX, 2007 A-09**Elasticity/Expansion Material Properties :**

Shell - TM-1 Carbon Steels with C<= 0.3%

Elastic Mod. at Design Temperature	350.0 F	0.28100E+08 psi
Elastic Mod. at Ambient Temperature	70.0 F	0.29400E+08 psi

Channel - TM-1 Carbon Steels with C<= 0.3%

Elastic Mod. at Design Temperature	285.0 F	0.28375E+08 psi
Elastic Mod. at Ambient Temperature	70.0 F	0.29400E+08 psi

Tubes - TM-1 Carbon Steels with C<= 0.3%

Elastic Mod. at Tubesht. Design Temp.	350.0 F	0.28100E+08 psi
Elastic Mod. at Ambient Temperature	70.0 F	0.29400E+08 psi

TubeSheet - TM-1 Carbon Steels with C<= 0.3%

Elastic Mod. at Design Temperature	350.0 F	0.28100E+08 psi
Elastic Mod. at Ambient Temperature	70.0 F	0.29400E+08 psi

Tube Required Thickness under Internal Pressure (Tubeside pressure) :

Thickness Due to Internal Pressure:

$$= (P \cdot (D/2 - CAE)) / (S \cdot E + 0.4 \cdot P) \text{ per Appendix 1-1 (a) (1)}$$

$$= (805.00 \cdot (0.7500/2 - 0.000)) / (13400.00 \cdot 1.00 + 0.4 \cdot 805.00)$$

$$= 0.0220 + 0.0000 = 0.0220 \text{ in.}$$

Tube Required Thickness under External Pressure (Shellside pressure) :

External Pressure Chart	CS-1	at	220.00 F
Elastic Modulus for Material			29000000.00 psi

Results for Max. Allowable External Pressure (Emawp):

TCA	ODCA	SLEN	D/T	L/D	Factor A	B
0.0830	0.75	222.52	9.04	50.0000	0.0134718	13900.00

$$EMAWP = (2.167 / (D/T) - 0.0833) \cdot B = 2175.5540 \text{ psig}$$

Results for Req'd Thickness for Ext. Pressure (Tca):

TCA	ODCA	SLEN	D/T	L/D	Factor A	B
0.0126	0.75	222.52	59.69	50.0000	0.0003087	4476.86

$$EMAWP = (4 \cdot B) / (3 \cdot (D/T)) = (4 \cdot 4476.8633) / (3 \cdot 59.6889) = 100.0044 \text{ psig}$$
Summary of Tube Required Thickness Results:

Total Required Thickness including Corrosion all.	0.0220 in.
Allowable Internal Pressure at Corroded thickness	3253.95 psig
Required Internal Design Pressure	805.00 psig
Allowable External Pressure at Corroded thickness	2175.55 psig
Required External Design Pressure	100.00



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Detailed Tubesheet Results for load Case 1 corr. (Fvs + Pt)

**Results for ASME U-tube Tubesheet Calculations for Configuration a,
Per Edition 2007 A-09, Original Thickness :**

Minimum Required Thickness for Shear [HreqS]:

$$= 1/(4 * \mu) * (D_o/(0.8 * S)) * |P_s - P_t| + C_{ats} + C_{atc}$$

$$= 1/(4 * 0.250) * (19.80/(0.8 * 20000.00)) * |-15.00 - 790.00| + 0.250$$

$$= 1.2461 \text{ in.}$$

UHX-12.5.1 Step 1:

Compute the Equivalent Outer Tube Limit Circle Diameter [Do]:

$$= 2 * r_o + d_t$$

$$= 2 * 9.5246 + 0.7500 = 19.799 \text{ in.}$$

Determine the Basic Ligament Efficiency for Shear [mu]:

$$= (p - d_t) / p$$

$$= (1.000 - 0.750) / 1.000 = 0.250$$

UHX-12.5.2 Step 2 :

Compute the Ratio [Rhos]:

$$= D_s / D_o \text{ (Configurations a, b, c)}$$

$$= 21.5000 / 19.7992 = 1.0859$$

Compute the Ratio [Rhoc]:

$$= D_c / D_o \text{ (Configurations a, e, f)}$$

$$= 20.7500 / 19.7992 = 1.0480$$

Moment on Tubesheet due to Pressures (Ps, Pt) [Mts]:

$$= D_o^2/16 * [(Rhos-1)*(Rhos^2+1)*P_s - (Rhoc-1)*(Rhoc^2+1)*P_t]$$

$$= 19.799^2/16 * [(1.086 - 1) * (1.086^2 + 1) * -15.000 -$$

$$(1.048 - 1) * (1.048^2 + 1) * 790.000]$$

$$= -2019.1654 \text{ psig*in.}^2$$

UHX-12.5.3 Step 3, Determination of Effective Elastic Properties :

Compute the Ratio [rho]:

$$= l_{tx} / h = 2.5000 / 2.7500 = 0.9091 \text{ (must be } 0 \leq \rho \leq 1 \text{)}$$

Compute the Effective Tube Hole Diameter [d*]:

$$= \max(d_t - 2t_{tt} * (E_t/E) * (S_t/S) * (\rho), d_t - 2t_{tt})$$

$$= \max(0.7500 - 2 * 0.0830 * (.28100E+08/.28100E+08) *$$

$$(13400/20000) * (0.909), 0.7500 - 2 * 0.0830)$$

$$= 0.6489 \text{ in.}$$

Compute the Effective Tube Pitch [p*]:

$$= p / \sqrt{1 - 4 * \min(AL * CNV_factor, 4 * D_o * p) / (\pi * D_o^2)}$$

$$= 1.0000 / \sqrt{1 - 4 * \min(74.25 * 1.000, 4 * 19.799 * 1.000)}$$

$$(3.141 * 19.799^2)}$$

$$= 1.1480 \text{ in.}$$

Compute the Effective Ligament Efficiency for Bending [mu*]:

$$= (p^* - d^*) / p^* = (1.1480 - 0.6489) / 1.1480 = 0.43474$$

E*/E and nu* for Triangular pattern from Fig. UHX-11.3.

$$h/p = 2.750000 ; \mu^* = 0.434743$$

$$E^*/E = 0.459088 ; \nu^* = 0.304726 ; E^* = 12900383. \text{ psi}$$

Note: As h/p (2.750) is > 2, data values for h/p = 2 were used.

UHX-12.5.4 Step 4:

Compute Shell Coefficient [betaS]:

$$= ((12 * (1 - \nu^2))^0.25) / ((D_s + t_s) * t_s) \%$$

$$= ((12 * (1 - 0.30^2))^0.25) / ((21.5000 + 0.2500) * 0.2500) \%$$

$$= 0.7796 \text{ 1/in.}$$

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Determine Shell Coefficient [ks]:

$$= \text{betaS} * \text{Es} * \text{ts}^3 / (6 * (1 - \text{rnus}^2))$$

$$= 0.780 * .28100\text{E}+08 * 0.250^3 / (6 * (1 - 0.300^2))$$

$$= 62688.7617 \text{ psig} \cdot \text{in.}^2$$

Determine Shell Coefficient [Lambdas]:

$$= (6 * \text{Ds} * \text{ks}) / h^3 * (1 + h * \text{betaS} + (h * \text{betaS})^2 / 2)$$

$$= 6 * 21.500 * 62688.762 / 2.750^3 * (1 + 2.750 * 0.780 + 2.298)$$

$$= 2116043.2500 \text{ psig}$$

Determine Shell Coefficient [deltaS]:

$$= \text{Ds}^2 / (4 * \text{Es} * \text{Ts}) * (1 - \text{nus} / 2)$$

$$= 21.500^2 / (4 * .28100\text{E}+08 * 0.250) * (1 - 0.3 / 2)$$

$$= 0.0000139827$$

Calculate Parameter [OmegaS]:

$$= \text{rhos} * \text{ks} * \text{betaS} * \text{deltaS} (1 + h * \text{betaS})$$

$$= 1.0859 * 62688.76 * 0.7796 * 0.000014 (1 + 2.7500 * 0.7796)$$

$$= 2.3328 \text{ in.}^2$$

Determine Channel Coefficient [betac]:

$$= ((12 * (1 - \text{nuc}^2))^0.25) / ((\text{Dc} + \text{tc}) * \text{tc})^0.5$$

$$= ((12 * (1 - 0.30^2))^0.25) / ((20.7500 + 0.6250) * 0.6250)^0.5$$

$$= 0.4974 \text{ 1/in.}$$

Determine Channel Coefficient [kc]:

$$= \text{betac} * \text{Ec} * \text{tc}^3 / (6 * (1 - \text{rnus}^2))$$

$$= 0.497 * .28375\text{E}+08 * 0.625^3 / (6 * (1 - 0.300^2))$$

$$= 631024.0000 \text{ psig} \cdot \text{in.}^2$$

Determine Channel Coefficient [Lambdac]:

$$= (6 * \text{Dc} * \text{kc}) / h^3 * (1 + h * \text{betac} + (h * \text{betac})^2 / 2)$$

$$= 6 * 20.750 * 631024 / (2.750^3) * (1 + 2.750 * 0.497 + 0.935)$$

$$= 12477578.0000 \text{ psig}$$

Determine Channel Coefficient [deltaC]:

$$= \text{Dc}^2 / (4 * \text{Ec} * \text{Tc}) * (1 - \text{nuc} / 2)$$

$$= 20.750^2 / (4 * .28375\text{E}+08 * 0.625) * (1 - 0.3 / 2)$$

$$= 0.0000051592$$

Calculate Parameter [OmegaC]:

$$= \text{rhoc} * \text{kc} * \text{betac} * \text{deltaC} (1 + h * \text{betac})$$

$$= 1.0480 * 631024 * 0.4974 * 0.000005 (1 + 2.7500 * 0.4974)$$

$$= 4.0178 \text{ in.}^2$$

UHX-12.5.5 Step 5:

Diameter ratio [K]:

$$= A / \text{Do} = 22.0000 / 19.7992 = 1.1112$$

Determine Coefficient [F]:

$$= (1 - \text{nu}) / \text{E} * (\text{Lambdas} + \text{Lambdac} + \text{E} * \ln(K))$$

$$= (1 - 0.30) / .12900\text{E}+08 * (.21160\text{E}+07 + .12478\text{E}+08 +$$

$$.28100\text{E}+08 * \ln(1.11))$$

$$= 0.9462$$

UHX-12.5.6 Step 6:

Moment Acting on Unperforated Tubesheet Rim [M*]

$$= \text{Mts} + \text{OmegaC} * \text{Pt} - \text{OmegaS} * \text{Ps}$$

$$= -2019.165 + 16.143 * 790.000 - 5.442 * -15.000$$

$$= 1189.8807 \text{ psig} \cdot \text{in.}^2$$

UHX-12.5.7 Step 7:

Maximum Bending Moment acting on Periphery of Tubesheet [Mp]:

$$= ((M*) - \text{Do}^2 / 32 * F * (\text{Ps} - \text{Pt})) / (1 + F)$$

$$= ((1189.88) - 19.799^2 / 32 * 0.946 * (-15.00 - 790.00)) / (1 + 0.95)$$

$$= 5405.7222 \text{ psig} \cdot \text{in.}^2$$

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Maximum Bending Moment acting on Center of Tubesheet [Mo]:

$$\begin{aligned}
 &= M_p + D_o^2/64 * (3 + \nu) (P_s - P_t) \\
 &= 5405.72 + 19.799^2/64 * (3 + 0.305) (-15.00 - 790.00) \\
 &= -10889.0059 \text{ psig}\cdot\text{in.}^2
 \end{aligned}$$

Maximum Bending Moment acting on Tubesheet [M]:

$$\begin{aligned}
 &= \max(|M_p|, |M_o|) \\
 &= \max(|5405.722|, |-10889.006|) \\
 &= 10889.0059 \text{ psig}\cdot\text{in.}^2
 \end{aligned}$$

UHX-12.5.8 Results for Step 8:

Tubesheet Bending Stress at Original Thickness:

$$\begin{aligned}
 &= 6 * M / ((\mu) * (h - h_g)^2) \\
 &= 6 * 10889.006 / ((0.4347) * (2.7500 - 0.0000)^2) \\
 &= 19871.9941 \text{ psi}
 \end{aligned}$$

The Allowable Tubesheet Bending Stress [SigmaAll]:

$$= 2 * S = 2 * 20000.00 = 40000.00 \text{ psi}$$

Tubesheet Bending Stress at Final Thickness [Sigma]:

$$\begin{aligned}
 &= 6 * M / ((\mu) * (h - h_g)^2) \\
 &= 6 * 9502.534 / ((0.4436) * (1.7970 - 0.0000)^2) \\
 &= 39807.1680 \text{ psi}
 \end{aligned}$$

Required Tubesheet Thickness, for Bending Stress [HreqB]:

$$= H + CATS + CATC = 1.7970 + 0.1250 + 0.1250 = 2.0470 \text{ in.}$$

Required Tubesheet Thickness for Given Loadings (includes CA) [Hreq]:

$$= \max(H_{reqB}, H_{reqS}) = \max(2.0470, 1.2461) = 2.0470 \text{ in.}$$

UHX-12.5.9 Step 9:

$$|P_s - P_t| = |-15.00 - 790.00| = 805.000 \text{ psig}$$

Shear Stress check [Tau_limit]:

$$\begin{aligned}
 &= 3.2 * S * \mu * h / D_o \\
 &= 3.2 * 20000.00 * 0.250 * 2.750 / 19.80 = 2222.31 \text{ psig}
 \end{aligned}$$

Average Shear Stress at the Outer Edge of Perforated Region [Tau]:

$$\begin{aligned}
 &= 1/(4 * \mu) * (D_o/h) * |P_s - P_t| \\
 &= 1/(4 * 0.250) * (19.80/2.75) * |-15.00 - 790.00| \text{ psi} \\
 &= 5795.77 \text{ psi}
 \end{aligned}$$

UHX-12.5.10 Results for Step 10:

Note: For a given Shell thickness of: 0.250 in.

Min. Shell len. adjacent to the tubesheet is: 4.173 in.

Axial Shell Membrane Stress [Sigmasm]:

$$\begin{aligned}
 &= D_s^2 / (4 * t_s * (D_s + t_s)) * P_s \\
 &= 21.5000^2 / (4 * 0.2500 * (21.5000 + 0.2500)) * -15.000 \\
 &= -318.793 \text{ psi}
 \end{aligned}$$

Axial Shell Bending Stress [Sigmasb]:

$$\begin{aligned}
 &= 6 * k_s / t_s^2 * (\beta S * P_s + 6 * (1 - \nu) / (E) * \\
 &\quad D_o/h^3 * (1 + h * \beta S/2) * (M_p + D_o^2/32 * (P_s - P_t))) \\
 &= 6 * 62688.76 / 0.250^2 * [0.780 * 0.00 + 6 * (1 - 0.305) / .12900E+08 * \\
 &\quad 19.799 / 2.750^3 * (1 + 2.750 * 0.780/2) * (5405.72 + 19.799^2/32 * \\
 &\quad (-15.00 - 790.00))] \\
 &= -18088.387 \text{ psi}
 \end{aligned}$$

Shell Membrane + Bending Stress [Sigmas]:

$$\begin{aligned}
 &= |\sigma_{sm}| + |\sigma_{sb}| \text{ (Should be } \leq 1.5 * S_s) \\
 &= 18407.180 \text{ psi (Should be } \leq 25650.00)
 \end{aligned}$$

Note: For a given Channel thickness of: 0.625 in.

Min. Channel len. adjacent to the tubesheet is: 6.482 in.

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Axial Channel Membrane Stress [Sigmacm]:

$$= Dc^2 / (4 * tc * (Dc + tc)) * Pt$$

$$= 20.7500^2 / (4 * 0.6250 * (20.7500 + 0.6250)) * 790.000$$

$$= 6365.275 \text{ psi}$$

Axial Channel Bending Stress [Sigmacb]:

$$= 6 * kc / tc^2 * [\text{Betac} * (\text{deltaC} * Pt) - 6 * (1 - \nu) / (E) * Do / h^3 * (1 + h * \text{Betac} / 2) * (Mp + Do^2 / 32 * (Ps - Pt))]$$

$$= 6 * 631024 / 0.625^2 * [0.497 * 0.00 - 6 * (1 - 0.305) / .12900E+08 * 19.799 / 2.750^3 * (1 + 2.750 * 0.497 / 2) * (5405.72 + 19.799^2 / 32 * (-15.00 - 790.00))]$$

$$= 42035.566 \text{ psi}$$

Channel Membrane + Bending Stress [Sigmac]:

$$= |\text{Sigmacm}| + |\text{Sigmacb}| \text{ (Should be } \leq 1.5 * Sc)$$

$$= 48400.840 \text{ psi (Should be } \leq 30000.00) \text{ (OK FOR SIMPLY SUPPORTED PER UHX 12.6.3)}$$

Step 11, The Cylinder-to-Tubesheet Junction is Overstressed.
 Performing a simplified Elastic-Plastic calculation
 (option 3) to reduce the overstress condition.
 Modify Es and/or Ec and Recompute from Step 4 onwards.

$$Ec = Ec * (1.5 * Sc / \text{Sigmac})^{1/2}$$

$$= .28375E+08 * (1.5 * 20000.00 / 48400.84)^{1/2}$$

$$Ec = 22339326.0 \text{ psi}$$

Tubesheet Bending Stress at Original Thk., after Elas-Plas iteration:

$$= 6 * M / ((\mu) * (h - h'g)^2)$$

$$= 6 * 11242.491 / ((0.4347) * (2.7500 - 0.0000)^2)$$

$$= 20517.0898 \text{ psi (Should be } \leq 40000.00)$$

Note: Tubesheet is Not overstressed after Elas-Plastic iteration
 the design is acceptable. Recomputing tubesheet required thickness.

Required Tubesheet Thk., for Bending Stress after Elas-Plas iteration [HreqB]:

$$= H + CATS + CATC = 1.8421 + 0.1250 + 0.1250 = 2.0921 \text{ in.}$$

Required Tubesheet Thk. after Elas-Plas iteration (includes CA) [Hreq]:

$$= \text{Max}(HreqB, HreqS) = \text{Max}(2.0921, 1.2461) = 2.0921 \text{ in.}$$

Tube Weld Size Results per UW-20:

Tube Strength [Ft]:

$$= 3.1415 * t * (do - t) * Sa$$

$$= 3.1415 * 0.083 * (0.750 - 0.083) * 13400.00 = 2330.551 \text{ lb.}$$

Fillet Weld Strength [Ff]:

$$= .55 * 3.1415 * af * (do + 0.67 * af) * Sw \text{ (but not } > Ft)$$

$$= .55 * 3.1415 * 0.125 * (0.750 + 0.67 * 0.125) * 13400.00$$

$$= 2330.5510 \text{ lb.}$$

Groove Weld Strength [Fg]:

$$= .85 * 3.1415 * ag * (do + 0.67 * ag) * Sw \text{ (but not } > Ft)$$

$$= .85 * 3.1415 * 0.125 * (0.750 + 0.67 * 0.125) * 13400.00$$

$$= 2330.5510 \text{ lb.}$$

Max. Allow. Tube-Tubesheet Joint load, Lmax

$$= Ft = 2330.5510 \text{ lb.}$$

Design Strength Ratio [fd]:

$$= 1.0000$$

Weld Strength Factor [fw]:

$$= Sot / (\text{Min}(Sot, S)) = 1.0000$$

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Min Weld Length [ar]:

$$= 2 * ((0.75 * do)^2 + 1.07 * t * (do - t) * fw * fd) / 2 - .75 * do$$

$$= 0.1008 \text{ in.}$$

Minimum Required Fillet Weld Leg

afr 0.0504 in.

Minimum Required Groove Weld Leg

agr 0.0504 in.

Tube-Tubesheet Jt allowable, 2330.55 is >= tube strength 2330.55 lb.

Note: This tube-tubesheet joint is a Full Strength joint

Stress/Force summary for loadcase 1 corr. (Fvs + Pt):

Stress Description	Actual	Allowable	Pass/Fail
Tubesheet bend. stress	20517.1	<= 40000.0 psi	Ok
Tubesheet shear stress	5795.8	<= 16000.0 psi	Ok
Stress in Shell at Tubesheet	18407.2	<= 25650.0 psi	Ok
Stress in Channel at Tubesheet	48400.8	<= 67560.0 psi	Ok

Thickness results for loadcase 1 corr. (Fvs + Pt):

Thickness (in.)	Required	Actual	P/F
Tubesheet Thickness :	2.0921	3.0000	Ok
Tube-Tubesheet Fillet Weld Leg :	0.0504	0.1250	Ok
Tube-Tubesheet Groove Weld Leg :	0.0504	0.1250	Ok

U-Tube Tubesheet results per ASME UHX-12 2007 A-09**Results for 8 Load Cases:**

Case#	--Reqd. Thk. + CA Tbsht Extnsn	----- Tubesheet Bend Allwd	Stresses Shear Allwd	Case Type	Pass/ Fail
1uc	1.687 ...	15616 40000	5313 16000	Fvs+Pt	Ok
2uc	0.634 ...	2128 40000	660 16000	Ps+Fvt	Ok
3uc	1.566 ...	13358 40000	4653 16000	Ps+Pt	Ok
8uc	0.249 ...	325 40000	99 16000	Fvs+Fvt	Ok
1c	2.092 ...	20517 40000	5796 16000	Fvs+Pt-Ca	Ok
2c	0.878 ...	2765 40000	720 16000	Ps+Fvt-Ca	Ok
3c	1.921 ...	17504 40000	5076 16000	Ps+Pt-Ca	Ok
8c	0.499 ...	423 40000	108 16000	Fvs+Fvt-Ca	Ok
Max: 2.0921 ... in. 0.513 0.362 (Str. Ratio)					

Load Case Definitions:

Fvs,Fvt - User-defined Shell-side and Tube-side vacuum pressures or 0.0.

Ps, Pt - Shell-side and Tube-side Design Pressures.

Ca - With or Without Corrosion Allowance.

Shell and Channel Stress Summary:

Case#	-- Integral Cyl. Req'd. Thk. Shell Channel	Shell Stress Stress Allwd	Channel Stress Stress Allwd	Pass Fail
1uc		12937 25650	36249 67560	Ok
2uc		6811 25650	2851 30000	Ok
3uc		7553 25650	33696 67560	Ok
8uc		1163 25650	383 30000	Ok
1c		18407 25650	48401 67560	Ok
2c		10131 25650	4091 30000	Ok
3c		10474 25650	44656 67560	Ok
8c		1732 25650	562 30000	Ok
Max 0.718 0.716				

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Summary of Thickness Comparisons for 8 Load Cases:

Thickness (in.)	Required	Actual	P/F
Tubesheet Thickness :	2.0921	3.0000	Ok
Tube Thickness :	0.0220	0.0830	Ok
Tube-Tubesheet Fillet Weld Leg :	0.0504	0.1250	Ok
Tube-Tubesheet Groove Weld Leg :	0.0504	0.1250	Ok

Given Shell Thickness: 0.3750 in.
 Given Channel Thickness: 0.7500 in.

Min Shell length of thk, (0.375) adj. to tubesheet: 5.081 in.
 Min Channel length of thk, (0.750) adj. to tubesheet: 7.058 in.

Note: This is a full strength Tube to Tubesheet Joint.

Tubesheet MAWP used to Compute Hydrotest Pressure:

Stress / Force Condition	Tubeside (0 shellside)		Shellside (0 tubeside)	
	MAWP	Stress Rat.	MAWP	Stress Rat.
Tubesheet Bending Stress	1624.73	1.000	1419.19	1.000
Tubesheet Shear Stress	2222.30	1.000	2222.30	1.000
Shell Stress (Axial, Junc)	2222.30	0.770	527.43	1.000
Tubesheet-Channel Junction	1115.57	1.000	527.43	0.375
Tube Pressure Stress	3253.94	1.000	2175.54	1.000
Minimum MAWP	1115.57		527.43	

Tubesheet MAPnc used to Compute Hydrotest Pressure:

Stress / Force Condition	Tubeside (0 shellside)		Shellside (0 tubeside)	
	MAPnc	Stress Rat.	MAPnc	Stress Rat.
Tubesheet Bending Stress	2089.65	1.000	1843.79	1.000
Tubesheet Shear Stress	2424.33	1.000	2424.33	1.000
Shell Stress (Axial, Junc)	2424.33	0.518	897.94	0.995
Tubesheet-Channel Junction	1677.87	1.000	897.94	0.495
Tube Pressure Stress	3253.94	1.000	2175.54	1.000
Minimum MAPnc	1677.87		897.94	

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$$t = b \sqrt{\frac{q B}{1.5 S}}$$

TUBE SIDE PRESSURE DROP $q = 11.00000$

FRONT PASS PLATE THK..... = 0.37500
MATERIAL..... = SA-516-70N
STRESS OPER..... = 20000.00
FRONT Chan ID..... = 22.00000
FRONT Chan OAL..... = 0.00000
a..... = 23.56250
b..... = 9.93750
TABLE RCB-9.132..... = Short sides fixed
a/b..... = 2.37107
B..... = 0.75000
t..... = 0.16479

Min fillet leg [both sides] = $3/4t = .75 \times 0.16479 = 0.12359$

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Customer : SOUTHERN / MISS. POWER CO.		Item No.	HX1027/2027	W.O. : X-7930
Subject : Seismic and Wind Loading Factors		Date	6/29/2011	By : DN/MD
Wind Loading		Seismic Loading		
Given Data: From Customer Spec		Given Data: From Customer Spec		
Exposure Cat	C	Occupancy Cat:	III	
Occupancy Cat	III	Design Cat:	B	
Importance Fact	1.150	Reliability	1	
Kzt	1.000	Importance Factor	1.25	
V	100.000 mph	Site Class	C	
$qz = 0.00256KzKzIKdV^2I$		Ss	0.204 g	
Height of vessel	15.000 ft or less	S1	0.087 g	
Alpha	9.5 Table 6-2	R (Table 15.4.2)	3	
Zg	900 Table 6-2	Fa	1.2	
Kz	0.849 Table 6-3	Fv	1.7	
Kd	0.950 (Table 6-4)	Sms	0.2448 g	
qz =	23.742	Sm1	0.1479 g	
G	0.850	Sds	0.1632 g	
Cf =	0.800 (Fig 6-21)	Sd1	0.0986 g	
Wind Pressure	$= qz * G * Cf$	Cs = Sds/(R/I)	0.0680	
	16.144 psf	Min Cs =	0.0100	
SNOW LOADS				
Pg	5 psf			
CAT	C			
Ct	1.2			
I	1.1			
Pf = $0.7 * Ct * I$	6.6 psf			
SNOW LOAD AREA	48 sf			
ADDITIONAL WEIGHT	316.8 lbs			

Input Echo, Horizontal Vessel Item 1, Description: X-7930 SPTS

Design Internal Pressure	85.00	psig
Design Temperature	350.00	F
Corrosion Allowance for Vessel	0.1250	in.
Shell Material	SA-106 B	
Shell Material UNS Number	K03006	
Shell Operating Allowable Stress	17100.00	psi
Shell Ambient Allowable Stress	17100.00	psi
Head Material	SA-516 70	
Head Material UNS Number	K02700	
Head Operating Allowable Stress	20000.00	psi
Head Ambient Allowable Stress	20000.00	psi
Density of Shell and Head Material	0.2830	lb./in ³
Density of Stored Liquid	59.7420	lb./ft ³
Liquid Height in Vessel	21.5000	in.
NOTE: Liquid Height is not entered, it is being set equal to the vessel ID.		
Extra Weight	6888.490	lb. ← INCLUDES SNOW LOAD
Saddle Reaction Force Factor	3.00	
Distance from Center of Vessel to Support B	19.75	in.
Baseplate Length	19.0000	in.
Baseplate Thickness	0.5000	in.
Baseplate Width	6.0000	in.
Number of Ribs (inc. outside ribs)	2	
Rib Thickness	0.5000	in.
Web Thickness	0.5000	in.
Web Location	Side	
Height of Center Web	8.2500	in.
Design Temperature of Base Structure	100.00	F
Saddle\Baseplate\Rib\Web Material	SA-516 70	
Saddle\Baseplate\Rib\Web Material UNS Number	K02700	
Operating Allowable Stress	20000.00	psi
Ambient Allowable Stress	20000.00	psi
Force Coefficient (Shape factor)	Cf	0.800
Extra Area	0.0000	in ²
User defined Wind Pressure on Vessel	Wpre	16.14 psf
Seismic Zone Identifier, Zone	0	Zone 0
User Entered Seismic Zone Coefficient	0.0680	
Diameter Basis for Vessel	OD	
Shell Diameter	22.000	in.
Shell Length Tangent to Tangent	19.984	ft.
Thickness of Shell	0.3750	in.
Shell Joint Efficiency	0.8500	
Head Type	Elliptical	
Head Thickness	0.3125	in.
Head Joint Efficiency	0.8500	
Distance from Saddle to Vessel Tangent	29.250	in.
Saddle Width	6.000	in.
Saddle Bearing Angle	120.0000	degrees
Wear Pad Thickness	0.3750	in.
Wear Pad Extension above Horn of Saddle	2.0000	in.
Wear Pad Width	10.000	in.
Stiffening Ring Present	N	

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Results for Horizontal Vessel Number 1, Description: X-7930 SPTS**Vessel Stress Summary**

Shell Allowable Stress	used in Calculation	17100.00	psi
Shell Compressive Yield	used in Calculation	30450.00	psi
Head Allowable Stress	used in Calculation	20000.00	psi
Volume of Vessel		51.89	ft.**3
Weight of Vessel, Empty		8717.06	lb.
Weight of Vessel, Full		11816.80	lb.
Shell Thk. + CA, Req'd. vs. Actual	0.190	0.375	in.
Head Thk. + CA, Req'd. vs. Actual	0.188	0.312	in.
Shell M.A.W.P. , Req'd. vs. Actual	85.00	333.37	psig
Head M.A.W.P. , Req'd. vs. Actual	85.00	294.29	psig
	Actual	Allowable	
Long. Stress at Top of Saddles	4952.41	14535.00	psi
Long. Stress at Bottom of Saddles	-1331.41	-15118.57	psi
Long. Stress at Top of Midspan	-543.10	-15118.57	psi
Long. Stress at Bottom of Midspan	4164.10	14535.00	psi
Tangential Shear in Shell	2291.70	13680.00	psi
Circ. Stress at Horn of Saddle	-10187.31	-25650.00	psi
Circ. Stress at Tip of Wear Plate	-7370.66	-25650.00	psi
Circ. Compressive Stress in Shell	-892.24	-15225.00	psi

Wind(ASCE #7) and Seismic Results :

Transverse Wind Load Component, Ftw:

$$F_{tw} = (AFT * C_f * QZ * C_{nv_Fac}) * 0.5$$

$$F_{tw} = (8276.812 * 1.000 * 16.1440 * 0.00694) * 0.5$$

$$F_{tw} = 463.961 \text{ lb.}$$

Longitudinal Wind Load Component, Flw:

$$F_{lw} = (AFL * QZ * C_{nv_fac})$$

$$F_{lw} = (855.299 * 16.1440 * 0.00694)$$

$$F_{lw} = 95.888 \text{ lb.}$$

Transverse Earthquake Load Component, Fte:

$$F_{te} = (C_s * W_o) * 0.5$$

$$F_{te} = (0.0680 * 11816.80) * 0.5$$

$$F_{te} = 401.771 \text{ lb.}$$

Longitudinal Earthquake Load Component, Fle:

$$F_{le} = C_s * W_o$$

$$F_{le} = 0.0680 * 11816.80$$

$$F_{le} = 803.543 \text{ lb.}$$

Saddle Reaction Force due to Transverse Forces, Qr:

$$Q_r = f_{tr} * \text{Max}(F_{tw}, F_{te}) * B / E$$

$$Q_r = 3.0 * \text{Max}(463.96 , 401.77) * 19.7500 / 19.2691$$

$$Q_r = 1426.624 \text{ lb.}$$

Saddle Reaction Force due to Longitudinal forces, Ql:

$$Q_l = \text{Max}(F_{lw}, F_{le}, F_{lf}, F_{lu}) * B / L_s$$

$$Q_l = \text{Max}(95.89 , 803.54 , 0.00 , 0.00) * 19.7500 / 181.3125$$

$$Q_l = 87.528 \text{ lb.}$$

Load Combination Results for Q + Wind or Seismic or Friction or User

$$Q = W_o/2 + \text{Max}(Q_r, Q_l)$$

$$Q = 5908.40 + \text{Max}(1426.62 , 87.53)$$

$$Q = 7335.026 \text{ lb.}$$

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Summary of Loads on this Saddle Support:

Vertical Load on this Saddle	7335.03	lb.
Transverse Shear Load on this Saddle	463.96	lb.
Longitudinal Shear Load on this Saddle	803.54	lb.

Formulae and substitutions for ZICK Analysis

Shell and Head Required Thickness and MAWP :

Shell:

Thickness Due to Internal Pressure:

$$= \{P \cdot (D/2 - CAE)\} / \{S \cdot E + 0.4 \cdot P\} \text{ per Appendix 1-1 (a) (1)}$$

$$= \{85.74 \cdot (22.0000/2 - 0.000)\} / \{17100.00 \cdot 0.85 + 0.4 \cdot 85.74\}$$

$$= 0.0647 + 0.1250 = 0.1897 \text{ in.}$$

Max. All. Working Pressure at Given Thickness (MAWP):

Less Operating Hydrostatic Head Pressure of 0.74 psig

$$= \{S \cdot E \cdot (T - CA - CAE)\} / \{(D/2 - CAE) - 0.4 \cdot (T - CA - CAE)\} \text{ per Appendix 1-1 (a) (1)}$$

$$= \{17100.00 \cdot 0.85 \cdot (0.2500)\} / \{22.0000/2 - 0.000 - 0.4 \cdot 0.2500\}$$

$$= 333.37 - 0.74 = 332.63 \text{ psig}$$

Maximum Allowable Pressure, New and Cold (MAPNC):

$$= \{SA \cdot E \cdot T\} / \{D/2 - 0.4 \cdot T\} \text{ per Appendix 1-1 (a) (1)}$$

$$= \{17100.00 \cdot 0.85 \cdot 0.3750\} / \{22.0000/2 - 0.4 \cdot 0.3750\}$$

$$= 502.36 \text{ psig}$$

Actual stress at given pressure and thickness (Sact):

$$= \{P \cdot \{(D/2 - CAE) - 0.4 \cdot (T - CA - CAE)\}\} / \{E \cdot (T - CA - CAE)\}$$

$$= \{85.74 \cdot \{(22.0000/2 - 0.000) - 0.4 \cdot (0.2500)\}\} / \{0.85 \cdot (0.2500)\}$$

$$= 4398.13 \text{ psi}$$

Elliptical Head:

Thickness Due to Internal Pressure:

$$= \{P \cdot (D - 2 \cdot CAE) \cdot K\} / \{2 \cdot S \cdot E + 2 \cdot P \cdot (K - 0.1)\} \text{ per Appendix 1-4 (c)}$$

$$= \{85.74 \cdot (22.0000 - 2 \cdot 0.000) \cdot 1.00\} / \{2 \cdot 20000.00 \cdot 0.85 + 2 \cdot 85.74 \cdot (1.00 - 0.1)\}$$

$$= 0.0552 + 0.1250 = 0.1802 \text{ in.}$$

$$= 0.0625 \text{ in. (Per Ug 16b)}$$

Max. All. Working Pressure at Given Thickness (MAWP):

Less Operating Hydrostatic Head Pressure of 0.74 psig

$$= \{2 \cdot S \cdot E \cdot (T - CA - CAE)\} / \{K \cdot (D - 2 \cdot CAE) - 2 \cdot (T - CA - CAE) \cdot (K - 0.1)\} \text{ per Appendix 1-4 (c)}$$

$$= \{2 \cdot 20000.00 \cdot 0.85 \cdot (0.1875)\} / \{1.00 \cdot 22.0000 - 2 \cdot (0.1875) \cdot (1.00 - 0.1)\}$$

$$= 294.29 - 0.74 = 293.54 \text{ psig}$$

Maximum Allowable Pressure, New and Cold (MAPNC):

$$= \{2 \cdot SA \cdot E \cdot T\} / \{K \cdot D - 2 \cdot T \cdot (K - 0.1)\} \text{ per Appendix 1-4 (c)}$$

$$= \{2 \cdot 20000.00 \cdot 0.85 \cdot 0.3125\} / \{1.00 \cdot 22.0000 - 2 \cdot 0.3125 \cdot (1.00 - 0.1)\}$$

$$= 495.63 \text{ psig}$$

Actual stress at given pressure and thickness (Sact):

$$= \{P \cdot \{K \cdot (D - 2 \cdot CAE) - 2 \cdot (T - CA - CAE) \cdot (K - 0.1)\}\} / \{2 \cdot E \cdot (T - CA - CAE)\}$$

$$= \{85.74 \cdot \{1.00 \cdot 22.0000 - 2 \cdot (0.1875) \cdot (1.00 - 0.1)\}\} / \{2 \cdot 0.85 \cdot (0.1875)\}$$

$$= 5827.18 \text{ psi}$$

Longitudinal Bending (+-) at Midspan

$$= \{3 \cdot Q \cdot L \cdot K \cdot 2 / \{PI \cdot R^2 \cdot (T - CA)\}\}$$

$$= \{3 \cdot 7335 \cdot 19.98 \cdot 0.4858\} / \{PI \cdot 10.7500 \cdot 10.7500 \cdot (0.3750 - 0.1250)\}$$

$$= 2353.60 \text{ psi}$$

Compute the area ratio [K]:

$$= \{PI \cdot (\sin(\Delta)/\Delta - \cos(\Delta)) / (\Delta + \sin(\Delta) \cdot \cos(\Delta) - (\Delta + \sin(\Delta) \cdot \cos(\Delta) - 2 \cdot \sin(\Delta) \cdot \sin(\Delta))/\Delta)\}$$

$$= \{PI \cdot (\sin(1.396) / 1.396 - \cos(1.396)) / (1.396 + \sin(1.396) \cdot \cos(1.396) - 2 \cdot \sin(1.396) \cdot \sin(1.396) / 1.396)\}$$

$$= 9.3799$$

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Compute the moment fraction [X]:

$$\begin{aligned}
 &= (1 - (1 - A/L + (R^2 - H^2)/(2 * A * L)) / (1 + (4 * H)/(3 * L))) \\
 &= (1 - (1 - 2.438/19.984 + (0.896^2 - 0.452^2)/(2 * 2.438 * 19.984)) / \\
 &\quad (1 + (4 * 0.452)/(3 * 19.984))) \\
 &= 0.1417
 \end{aligned}$$

Intermediate Product [K.1]:

$$\begin{aligned}
 &= K * X * 4 * A / L \\
 &= 9.380 * 0.142 * 4 * 2.438 / 19.984 = 0.6485
 \end{aligned}$$

Longitudinal Bending (+-) at Saddle

$$\begin{aligned}
 &= (3 * Q * L * K.1 / (PI * R^2 * (T - CA))) \\
 &= (3 * 7335 * 19.98 * 0.6485) / \\
 &\quad (PI * 10.7500 * 10.7500 * (0.3750 - 0.1250)) \\
 &= 3141.91 \text{ psi}
 \end{aligned}$$

Longitudinal Pressure Stress

$$\begin{aligned}
 &= DP * ((SID/2 + CA) - 0.4 * (T - CA)) / (2.0 * (T - CA)) \\
 &= 85.0 * ((21.25 / 2 + 0.1250 - 0.4 * (0.375 - 0.1250)) / \\
 &\quad (2.0 * (0.375 - 0.1250))) \\
 &= 1810.50 \text{ psi}
 \end{aligned}$$

Note: The Longitudinal Stress from Zick Analysis is combined with the
Longitudinal Pressure Stress to get the total stress.

Tangential Shear in Shell near Saddle

$$\begin{aligned}
 &= Q * K.4 * ((L - H - 2A)/(L + H)) / (R * (T - CA)) \\
 &= 7335 * 1.1707 * ((19.98 - 0.45 - 2 * 2.44) / \\
 &\quad (19.98 + 0.45)) / (10.7500 * (0.3750 - 0.1250)) \\
 &= 2291.70 \text{ psi}
 \end{aligned}$$

Circumferential Stress at Tip of the Wear Plate (L >= 8R)

$$\begin{aligned}
 &= -Q / (4 * (T - CA) * (SADWTH + 1.56 * SQRT(R * (T - CA)))) - 3.0 * Q * K13 / \\
 &\quad (2 * (T - CA)^2) \\
 &= -7335 / (4 * 0.2500 * (6.00 + 1.56 * SQRT(10.7500 * 0.2500))) \\
 &\quad - 3 * 7335 * 0.0370 / (2 * 0.2500^2) \\
 &= -7370.66 \text{ psi}
 \end{aligned}$$

Note: Wear Plate thk. could Not be considered in this formula because.

Saddle-Tangent Distance A (29.2) is > R/2 (5.4 in.)

Circumferential Stress at Horn of Saddle (L >= 8R)

$$\begin{aligned}
 &= -Q / (4 * TEM * (SADWTH + 1.56 * SQRT(R * (T - CA)))) - 3.0 * Q * K.7 / (2 * TEB) \\
 &= -7335 / (4 * 0.2500 * (6.00 + 1.56 * SQRT(10.7500 * 0.2500))) \\
 &\quad - 3 * 7335 * 0.0530 / (2 * 0.0625) \\
 &= -10187.31 \text{ psi}
 \end{aligned}$$

Circumferential Compression at Bottom of Shell

$$\begin{aligned}
 &= (Q * (K.9 / (TEM9 * WPDWTH))) \\
 &= (7335 * (0.7603 / (0.6250 * 10.000))) \\
 &= -892.24 \text{ psi}
 \end{aligned}$$

Moment of Inertia of Saddle - Lateral Direction

	Y	A	AY	Ay ²	Io
Shell	0.1250	3.1394	0.3924	0.0491	0.0164
Wearplate	0.4375	3.7500	1.6406	0.7178	0.0439
Web	4.1875	3.5625	14.9180	62.4690	15.0710
BasePlate	8.0000	3.0000	24.0000	192.0000	0.0625
Totals	12.7500	13.4518	40.9510	255.2358	15.1938

Value $C1 = \text{Sumof}(Ay) / \text{Sumof}(A)$ = 3.0443 in.
 Value $I = \text{Sumof}(Ay^2) + \text{Sumof}(Io) - C1 * \text{Sumof}(Ay)$ = 145.7639 in⁴
 Value $As = \text{Sumof}(A) - A_{shell}$ = 10.3125 in²

$K1 = (1 + \cos(b) - .5 * \sin(b)^2) / (\pi - b + \sin(b) * \cos(b)) = 0.2035$

$Fh = K1 * Q = 0.2035 * 7335.026 = 1492.837 \text{ lb.}$

Tension Str., $St = (Fh / As)$ = 144.7600 psi
 Allowed Str., $Sa = .6 * \text{Yield Stress}$ = 22800.0000 psi

$d = B - R * \sin(\theta) / \theta$ = 10.1098 in.
 Bending Moment, $M = Fh * d$ = 1257.6931 ft.lb.

Bending Stress, $S_{bnd} = (M * C1 / I)$ = 315.2018 psi
 Allowed Str., $Sa = .66 * \text{Yield Str.}$ = 25080.0020 psi

Minimum Thickness of Baseplate

$= (3 * Q * \text{BasePlateWidth} / (2 * \text{BasePlateLength} * \text{AllStress}))^{1/2}$
 $= (3 * 7335 * 6.00 / (2 * 19.000 * 25080.002))^{1/2}$
 $= 0.372 \text{ in.}$

Calculation of Axial Load, Intermediate Values and Compressive Stress:

Effective Baseplate Length (e)
 $= (B_{plen} - \text{Clearance}) / (N_{ribs} - 1)$
 $= (19.0000 - 1.0) / (2 - 1) = 18.0000 \text{ in.}$

Baseplate Pressure Area (Ap)
 $= e * B_{pwid} / 2$
 $= 18.0000 * 6.0000 / 2 = 54.0000 \text{ in}^2$

Axial Load (P)
 $= Ap * B_p$
 $= 54.00 * 64.34 = 3474.49 \text{ lb.}$

Area of the Rib and Web (Ar)
 $= (B_{pwid} - \text{Clearance} - \text{Webtk}) * \text{Ribtk} + e/2 * \text{Webtk}$
 $= (6.000 - 1.0 - 0.500) * 0.500 + 18.0000 / 2 * 0.500$
 $= 6.750 \text{ in}^2$

Compressive Stress (Sc)
 $= P / Ar$
 $= 3474.49 / 6.7500 = 514.7387 \text{ psi}$

Check of Outside Ribs**Inertia of Saddle, Outer Ribs - Axial Direction**

	Y	A	AY	Ay ²	Io
Rib	2.7500	2.5000	6.8750	6.4573	6.9323
Web	0.2500	4.5000	1.1250	3.5874	0.1875
Values	1.1429	7.0000	8.0000	10.0446	7.1198

$KL/R < C_c$ (8.4659 < 123.2882) per AISC E2-1 9th Edition

$Sca = (1 - (Klr)^2 / (2 * Cc^2)) * Fy / (5/3 + 3 * (Klr) / (8 * Cc) - (Klr^3) / (8 * Cc^3))$

$Sca = (1 - (8.47)^2 / (2 * 123.29^2)) * 38000 /$
 $(5/3 + 3 * (8.47) / (8 * 123.29) - (8.47^3) / (8 * 123.29^3))$

$Sca = 22400.70 \text{ psi}$

AISC Unity Check on Outside Ribs (must be ≤ 1.0)

$Check = Sc/Sca + (Rm/Z) / Sba$

$Check = 514.74 / 22400.70 + (2569.22 / 4.450) / 25080.00$

$Check = 0.05$

PV Elite is a registered trademark of Intergraph Corporation [2010]

Item No.: HX1027/2027

Job No.: X-7930

REV. 1

By: DN/MD

2/16/2011

P.O. No.: 17496-0001

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Energy Exchanger Company

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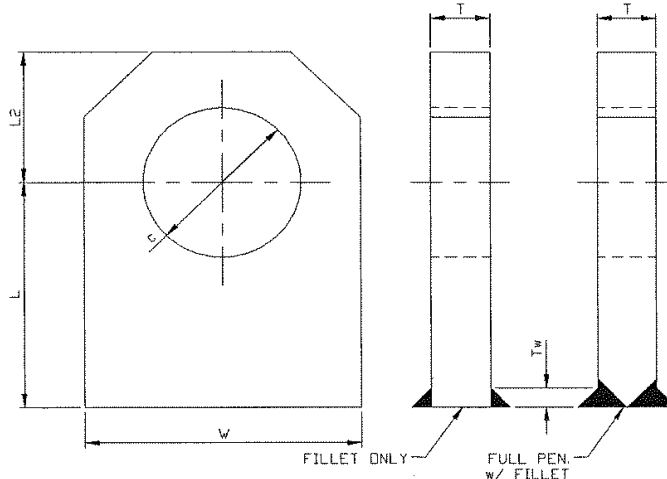
Customer :	MISSISSIPPI POWER/SOUTHERN COMPANY SERVICES	Item No	HX1027/2027	W.O. :	X-7930
Subject :	LIFTING LUG CALCULATION	Date	2/16/2011	By :	DN/MD

Note : Lugs are not designed for side loading. Do not side load lugs.

Material	SA-516-70
Yield Strength	38000 psi
T =	1/2 in
Tw =	1/4 in
W =	4 1/4 in
L =	4 3/4 in
L2 =	2 1/8 in
OAL =	6 7/8 in
C =	2 in
Analysis Type	Full Pen w/ Fillet
Impact Factor	1.500
Occasional Load Factor	1.125
Heaviest Lug Load	600 #
(CHANNEL COVER)	
Weld Group Area (Aw)	3.182 in ²
Weld Group Inertia (Iw)	5.321 in ⁴
Shear Area (As)	0.563 in ²
Lug Inertia (I)	3.199 in ⁴

Allowable Loading

Shear Stress	17100 psi
0.4 * Yield * Occ Factor	
Bearing Stress	32062.5 psi
MIN(0.75*Yield*Occ Factor, 0.9*Yield)	
Combined	28215 psi
MIN(.66*Yield*Occ Factor, 0.75*Yield)	



Calculated Loads

Primary Shear in Welds	282.89 psi
Load*Impact/(Aw)	
Bending Shear Stress in Welds	401.72 psi
Load*Impact*(W+2*Tw)/2/(Iw)	
Total Combined Shear	684.60 psi
Shear in Lug Above Hole	1066.67 psi
Load*Impact/(As)	
Pin Hole Bearing Stress	900.00 psi
Load*Impact/(T*C)	
Bending Stress @ Lug Base	2840.14 psi
Load*Impact*L/(W^2*T/6)	
Tensile @ Lug Base	423.53 psi
Load*Impact/(W*T)	
Total Combined Stress @ lug Base	3263.67 psi



Energy Exchanger Company

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Customer : MISSISSIPPI POWER c/o SOUTHERN COMPANY SERVICES

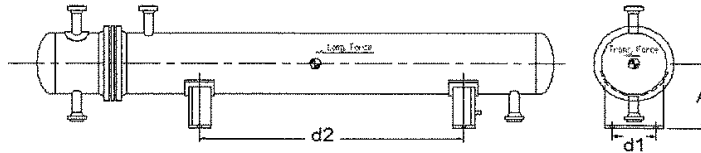
Item No HX1027/2027

W.O. : X-7930

Subject : ANCHOR BOLTING CALC

Date 4/7/2011

By : DN/MD



Static Balance

Near Saddle Ref Dimension:	40 in	Number of Bolts (Fixed only)*	2
Far Saddle Ref Dimension:	196 in	Bolt Diam.	1 in 
COG Ref Dimension:	94 in	Bolt Area (Ab)	0.551 in ²
Weight	11500 lb	Bolting Material	F1554 (Gr 36)
Dim A	19.75 in	Allowable Stress Shear	11800 psi
Dim d1	15 in	Allowable Stress Tension	11800 psi
Dim d2	156 in		

Reaction Forces

Near Saddle (Rfn)	7519 lb	Greatest Transverse Load (Ft)	464 lb
Far Saddle (Rff)	3981 lb	Greatest Longitudinal Load (Fl)	804 lb
Rf = 0 or Rff if COG outside saddles	0 lb		

Transverse Shear Calculation:

$$Ss = Ft / (\text{total bolts} * \text{bolt area}) = 211 \text{ psi}$$

Longitudinal Shear Calculation:

$$Sl = Fl / (\text{fixed bolts} * \text{bolt area}) = 730 \text{ psi}$$

Transverse Overturning Moment Calc

$$Stm = (48 * (Ft * A / 12) / (d1 * \text{total bolts}) - (\text{Weight} / \text{total bolts})) / Ab$$

$$Stm = -4109 \text{ psi}$$

Longitudinal Overturning Moment Calc

$$Slm = (48 * (Fl * A / 12) / (d2 * \text{total bolts}) - (\text{Weight} / \text{total bolts})) / Ab$$

$$Slm = -5033 \text{ psi}$$

* Longitudinal shear forces countered by bolting in stationary support only.
transverse forces counter by full bolting (fixed support bolts * 2)

All calculated stresses are less than allowable
Anchor bolting design is acceptable.

CALCULATION IS FOR SIZING OF SUPPORT HOLES & SLOTS. THIS CALCULATION DOES NOT REPLACE OR RELIEVE THE CIVIL/STRUCTURAL ENGINEERING DESIGN FOR THE PARTY SUPPLYING ANCHOR BOLTS

SECTION 3

FORM U-1 MANUFACTURER'S DATA REPORT FOR PRESSURE VESSELS
As Required by the Provisions of the ASME Code Rules, Section VIII, Division 1

1. Manufactured and certified by ENERGY EXCHANGER COMPANY, 1844 NORTH GARNETT ROAD, TULSA, OK 74116
(Name and address of Manufacturer)

2. Manufactured for SOUTHERN COMPANY SERVICES, INC. 42 INVERNESS CENTER PARKWAY BIRMINGHAM, AL 35242
(Name and address of Purchaser)

3. Location of installation MISSISSIPPI POWER, DEKALB MS.
(Name and address)

4. Type: HORIZ. HEAT EXCHANGER X-7930 A
(Horiz., vert., or sphere) (Tank, separator, jkt. vessel, heat exch., etc.) (Mfg's serial No.)

N/A X-7930-A REV. 5 6044 2012
(CRN) (Drawing No.) (Nat'l Bd. No.) (Year built)

5. ASME Code, Section VIII, Div. 1 2007 EDITION, '09 ADD. N/A N/A
(Edition and Addenda (date)) (Code Case No.) (Special Service per UG-120(d))

Items 6-11 incl. to be completed for single wall vessels, jackets of jacketed vessels, shell of heat exchangers, or chamber of multichamber vessels.

6. Shell (a) No. of course(s): 1 (b) Overall length (ft & in.): 19'-8 13/16"

Course(s)			Material	Thickness		Long. Joint (Cat. A)			Circum. Joint (Cat. A, B, & C)			Heat Treatment	
No.	Diameter, in.	Length (ft & in.)	Spec./Grade or Type	Nom.	Corr.	Type	Full, Spot, None	Eff.	Type	Full, Spot, None	Eff.	Temp.	Time
1	22" O.D.	19'-8 13/16"	SA-106B	3/8"	1/8"	S	NONE	0.85	1 (f)	SPOT	0.85	N/A	N/A

7. Heads: (a) SA-516-70 (b) NA
(Mat'l Spec. No., Grade or Type) (H.T. - Time & Temp.) (Mat'l Spec. No., Grade or Type) (H.T. - Time & Temp.)

	Location (Top, Bottom, Ends)	Thickness		Radius		Elliptical Ratio	Conical Apex Angle	Hemispherical Radius	Flat Diameter	Side to Pressure		Category A		
		Min.	Corr.	Crown	Knuckle					Convex	Concave	Type	Full, Spot, None	Eff.
(a)	END	5/16"	1/8"			2:1					X	S	NONE	0.85
(b)														

If removable, bolts used (describe other fastening) NA
(Mat'l Spec. No., Grade, size, No.)

8. Type of jacket NA Jacket closure NA
(Describe as open & weld, bar, etc.)

If bar, give dimensions NA If bolted, describe or sketch.

9. MAWP 215 15 psi at max. temp. 350 350 °F Min. design metal temp. 10 °F at 215 psi.
(internal) (external) (internal) (external)

10. Impact test NO, EXEMPT PER UG-20(f) at test temperature of NA °F.
(Indicate yes or no and the component(s) impact tested)

11. Hydro., pneu., or comb. Test press. 280 P.S.I.G. Proof test NA

Items 12 and 13 to be completed for tube sections.

12. Tubesheet: SA-286-4N 22" 3" 1/4" Welded
(Stationary (Mat'l Spec. No.)) (Dia., in. (subject to press.)) (Nom. thk., in.) (Corr. Allow., in.) (Attachment (welded or bolted))

NA NA NA NA NA
(Floating (Mat'l Spec. No.)) (Dia., in.) (Nom. thk., in.) (Corr. Allow., in.) (Attachment)

13. Tubes: SA-179 3/4" 0.083" THK (MIN) 133 "U"
(Mat'l Spec. No., Grade or Type) (O.D., in.) (Nom. thk., in. or gauge) (Number) (Type (Strait or U))

Items 14-18 incl. to be completed for inner chambers of jacketed vessels or channels of heat exchangers.

14. Shell (a) No. of course(s): 1 (b) Overall length (ft & in.): 1'-7 7/16"

Course(s)			Material	Thickness		Long. Joint (Cat. A)			Circum. Joint (Cat. A, B, & C)			Heat Treatment	
No.	Diameter, in.	Length (ft & in.)	Spec./Grade or Type	Nom.	Corr.	Type	Full, Spot, None	Eff.	Type	Full, Spot, None	Eff.	Temp.	Time
1	20 1/2" I.D.	1'-7 7/16"	SA-516-70N	3/4"	1/8"	1	SPOT	0.85	1 (f)	SPOT	0.85	1150° F.	1-HR.

15. Heads: (a) SA-286-4N (b) NA
(Mat'l Spec. No., Grade or Type) (H.T. - Time & Temp.) (Mat'l Spec. No., Grade or Type) (H.T. - Time & Temp.)

	Location (Top, Bottom, Ends)	Thickness		Radius		Elliptical Ratio	Conical Apex Angle	Hemispherical Radius	Flat Diameter	Side to Pressure		Category A		
		Min.	Corr.	Crown	Knuckle					Convex	Concave	Type	Full, Spot, None	Eff.
(a)	END	3 1/4"	3/16"						21 5/16"					
(b)														

If removable, bolts used (describe other fastening) a) SA-193B7 ; 1 1/8" DIA; 24
(Mat'l Spec. No., Grade, size, No.)

FORM U-1 (Back)

16. MAWP 792 NA psi at max. temp. 285 NA °F Min. design metal temp. 10 °F at 792 psi.
(internal) (external) (internal) (external)
17. Impact test NO, EXEMPT PER UG-20(f) at test temperature of NA °F.
(Indicate yes or no and the component(s) impact tested)
18. Hydro., pneu., or comb. Test press. 1030 P.S.I.G. Proof test NA
19. Nozzles, inspection, and safety valve openings:

Purpose (Inlet, Outlet, Drain, etc.)	No.	Diameter or Size	Flange Type	Material		Nozzle Thickness		Reinforcement Material	How Attached		Location (Insp. Open.)
				Nozzle	Flange	Nom.	Corr.		Nozzle	Flange	
INLET	1	6"-150#	RF-WN	SA-108B	SA-105	0.4320"	1/8"	SA-516-70	WELDED	WELDED	SHELL
OUTLET	1	2"-150#	RF-LWN	SA-105	—	0.5300"	1/8"	WELD	WELDED	—	SHELL
INLET	1	4"-600#	RF-LWN	SA-105N	—	1.0000"	1/8"	WELD	WELDED	—	CHANNEL
OUTLET	1	4"-600#	RF-LWN	SA-105N	—	1.0000"	1/8"	WELD	WELDED	—	CHANNEL
VENT	1	2"-600#	RF-LWN	SA-105N	—	0.6800"	1/8"	WELD	WELDED	—	CHANNEL
DRAIN	1	2"-600#	RF-LWN	SA-105N	—	0.6800"	1/8"	WELD	WELDED	—	CHANNEL

20. Supports: Skirt NO Lugs Legs Others (2) Saddles Attached WELDED TO SHELL
(Yes or no) (No.) (No.) (Describe) (Where and how)
21. Manufacturer's Partial Data Reports properly identified and signed by Commissioned Inspectors have been furnished for the following items of the report:
 (List the name of part, item number, mfg's. name and identifying number)

22. Remarks: SERVICE: PROCESS CONDENSATE TRIM COOLER; P.O. NO: 17496-0001; ITEM NO.: HX1027
SIZE: 20-216, TYPE: NEU, TUBES DESIGNED W/ 0" C.A., SAFETY RELIEF DEVICES BY OTHERS
LINES 14-18 INCLUDES (1) 27 7/8" O.D. X 20 1/2" I.D. X 4 9/16" THK., SA-266-4N RING
(1) Tubesheet to cylinder circumferential seams are Type 7 joints w/ efficiency of 1.0

CERTIFICATE OF SHOP COMPLIANCE

We certify that the statements in this report are correct and that all details of design, material, construction, and workmanship of this vessel conform to the ASME BOILER AND PRESSURE VESSEL CODE, Section VIII, Division 1.

U Certificate Authorization No. 12370 Expires SEPTEMBER 27, 20 13

Date 6-22-12 Name ENERGY EXCHANGER COMPANY Signed Mark Wells
(Manufacturer) (Representative)

CERTIFICATE OF SHOP INSPECTION

I, the undersigned, holding a valid commission issued by the National Board of Boiler and Pressure Vessel Inspectors and/or the State or Province of OKLAHOMA and employed by ONEBEACON AMERICA INSURANCE COMPANY of LYNN, MA

have inspected the pressure vessel described in this Manufacturer's Data Report on 6-22-2012, and state that, to the best of my knowledge and belief, the Manufacturer has constructed this pressure vessel in accordance with ASME BOILER AND PRESSURE VESSEL CODE, Section VIII, Division 1. By signing this certificate neither the Inspector nor his employer makes any warranty, expressed or implied, concerning the pressure vessel described in this Manufacturer's Data Report. Furthermore, neither the Inspector nor his employer shall be liable in any manner for any personal injury or property damage or a loss of any kind arising from or connected with this inspection.

Date 6-22-12 Signed [Signature] Commissions N.B.# 12064 A OKLA.# 7
(Authorized Inspector) (Natl Board incl. endorsements, State, Province, and No.)

CERTIFICATE OF FIELD ASSEMBLY COMPLIANCE

We certify that the statements on this report are correct and that field assembly construction of all parts of this vessel conforms with the requirements of ASME BOILER AND PRESSURE VESSEL CODE, Section VIII, Division 1. U Certificate of Authorization No.

U Certificate of Authorization No. Expires , 20

Date Name Signed
(Assembler) (Representative)

CERTIFICATE OF FIELD ASSEMBLY INSPECTION

I, the undersigned, holding a valid commission issued by the National Board of Boiler and Pressure Vessel Inspectors and/or the State or Province of and employed by

of , have compared the statements in this Manufacturer's Data Report with the described pressure vessel and state that parts referred to as data items , not included in the certificate of shop inspection, have been inspected by me and to the best of my knowledge and belief, the Manufacturer has constructed and assembled this pressure vessel in accordance with ASME BOILER AND PRESSURE VESSEL CODE, Section VIII, Division 1. The described vessel was inspected and: psi. By signing this certificate neither the Inspector nor his employer makes any warranty, expressed or implied, concerning the pressure vessel described in this Manufacturer's Data Report. Furthermore, neither the Inspector nor his employer shall be liable in any manner for any personal injury or property damage or a loss of any kind arising from or connected with this inspection.

Date Signed Commissions
(Authorized Inspector) (Natl Board incl. endorsements, State, Province, and No.)

NB 6044



CERTIFIED BY
Energy Exchange Company
TULSA, OKLAHOMA

MAWP SHELL	215	P.S.I. @	350	OF	280	TEST P.S.I.G.
	150	P.S.I. @	350	OF		
MAWP TUBE	792	P.S.I. @	285	OF	1030	TEST P.S.I.G.
	- - -	P.S.I. @	- - -	OF		
MIN. DESIGN METAL TEMP.	RT-3 HT-T		10	OF @	215	P.S.I.G.
			10	OF @	792	P.S.I.G.

SERIAL NO. X-7930 A YEAR BUILT 2012

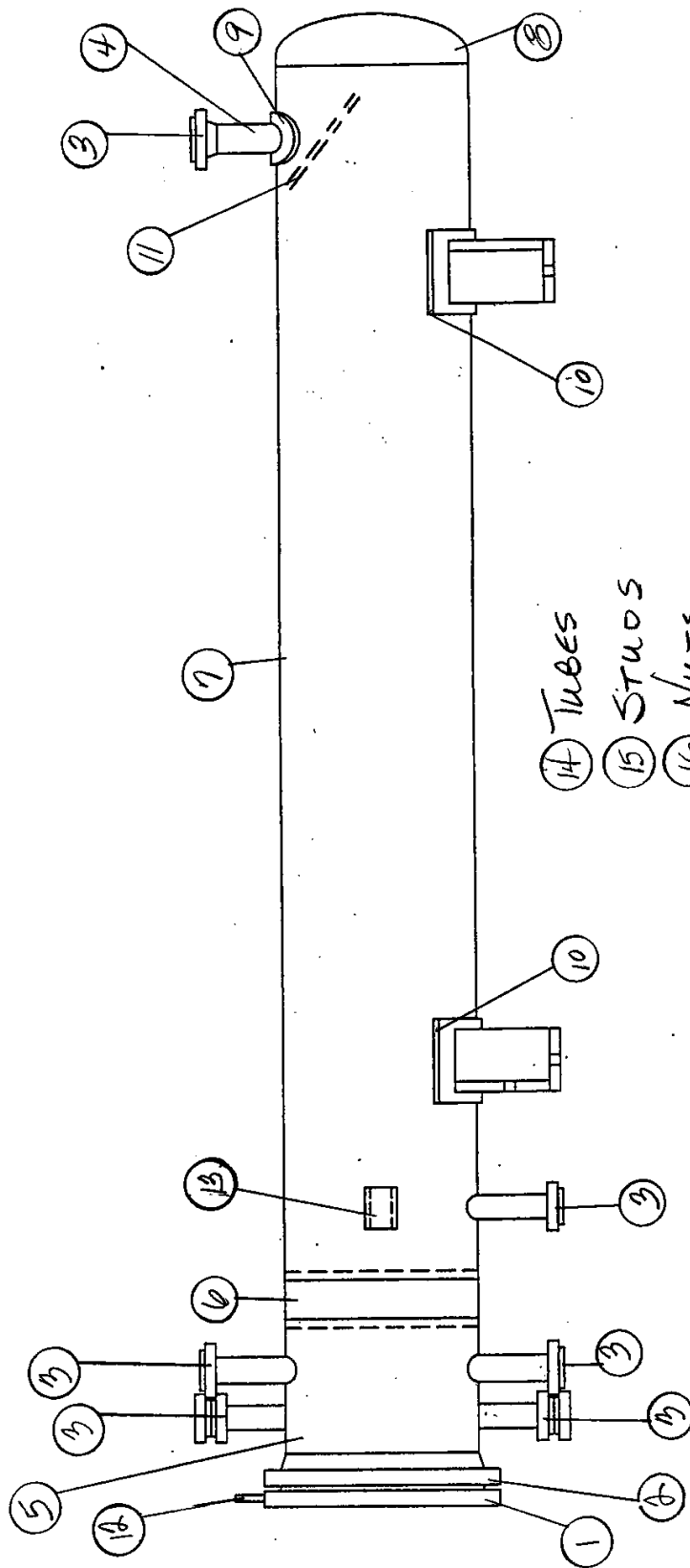
P.O. NO. 17496-0001

SERVICE PROCESS CONDENSATE TRIM COOLER

ITEM HX1027 SIZE 20-216 TYPE NEU

DESIGN PRESSURE: SHELL = 85 PSI; TUBE = 790 PSI

SECTION 4



- 14 TUBES
 15 STUDS
 16 NUTS
 17 PASS PLATES

Reviewed / Accepted
 I.Q.S. #3
 William Brennaugh

X-7930 A+B

ENERGY EXCHANGER COMPANY

MATERIAL HEAT NUMBER INDEX

Project: Kemper County 1 - IGCC

CUSTOMER: Southern Co. (for) Mississippi Power Company
 DESTINATION: DeKalb, Mississippi
 P.O. No: 17496-0001
 Req. No: MC202

ITEM NO: HX1027/HX2027
 SERVICE: Process Condensate Trim Heater
 DESCRIPTION: 2-20" x 216" NEU Exchangers

PAGE: 1 of 2
 DATE: June 12, 2012
 JOB NO: X-7930 A/B

LINE NO.	HEAT NO.	SLAB NO.	STEEL PRODUCER	GRADE	DESCRIPTION	PCS	SIZE
1	227N568		ArcelorMittal	SA-266-4N	(#1 Channel Cover)	2	27 7/8" OD x 3 1/4" thk.
2	110786		Nucor	SA-266-4N	(#2 Channel Flange)	2	27 7/8" OD x 20 1/2" ID x 4 9/16" thk.
3	B847		FCI	SA-105-N	(Nozzle Flange T-1 & 2)	4	4" 600# RF LWN x 13" lg.
3	C855AN		FVC	SA-105-N	(Nozzle Flange V-1 & D-1)	4	2" 600# RF LWN 12" lg.
3	3021551		Galperti	SA-105-N	(Nozzle Flange V-1 & D-1)	4	2" 600# RF Blind
3	JFS		Coffer	SA-105	(Nozzle Flange S-1)	2	6" 150# RF WN Sch X-Hvy. Bore
3	G136		FCI	SA-105	(Nozzle Flange S-2)	2	2" 150# RF LWN x 10" lg.
4	X22424		U.S.S.	SA-106-B	(Nozzle Pipe S-1)	2	6" Sch X-Hvy. X 7" lg.
5	R4137	11B	ArcelorMittal	SA-516-70N	(Channel Cylinder)	2	20 1/2" ID x 3/4" thk. x 1'-7 7/16" lg.
6	227N568		ArcelorMittal	SA-266-4N	(#4 Tubesheet)	2	22" OD x 3" thk.
7	MA2051		U.S.S.	SA-106-B	(Shell Cylinder)	2	22" OD x 3/8" thk. x 19'-8 13/16" lg.
8	AWDL W01628 AWGD	F12	SSAB	SA-516-70	(Shell Head) Unit B	1	22" OD x 5/16" (min) thk. 2:1 Ellip. w/2" S.F.
8	811P02140	H066332	ArcelorMittal	SA-516-70	(Shell Head) Unit A	1	22" OD x 5/16" (min) thk. 2:1 Ellip. w/2" S.F.

I hereby certify that the above information is correct to the best of my knowledge and belief.

ENERGY EXCHANGER COMPANY

By:

[Signature]

Reviewed / Accepted
 I.Q.S. # 3

William B. Breaugh

ENERGY EXCHANGER COMPANY MATERIAL HEAT NUMBER INDEX

Project: Kemper County 1 - IGCC

CUSTOMER: Southern Co. (for) Mississippi Power Company
 DESTINATION: DeKalb, Mississippi
 P.O. No: 17496-0001
 Req. No: MC202
 ITEM NO: HX1027/HX2027
 SERVICE: Process Condensate Trim Heater
 DESCRIPTION: 2-20" x 216" NEU Exchangers
 PAGE: 2 of 2
 DATE: June 12, 2012
 JOB NO: X-7930 A/B

PART NO.	HEAT NO.	SUB NO.	STEEL PRODUCER	GRADE	DESCRIPTION	QTY	SIZE
9	1502456	03	Nucor	SA-516-70	(Shell Weld Pads)	2	9 3/4" OD x 3/8" thk.
10	1502456	03	Nucor	SA-516-70	(Support Pads)	2	10" x 3/8" thk. x 26 1/2" lg.
11	1502456	03	Nucor	SA-516-70	(Deflector Plate)	2	7 1/8" x 3/8" thk. x 19 3/4" lg.
12	B1T7537	03	Nucor	SA-516-70	(Lifting Lugs)	2	3 1/2" x 1/2" thk. x 6 7/8" lg.
13	W0H543	24	SSAB	SA-516-70	(Name Plate Brackets)	2	7 1/2" x 3/16" thk. x 22" lg.
14	181069		Benteler	SA-179	(Tubes)	238	3/4" OD x .083" (min) x V/L
14	548853		Benteler	SA-179	(Tubes)	34	3/4" OD x .083" (min) x V/L
15	108465		Vulcan Thrd. Prod.	SA-193-B7	(Studs)	48	1 1/8" (8 Thd) x 9 1/8" lg.
16	MR851		Unytite	SA-194-2H	(Nuts)	96	1 1/8" (8 Thd)
17	821T00580	J031960	ArcelorMittal	SA-516-70	(Pass Plates)	2	9 15/16" x 3/8" thk. x 24" lg.
17	821T00580	J031960	ArcelorMittal	SA-516-70	(Pass Plates)	2	20 3/8" x 3/8" thk. x 24" lg.

MM187157

I hereby certify that the above information is correct to the best of my knowledge and belief.

INSPECTION DEPARTMENT

REVIEWED

WITNESSED

DATE: 6/26/12

ENERGY EXCHANGER COMPANY

By:

Signature of William Breunigh

Reviewed / Accepted
I.Q.S. # 3

William Breunigh



OKLAHOMA FORGE, INC.

Certification of Analysis and Tests

111-66965

Date: 6/20/11

Toll Free (866)909-5553
Local(918)446-5553 FAX (918)446-4150

e-Mail ~ sales@oklahomaforge.com
Web Site ~ www.oklahomaforge.com

P.O. Box 701500
Tulsa, Oklahoma 74170-1500

ENERGY EXCHANGER COMPANY
1844 N. GARNETT ROAD
TULSA, OK 74116 USA

1199
JIM ELDER
5/17/2011

111-51903
DELIVERY
6/20/2011

1	X-7926-4/9	111-51903-01	DISC	16.000"OD x 3.000"TH	2
		ARCELOMITTAL	227N568	SA266-10 GR4 NORMALIZED ✓	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.18 1.16 .014 .008	.23 .10 .09 .27 .027	.017 <.001 .021	.42	SN-.011; B-.0003
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	49,600 ✓	75,500 ✓	34 ✓	68 ✓	146 ✓
				FINE	CVN
				-50F	114 127 137 80
2	X-7926-1/1A	111-51903-02	DISC	21.125"OD x 1.625"TH	2
		ARCELOMITTAL	227N568	SA266-10 GR4 NORMALIZED	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.18 1.16 .014 .008	.23 .10 .09 .27 .027	.017 <.001 .021	.42	SN-.011; B-.0003
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	49,600 ✓	75,500 ✓	34 ✓	68 ✓	146 ✓
				FINE	CVN
				-50F	114 127 137 80
3	X-7930-4	111-51903-03	DISC	22.000"OD x 3.000"TH	2
		ARCELOMITTAL	227N568	SA266-10 GR4 NORMALIZED	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.18 1.16 .014 .008	.23 .10 .09 .27 .027	.017 <.001 .021	.42	SN-.011; B-.0003
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	49,600 ✓	75,500 ✓	34 ✓	68 ✓	146 ✓
				FINE	CVN
				-50F	114 127 137 80
4	X-7930-1	111-51903-04	DISC	27.875"OD x 3.250"TH	2
		ARCELOMITTAL	227N568	SA266-10 GR4 NORMALIZED	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.18 1.16 .014 .008	.23 .10 .09 .27 .027	.017 <.001 .021	.42	SN-.011; B-.0003
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	49,600 ✓	75,500 ✓	34 ✓	68 ✓	146 ✓
				FINE	CVN
				-50F	114 127 137 80
5	X-7930-2	111-51903-08	RING	27.875"OD x 20.500"ID x 4.188"TH	2
		NUCOR	110786	SA266-10 GR4 NORMALIZED	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.17 1.17 .010 .002	.20 .10 .10 .19 .03	.016 .003 .024	.41	SN-.008; TI-.002
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	48,800 ✓	73,500 ✓	35 ✓	74 ✓	143 ✓
				FINE	CVN
				-50F	85 85 104 67
9	X-7929-2/2A	111-51903-09	RING	28.188"OD x 23.000"ID x 3.063"TH	2
		NUCOR	110786	SA266-10 GR4 NORMALIZED	
	C ✓ Mn ✓ P ✓ S ✓	Si ✓ Ni ✓ Cr ✓ Cu ✓ Mo ✓	V ✓ Cb ✓ Al ✓ Pb ✓ Ce ✓	Other	
	.17 1.17 .010 .002	.20 .10 .10 .19 .03	.016 .003 .024	.41	SN-.008; TI-.002
	Yield Lb/SqIn	Tensile Strength Lb/SqIn	Elong%in 2In	Red of Area%	Brinell
	48,800 ✓	73,500 ✓	35 ✓	74 ✓	143 ✓
				FINE	CVN
				-50F	85 85 104 67

Notes:

Reviewed / Accepted
I.Q.S. #3

William Brennaugh

VERIFIED BY

JUN 27 2011

INSPECTION DEPARTMENT #1

REVIEWED

WITNESSED

DATE: 6/26/12

I CERTIFY THAT THERE IS A TRUE COPY OF THE ORIGINAL TEST SHEET NOW ON FILE AT THE OFFICE OF OKLAHOMA FORGE, INC. AND THAT THIS MATERIAL WAS MANUFACTURED IN THE UNITED STATES OF AMERICA.

Anneal by heating to 1450-1550 degrees F for one hour/inch of thinnest section. Slow cool furnace to 700 degrees F then air cool by opening door.
Normalize by heating to 1650 degrees F. Hold at 1650 degrees F for one hour/inch of thinnest section and air cool.
Solution Anneal by heating to 2000-2050 degrees F and Water Quenching.

R. J. Patterson

MM187157

CUSTOMER ORDER NUMBER
SOLD/SHIPPED TO

56074-12
PROGRESSIVE SUPPLY
P.O. BOX 470748

TULSA

OK 74147

USA

Item Quantity Description

1 4 4" X 600 X 14" LG RF LWN

Noz. T1+T2
X-7430-81482

HEAT NUMBER:
B847

MATERIAL TYPE:
SA105N ✓

Material Origin:
USA ✓

Manufactured in
USA ✓

I.A.W. ASME 2010 ED.

CHEMICAL ANALYSIS

C	.210 ✓
Mn	1.230 ✓
P	.0090 ✓
S	.0130 ✓
Si	.230 ✓
Cr	.080 ✓
Mo	.030 ✓
V	.050 ✓
Cu	.160 ✓
Ni	.060 ✓
Cb	.002

PHYSICAL PROPERTIES

Yield PSI	55,700 ✓
Tensile PSI	79,600 ✓
Elongation	30 ✓
Reduction of Area	67 ✓
Hardness	163 HBW ✓

Al .024

C E .46

VERIFIED BY

JUL 11 2011

EEC QC DEPT

G. Patterson

Heat Treatment
Temperature
Time at Temperature
Cooling Media

NORMALIZED
1650 °F
1/2 HR/IN THK MIN
AIR

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 6/26/12

We hereby certify that all test results and process information contained herein are correct and true as contained in the records of the company.

Prepared by

Name: Helen Fielder

Title: QA Representative

Reviewed / Accepted
Reviewed / Accepted
I.Q.S. #3

William Bronaugh



Material Test Report

Heat Code: C855AN

ISO 9001:2008 Certified

This MTR applies to your

PO#

An Ameri-Forge Group Company

2525 De Soto Houston, TX 77091

Sales: (713) 868-4421 Fax: (713) 455-8366

Progressive Supply	PO: 57063-12	Sales Order: 97178	Line: 1
Attn: Accounts Payable	Item Code: lwn020600120a002a1	Qty Shipped: 10	
P.O. Box 470748	Item Desc: LWN, SA105N, 600#, 2 x 12", RF&D		
Tulsa, OK 74147	Supplier: STEEL DYNAMICS INC	Supplier Heat: A110108	

Spec: ASME SA105N, 2007 Edition, 2009 Addenda

Element	(%wt)	Ladle	Product	EPCRA	CAS#	Element	(%wt)	Ladle	Product	EPCRA	CAS#
C	Carbon	0.19 ✓				Cb	Columbium	0.000 ✓			
Mn	Manganese	1.13 ✓			7439-96-5	Sn	Tin	0.009			
P	Phosphorous	0.008 ✓				Al	Aluminum	0.031			
S	Sulphur	0.003 ✓				N	Nitrogen	0.0058			
Si	Silicon	0.24 ✓				As	Arsenic	0.004			7440-38-2
Cu	Copper	0.18 ✓			7440-50-8	Sb	Antimony	0.002			7440-36-0
Ni	Nickel	0.08 ✓			7440-02-0	CE	C+Mn/6+(Cr+Mo+V)/5	0.43			
Cr	Chromium	0.13 ✓			7440-47-3	Cu+Ni+Cr+Mo		0.42			
Mo	Molybdenum	0.03 ✓				Cr+Mo		0.11			
V	Vanadium	0.03 ✓									

Mechanical Testing		Other	
HBW	149 ✓	Country of Origin	USA ✓
Elg (%)	32.0 ✓	Manufactured In	USA ✓
RA (%)	68.0 ✓	Production Method	EAF
Tensile (ksi)	77.687 ✓	EF	YES
Yield (ksi)	44.811 ✓	VD	YES
Charpy Temp (F)		Fully Killed	YES
		Reduction Ratio (Mill) x:1	14.9:1
		Made to Fine Grain Practice	YES ✓
Heat Treatment	Heat Treat NORMALIZED ✓		

VERIFIED BY
AUG 05 2011
EEC QC DEPT
L. J. Johnson

NACE MR0175 & MR0103 LATEST EDITION. CE=C+(Mn/6)+((Cr+Mo+V)/5)+((Ni+Cu)/15), Elongation in 2" round specimen.

FVC STANDARD MANUFACTURING PRACTICES:

1) FLANGE DIMENSIONS & BOLTING COMPLY - ASME B16.5

2) SELF-REINFORCING NOZZLES COMPLY WITH SPECIFICATION OF SECTION VIII DIV. 1 OR DIV. 2 PER CUSTOMER DESIGN/FVC DESIGN

3) MATERIAL SPECIFICATION COMPLIES WITH ASME SECT. II PART A

4) ALL FVC MATERIAL MANUFACTURED PER FINE GRAIN PRACTICE

5) ALL FVC MATERIAL CERTIFIED PER EN 10204, 3.1.B UNLESS OTHERWISE SPECIFIED

6) CERTIFICATE OF INSURANCE AVAILABLE UPON REQUEST

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 8/12/11

EPCRA Supplier Notification: This product may contain one or more toxic chemicals subject to the reporting requirements of Section 313 of the Emergency Planning and Community Right-to-Know Act (Title III of the Superfund Amendments and Reauthorization Act of 1996) and 40 C.F.R. Part 372. Potentially reportable chemicals are indicated with a checkmark in the "EPCRA" column and a Chemical Abstract Services (CAS) registry number is provided for each such chemical in addition to the percent by weight of the chemical present in this product. It is your responsibility alone to determine whether your facility is required to submit a Toxic Release Inventory Report under EPCRA Section 313.

Certification No.: 1006739

Certification Date: 7/29/2011

Issued By: Stephanie Kobs

This report is issued in compliance with the requirements of EN10204 3.1 / ISO 10474 3.1.b

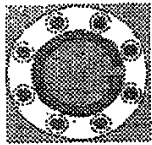
Reviewed / Accepted

I.Q.S. #3

William Brown

Puneet Sagar
Puneet Sagar - Plant Metallurgist

MM187157



GALPER, INC.
160 Southbelt Industrial Drive
Houston, Texas 77047
PH. 713-433-0700 - FAX 713-433-6680
Email: galper@galper-inc.com

PROGRESSIVE SUPPLY

**P. O. BOX 470748
TULSA OK 74145**

This MTR applies to your

PO# 1221

Part #3

TEST/CERTIFICATE EN 10204 INTERNAL JOB
3.1B 111106

M.T. CERTIFICATE N. 002929/B DATE 04/01/2011 YOUR P.O. 119520 DATE 03/25/2011
X-7930-83D + 84D

ITEM	DESCRIPTION	QUANTITY	B/P	MATERIAL	HEAT N°	#
037/037	3" 150 BL RF A105 B1 F	25	B	ASTM A/SA105 03c	3021550	A
040/040	4" 300 BL RF A105 B1 F	20	B	ASTM A/SA105 03c	3019786	B
041/041	6" 300 BL RF A105 B1 F	20	B	ASTM A/SA105 03c	101952N/02	C
042/042	2" 600 BL RF A105 B1 F	258	A	ASTM A/SA105 03c	3021551	D

Noz. V1+D1

#	C %	MN %	SI %	P %	S %	CR %	NI %	MO %	CU %	V %	SN %	AL %	NE %	TI %	N %	CB %	FL %
A	0.200	1.070	0.250	0.009	0.016	0.070	0.080	0.020	0.210	0.002			0.001			0.001	0.41
A C	0.190	1.090	0.270	0.012	0.019	0.080	0.090	0.010	0.220	0.002			0.001			0.001	0.41
B	0.190	1.030	0.240	0.005	0.015	0.050	0.090	0.025	0.180	0.002		0.002	0.001			0.001	
B C	0.180	1.050	0.220	0.002	0.014	0.040	0.100	0.035	0.190	0.002		0.005	0.001			0.001	
C	0.180	1.180	0.190	0.010	0.004	0.100	0.090	0.030	0.200	0.017		0.026	0.002			0.002	0.42
C C	0.170	1.160	0.170	0.007	0.001	0.090	0.100	0.040	0.210	0.012		0.027	0.002			0.002	0.41
D	0.210	1.050	0.240	0.008	0.019	0.070	0.080	0.030	0.220	0.002		0.002	0.001			0.001	0.42
D C	0.200	1.030	0.260	0.011	0.022	0.060	0.090	0.020	0.230	0.002		0.004	0.001			0.001	0.40

NOTES
FL=Carbon Equivalent Long Formula

C = CHECK ANALYSIS

#	TENSILE										CHARPY TEST		
	TYPE	Ø DIAMETER mm.	AREA mm²	LENGHT mm.	TEMP. F	TENSILE PSI	YIELD PSI	ELONG %	REDUCT. %	TYPE	TEMP.	VALUES	HB HARDNESS (AVERAGE)
A	S	12.50	122.70	50.00	68	70,000	36,000	22.0	30.0				187
A O		12.50	122.70	50.00	68	78,735	47,993	28.0	68.0				150
B	S	12.50	122.70	50.00	68	70,000	36,000	22.0	30.0				187
B O		12.50	122.70	50.00	68	77,641	47,567	28.0	67.2				158
C	S	12.50	122.70	50.00	68	70,000	36,000	22.0	30.0				187
C O		12.50	122.70	50.00	68	77,992	49,358	28.0	66.0				150
D	S	12.50	122.70	50.00	68	70,000	36,000	22.0	30.0				187
D O		12.50	122.70	50.00	68	78,075	46,845	31.0	68.9				157

NOTES

O = OBTAINED
S = STANDARD

#	HEAT TREATMENTS	GENERAL NOTES
A	Normalized at 900 dgr.C for 1 h.-Cooling from 900 dgr.C in still air	ROUGHNESS F - STOCK FINIS' '50 microinch
B	Normalized at 900 dgr.C for 1.1/2 h.-Cooling from 900 dgr.C in still air	INSPECTION DEPARTMENT
C	Normalized at 900 dgr.C for 1.1/2 h.-Cooling from 900 dgr.C in still air	VERIFIED BY REVIEWED STANDARD B1 - ASME B16.5 JUN 16 2011
D	Normalized at 900 dgr.C for 1 h.-Cooling from 900 dgr.C in still air	WITNESSED ☐ DATE: <i>6/16/11</i>

NOTES
Material I.A.W. Nace MR-0175-2003 COUNTRY OF ORIGIN: USA

EEC QC DEPT

TRADE MARK / LOGO
Stamped on product  INT. INSPECT DATE 04/01/2011 INT. INSPECTOR D.RUZICKA

INSPECTION AUTHORITY

Reviewed / Accepted
I.Q.S. #3

William Bronaugh

GALPER, INC

An ISO 9001/2008 certified company.
Certification issued by:
Lloyds register quality assurance
Certificate No. UQA 0110391

MM187157



Material Test Report

Heat Code: JFS

ISO 9001:2008 Certified

An Ameri-Forge Group Company

13770 Industrial Rd. Houston, TX 77015

Sales: (713) 865-4421 Fax: (713) 455-8366

Part #3

Progressive Supply Inc. PO Box 470748 Tulsa, OK 74147-0748	PO: 119532 Item Code: 0151600102-0020F Item Desc: FLG 06.00 0150 WN RF XH Supplier: CMC	Sales Order: 94151 Line: 10 Qty Shipped: 104 Supplier Heat: 3021470
--	--	--

Spec: ASTM A105/A105M-(10)/ASME SA 105/SA 105M-(08a) Section II Part A

Element	(%wt)	Ladle	Product	EPCRA	CAS#	Element	(%wt)	Ladle	Product	EPCRA	CAS#
C	Carbon	0.20 ✓				Cr	Chromium	0.07 ✓		✓	7440-47-3
Mn	Manganese	1.04 ✓		7439-96-5		Mo	Molybdenum	0.02 ✓			
P	Phosphorous	0.010 ✓				V	Vanadium	0.003 ✓			
S	Sulphur	0.020 ✓				Cb	Columbium	0.001 ✓			
Si	silicon	0.24 ✓				C.B.		0.41			
Cu	Copper	0.23 ✓		7440-50-8		CuNiCrMo		0.401			
Ni	Nickel	0.08 ✓		7440-02-0		CrMo		0.091			

X-7930-71 Noz. 51

Mechanical Testing		Other	
Test Lab	APG	MILL	CMC-TEXAS ✓
Test Bar Size	Test Piece	MHC	3021470
RBW	156 - 156 ✓	Country of Origin	USA (US) ✓
Elg (%)	27 ✓		
RA (%)	55 ✓		
Tensile Specimen Size (in)	.497		
Tensile (ksi)	78.4 ✓		
Yield (ksi)	48.6 ✓		
Gauge Length	2		

This MTR applies to your
PO# 1221

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 6/26/12

No weld repair performed. Chemical Analysis results shown are actual. Forgings are capable of passing hydrostatic test compatible with the appropriate rating. Elongation taken from a round specimen. All material supplied under this order is certified to be free of mercury contamination and no mercury bearing equipment was used in manufacturing, fabrication or testing. Yield strength was determined using the 0.2% offset method. No weld repair performed on this product. Product compliant with NACE MR0175, latest edition and dimensions to ASME B16.5

EPCRA Supplier Notification: This product may contain one or more toxic chemicals subject to the reporting requirements of Section 313 of the Emergency Planning and Community Right-to-Know Act (Title III of the Superfund Amendments and Reauthorization Act of 1986) and 40 C.F.R. Part 372. Potentially reportable chemicals are indicated with a checkmark in the "EPCRA" column and a Chemical Abstract Service (CAS) registry number is provided for each such chemical in addition to the percent by weight of the chemical present in this product. It is your responsibility alone to determine whether your facility is required to submit a Toxic Release Inventory Report under EPCRA Section 313.

JUN 16 2011

Reviewed / Accepted
I.Q.S. #3

EEC QC DEPT

William Bronaugh

Certification No.: 205991

Certification Date: 4/20/2011

L. Jatterson

Nicholas Tepovich

This report is issued in compliance with the requirements of EN10204 3.1 / ISO 10474 3.1.b

Nicholas Tepovich - Metallurgic Lab Manager

MM187157

Part #3

CUSTOMER ORDER NUMBER 119533
SOLD/SHIPPED TO PROGRESSIVE SUPPLY
P.O. BOX 470748

This MTR applies to your

PO# 1221

TULSA

OK 74147

USA

Item Quantity Description

5 5 2" X 150 X 12" LG RF LWN

X-7930-72

Noz. 52

HEAT NUMBER:
G136

MATERIAL TYPE:
SA105

Material Origin: Manufactured in
ITALY ✓ USA ✓
I.A.W. ASME 2010 ED.

CHEMICAL ANALYSIS

PHYSICAL PROPERTIES

C .160 ✓
Mn 1.220 ✓
P .0130 ✓
S .0060 ✓
Si .220 ✓
Cr .200 ✓
Mo .005 ✓
V .004 ✓
Cu .036 ✓
Ni .015 ✓
Cb .003 ✓
Sn .002

Yield PSI 46,992 ✓
Tensile PSI 76,623 ✓
Elongation 37.1 ✓
Reduction of Area 71.8 ✓
Hardness 150 HBW ✓

Ti .0170
Al .025

C E .41

VERIFIED BY

JUN 16 2011

EEC QC DEPT

INSPECTION DEPARTMENT

REVIEWED

WITNESSED ☐ DATE: *6/2/11*

Heat Treatment AS FORGED ✓
Temperature
Time at Temperature
Cooling Media

[Signature]

We hereby certify that all test results and process information contained herein are correct and true as contained in the records of the company.

Prepared by

Name: Helen Fielder

Title: QA Representative

Reviewed / Accepted
I.Q.S. # 3

William Brenaugh



UNITED STATES STEEL

TUBULAR PRODUCTS

DATE: 02/04/11
TIME: 11:04:35
SERIAL NO: F062922

CERTIFIED TEST REPORT

(IN ACCORDANCE WITH ISO 9047/EN10246/DIN50048 "type 3.1")

MILL ORDER ITEM NO. DR00486 01	SHIPPER'S NO.	P.O. NUMBER D1721000	O.D. 6.625 (168.275)		WALL 0.432 (10.972)		I.D. (mm)							
MATERIAL COND: AS-ROLLED		MIN COLLAPSE		CHAMPY V-NOTCH IMPACT TESTING FT/LBS		I.D. (mm)								
PRODUCT IDENTIFICATION X22424	FLAT	BEND	GRAIN SIZE	DR	TEST LOC.	TEMP	SIZE	TEST COND.	1	2	3	AVG	% SHEAR	
	OK					DEG F			12	12	12	15		
						T B + 32	3/4	AR	27	26	20	24	10	10
** END OF DATA THIS SHEET **														
LEGEND L - LONGITUDINAL T - TRANSVERSE B - BODY W - WELD HAZ - HEAT AFFECTED ZONE														
TESTING / INSPECTION INFORMATION														
RESULTS / COMMENTS														
FULL LENGTH VISUAL X														
FULL LENGTH EW X														
FULL LENGTH MPI														
END AREA INSPECTION (FLAM END)														
SPECIAL END AREA (SEA) INSP														
FULL LENGTH DRIFT														
ADDITIONAL NOTES/COMMENTS														
ALL MELTING AND MANUFACTURING TOOK PLACE IN THE USA. MANUFACTURED IN AN ISO 9001 CERTIFIED FACILITY - CERTIFICATE #30727. NO REPAIRS BY WELDING. NO MERCURY OR MERCURY COMPOUNDS ARE ADDED TO THE STEEL AND ALL MERCURY BEARING EQUIPMENT IS PROTECTED BY A DOUBLE BOUNDARY OF CONTAINMENT. *NOTE A SEE ATTACHED REPORT FOR TENSILE RESULTS. ** END OF DATA **														

THIS IS TO CERTIFY THAT THE PRODUCT DESCRIBED HEREIN WAS MANUFACTURED, SAMPLED, TESTED AND/OR INSPECTED IN ACCORDANCE WITH THE SPECIFICATION AND FULFILLS THE REQUIREMENTS IN SUCH RESPECTS.

PREPARED BY THE OFFICE OF:

J. MAJERZAK - MANAGER, Q.A.

DATE 02/04/11

INSPECTION DEPARTMENT

REVIEWED

WITNESSED DATE: 2/26/12

Reviewed / Accepted
I.Q.S. #3

William Brownough

PAGE 2 OF 2

MM187157

Part #4



UNITED STATES STEEL

TUBULAR PRODUCTS
TENSILE TEST REPORT

DATE: 02/04/11
TIME: 11:04:51
PAGE: 1

MILL ORDER/ITEM NO. DR00486 01	SHIPPER'S NO.	P.O. NUMBER D1721000	HEAT	SERIAL NUMBER: F0062922
BOLD TO ADDRESS PROGRESSIVE SUPPLY, INC. 7615 E. 42 ND. PL. TULSA, OK. 74145		VENDOR USS TUBULAR PRODUCTS USS FAIRFIELD WORKS P.O. BOX 599 FAIRFIELD ALABAMA 35064		

TYPE /		DIR /		TEST		TENSILE		Y/T		ELONG %		REDUC	
HEAT	PIPE / LOT		LOC	COND	YIELD	EXT%							
X22424 2013	STRIP/L/B	AR		49,800	0.50	75,500	0.66	38.3					
X22424 2012	STRIP/L/B	AR		51,000	0.50	75,500	0.68	40.0					
X22424 2011	STRIP/L/B	AR		51,500	0.50	76,000	0.68	43.0					

Part #4

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 6/26/12

Reviewed / Accepted
I.Q.S. #3
William Brennaugh

09/19/2011 From: AMERICAN ALLOY STEEL

To: ENERGY EXCHANGERS

P.O.# 1346

S.O.# :396462

AA PL#:5909370

Item :7 (1 PC) 3/4" X 60" X 96"

:TAG:

X-7930-12

Part #5

TEST CERTIFICATE

SHIP TO: ARCELORMITTAL PLATE LLC

AMERICAN ALLOY STEEL
6230 N HOUSTON ROSSLYN RD
NORTH HOUSTON TX 77091PAGE NO: 01 OF 02
FILE NO: 0284-01-32
MILL ORDER NO: 36071-002
MELT NO: R4137
SLAB NO: 11E
DATE: 01/16/10

SOLD TO:

AMERICAN ALLOY STEEL, INC
P. O. BOX 40469
HOUSTON TX 77240-0469

SEND TO:

01-C

PLATE DIMENSIONS / DESCRIPTION

TOTAL QTY	GAUGE	WIDTH	LENGTH	DESCRIPTION	PIECE WEIGHT
1	.75"	75"	480"	RECTANGLE	7657#

BHN 159 TO 166
CERTIFIED BY
AMERICAN ALLOY STEEL
BY LMS DATE 9-19

CUSTOMER INFORMATION

CUSTOMER PO: 80702

SPECIFICATION(S)

THIS MATERIAL HAS BEEN MANUFACTURED AND TESTED IN ACCORDANCE WITH PURCHASE ORDER REQUIREMENTS AND SPECIFICATION(S).

AM ALLOY-TUF-37 REV 8 YR 06

ASME SA516 GR 60

ASME SA516 ED 04 GRADES 60/65/70 06 ADDENDA

THE MANAGEMENT SYSTEMS FOR MANUFACTURE OF THIS PRODUCT ARE CERTIFIED TO ISO 9001:2000 (CERTIFICATE NO. 30130) AND ISO 14001 (CERTIFICATE NO. 006928).

CHEMICAL COMPOSITION

MELT	C	MN	P	S	CU	SI	NI	CR	MO
MELT:R4137	.19	1.09	.006	.001	.06	.35	.04	.04	.01
MELT	V	TI	B	AL	CB	SB	AS	SN	CEF
MELT:R4137	.001	.003	.0007	.033	.001	.0010	.0020	.004	.39

INSPECTION DEPARTMENT

REVIEWED

WITNESSED

DATE: 9/19/10

CARBON EQUIVALENT FORMULA (CEF)

CEF = C + (MN * .1667) + ((CR + MO + V) * .2000) + ((CU + NI) * .0667)

MANUFACTURE

FINELINE - VACUUM DEGASSED - MCQUAID-EHN GRAIN SIZE PER E112 - 7-8

HEAT TREAT CONDITION

MATL OR TEST	HEAT TREAT DESCRIPTION	NOM TEMP	HOLD MINS	COOL MTHD
PL/TEST	NORMALIZE	1650F	28	AIR COOL

VERIFIED BY
SEP 21 2011
EEC OR DEPTAMERICAN ALLOY
STEEL
6230 N HOUSTON
ROSSLYN RD
NORTH HOUSTON TX 77091

WE HEREBY CERTIFY THE ABOVE INFORMATION IS CORRECT:

ARCELORMITTAL PLATE LLC
QUALITY ASSURANCE LABORATORY
139 MODENA ROAD
COATESVILLE, PA 19320

AMERICAN ALLOY STEEL

Reviewed By:

D. Stukho

Elinore Zaplitny

SUPERVISOR - TEST REPORTING
ELINORE ZAPLITNYReviewed / Accepted
I.Q.S. #3

William Brunaugh

MM187157

09/19/2011 From: AMERICAN ALLOY STEEL

To: ENERGY EXCHANGERS

P.O.# :1346

S.O.# :396462

AA PI# 5909370

Item :7 (1 PC) 3/4" X 60" X 96"

:TAG: X-7994 & 95 LN 15B

Part #5

TEST CERTIFICATE

PAGE NO: 02 OF 02
 FILE NO: 0284-01-32
 MILL ORDER NO: 36071-002
 MELT NO: R4137
 SLAB NO: 11B
 DATE: 01/16/10

TENSILE PROPERTIES

SLAB NO.	LOC	DIR	YIELD STRENGTH PSI X 100	TENSILE STRENGTH PSI X 100	ELONGATION GAGE LGTH %	%R.A.
11B	BOT.	TRANS.	485	739	8.00" 28.0	64.0

GENERAL INFORMATION

ALL STEEL HAS BEEN MELTED AND MANUFACTURED IN THE U.S.A.
 MATERIAL HAS BEEN VACUUM DEGASSED AND CALCIUM TREATED
 FOR SULFIDE SHAPE CONTROL.
 FINELINE MOD FOR SULPHUR
 TEST CERTS. ARE PREPARED IN ACCORD. WITH PROCEDURES
 OUTLINED IN EN 10204:2004 TYPE 3.1.

B/L #01202 UMP 63044

INSPECTION DEPARTMENT
 REVIEWED
 WITNESSED ☐ DATE 1/16/10

Reviewed By:
 Elinore Zaplitny

WE HEREBY CERTIFY THE ABOVE
 INFORMATION IS CORRECT:

ARCELORMITTAL PLATE LLC
 QUALITY ASSURANCE LABORATORY
 139 MODENA ROAD
 COATESVILLE, PA 19320

Elinore Zaplitny
 SUPERVISOR - TEST REPORTING
 ELINORE ZAPLITNY

Reviewed / Accepted
 I.Q.S. #3

William Bronaugh

MM187157

DATE: 01/05/11
TIME: 04:06:47
SERIAL NO: 10034428

UNITED STATES STEEL
TUBULAR PRODUCTS
CERTIFIED TEST REPORT

(IN ACCORDANCE WITH ISO 10474EM10204DIN5049 "Type 3.1")

MILL ORDERED NO DR49778 01	SHIPPER'S NO. R83114	P.O. NUMBER 6019	VENUE/LO 178380
SOLD TO ADDRESS PROGRESSIVE SUPPLY, INC. 7815 E. 42 ND. PL. TULSA, OK. 74145		MAIL TO ADDRESS This MTR applies to your PO# _____	
VENDOR USS TUBULAR PRODUCTS 2199 EAST 28TH ST. LORAIN, OH 44055			

SPECIFICATION AND GRADE

PIPE CARBON SMLS STD PIPE API 5L-44TH ED DTD OCT 2007 AND ISO 3183:2007 MOD PSL-2 GRADE B AND GRADE X42 R N OR Q ASTM A53-07 ASTM A106-08 GRADE B QUAD STENCIL SPECIAL OD TOLERANCE ASME SA53-*2010 EDITION ASME SA106-*2010 EDITION GRADE B BLK REG MILL COAT PE BEV 30 DEG MEETING ALL THE APPLICABLE REQUIREMENTS OF NACE STANDARD MR-01-75 *2003/COR.1:2005 AND MR0103-2007

X-7930-15

MATERIAL COND:	AS ROLLED	O.D. 22.000 (558.800)		I.D. 19.375 (9.525)		WALL THICKNESS		ELONG %		HARDNESS		MIN HYDRO	
		PSI		TENSILE		YIELD		EXT %		SCALE: HRS		PSI	
PRODUCT IDENTIFICATION	TEST TYPE/ ORIENTATION	TEST COND.	GAUGE WIDTH	IN	AR	MIN	MAX	MIN	MAX	MIN	MAX	MIN	MAX
MA2050 S212AA	STRIP/L/B	AR	1.500	1.500	55000	55000	55000	50	50	78500	78500	1290	1290
MA2051 S213AA	STRIP/L/B	AR	1.500	1.500	57000	57000	57000	50	50	78000	78000	1290	1290
						** END OF DATA THIS SHEET **							

LEGEND: L-LONGITUDINAL U-UPSET T-TRANSVERSE NM-NORMALIZED QT-QUENCH & TEMPERED SR-STRESS RELIEVED AR-AS ROLLED TR-THERMO-MECHANICAL ROLLED B-BODY W-WELD

PRODUCT IDENTIFICATION	TYPE	B-BODY										W-WELD									
		CE	EL	FL	FR	GA	HA	HE	HO	HU	HY	CE	EL	FL	FR	GA	HA	HE	HO	HU	HY
MA2050	HEAT	19	21	105	011	004	19	14	105	010	004	19	14	105	010	004	19	14	105	010	004
MA2050 S212AA	PROD	19	21	105	011	004	19	14	105	010	004	19	14	105	010	004	19	14	105	010	004
MA2050 S212AA	PROD	19	21	105	011	004	19	14	105	010	004	19	14	105	010	004	19	14	105	010	004
MA2051	HEAT	19	21	105	009	002	19	13	105	009	002	19	13	105	009	002	19	13	105	009	002
MA2051 S213AA	PROD	19	21	105	009	004	20	14	105	009	004	20	14	105	009	004	20	14	105	009	004
MA2051 S213AA	PROD	19	21	102	008	004	19	13	106	008	004	19	13	106	008	004	19	13	106	008	004
		** END OF DATA THIS SHEET **																			

VERIFIED BY

CE=C+MN/6+ (CR+MO+V)/5+ (NI+CU)/15

JUL 11 2011 DECIMAL PC 3 FOR ELEMENTS ARE INDICATED BY THE LEFT MARGIN, VERTICAL DOTTED LINE OR DECIMAL POINT.

INSPECTION DEPARTMENT

EEC QC DEPT

REVIEWED

WITNESSED

DATE: 6/26/12

Reviewed / Accepted

I.Q.S.# 3

William Brennaugh



UNITED STATES STEEL

TUBULAR PRODUCTS

CERTIFIED TEST REPORT

(IN ACCORDANCE WITH ISO 10474/EN10204/DIN5048 "Type 3.1")

DATE: 01/05/11
TIME: 04:06:47
SERIAL NO: L0034428

BILL ORDER ITEM NO DR49778 01		SHIPPER'S NO. R03114		P.O. NUMBER 6019		O.D. 22.000 (558.800)		WALL 0.375 (9.525)		I.D. (mm)		I.D. (in)																											
MATERIAL COND: A5 ROLLED		FLAT		BEND		GRAIN SIZE		MIN COLLAPSE		DIR		TEST LOC.		TEMP		SIZE		TEST COND.		CHARPY V-NOTCH IMPACT TESTING FILLERS		1		2		3		AVG		1		2		3		AVG		% SHEAR	
PRODUCT IDENTIFICATION MA2050 S212AA MA2051 S213AA		OK OK						**		T B T B		+ 32 + 32		2/3 2/3		AR AR		82 81		80 90		85 89		100 100		100 100		100 100		100 100		100 100		100 100					
END OF DATA THIS SHEET **																																							
LEGEND		L - LONGITUDINAL		T - TRANSVERSE		B - BODY		W - WELD		HAZ - HEAT AFFECTED ZONE																													
TEST / INSPECTION		YES																																					
FULL LENGTH VISUAL		X																																					
FULL LENGTH EMI		X																																					
FULL LENGTH MPI		X																																					
END AREA INSPECTION (FLAT END)		X																																					
SPECIAL END AREA (SEA) INSP		X																																					
FULL LENGTH DRIFT																																							
ADDITIONAL NOTES/COMMENTS																																							
MELTED AND MANUFACTURED IN THE USA. NO REPAIRS BY WELDING. NO MERCURY OR MERCURY COMPOUNDS ARE ADDED TO THE STEEL AND ALL MERCURY BEARING EQUIPMENT IS PROTECTED BY A DOUBLE BOUNDARY OF CONTAINMENT.																																							
PRODUCT WAS HOT ROLLED AND HOT FINISHED																																							
PIPE ALSO MEET THE REQUIREMENTS OF ASTM A106 GRADE C & ASME SA106 GRADE C																																							

THIS IS TO CERTIFY THAT THE PRODUCT DESCRIBED HEREIN WAS MANUFACTURED, SAMPLED, TESTED AND/OR INSPECTED IN ACCORDANCE WITH THE SPECIFICATION AND FULFILLS THE REQUIREMENTS IN SUCH RESPECTS.

PREPARED BY THE OFFICE OF: R. HARRIS - MANAGER, Q.A.

DATE 01/05/11

Reviewed / Accepted
I.Q.S. # 3
William Brunaugh

Part # 7

MA205122375 max

Part #8

ArceIorMittal Burns Harbor Plate

QUALITY ASSURANCE
REPORT OF TEST AND ANALYSIS

SHIPMENT NO. 803-16018	DATE SHIPPED 11-24-10	CAR OR VEHICLE NO. IHB-MCCOO-BNST	TPPX 804917	PAGE 5
---------------------------	--------------------------	--------------------------------------	-------------	-----------

S O L D T O	# 003 RYERSON PROCUREMENT CORP PO BOX 4725 NORCROSS GA 30091-4725	S H I P T O	RYERSON PROCUREMENT CORP THEIR SIDING 6434 N ERIE TULSA OK
----------------------------	--	----------------------------	---

S E R I A L N U M B E R	P A T N O	H E A T N U M B E R	N O. P C S	S I Z E A N D Q U A N T I T Y				Y I E L D P O I N T	T E N S I L E S T R E N G T H	E L O N G	R E D.
				T H I C K N E S S	W I D T H O R D I A	L E N G T H	W E I G H T				

QUALITY STEEL MELTED & MANUFACTURED IN THE U. S. A.
PLATES - ASTM A516-06 GR 70 PVQ, ASME SA516
GR 70 PVQ 2010 EDITION --- MILL
TEST PCS NORM 1650F FOR 1HR/IN
AIRCL
NO WELD REPAIR WAS PERFORMED ON BELOW PLATE(S)
TEST CERTS ARE PREPARED IN ACCORDANCE WITH PROCEDURES OUTLINED
IN EN 10204:2004-TYPE 3.1
CO# M1661579 GE 841-0659
TEST SPECIMENS LABORATORY HEAT TREATED AND YIELD STRENGTH @ .5% E.U.L.
H066332 811P02140 5 3/8 96 240 AWBD 12250 52900 75100 8 21
(M55)MFST REF#:35992
H066333 811P02140 4 3/8 96 240 AWGB 9800 53800 75400 8 23
(M55)MFST REF#:35992
H066337 811P02170 4 3/8 96 240 AWGC 9800 53700 75100 8 24
(M55)MFST REF#:35992

(1 pc.) X-7930-18 "A"

Q-QUENCH TEMPERATURE T-TEMPER TEMPERATURE N-NORMALIZE TEMPERATURE

SERIAL NUMBER	PAT NO.	HEAT NUMBER	HARD BRIN HBN	BEND	THICKNESS INCHES	TYPE	SIZE	DIR	TEST TEMP F	CHARPY IMPACT								
										ENERGY FT LBS			SHEAR(%)			LAT. EXP MILS		
										1	2	3	1	2	3	1	2	3

HEAT NUMBER	CHEMICAL ANALYSIS																LIQUID GRAIN SIZE
	C	Mn	P	S	Si	Cr	Ni	Mo	V	Ti	Al	B	Cu	N	Sn		
811P02140	.16	1.05	.020	.007	.314	.242	.16	.04	.007	.002	.002	.032	.0003	.002	.005	.005	
811P02170	.16	1.06	.013	.005	.330	.228	.18	.03	.006	.002	.003	.044	.0003	.002	.006	.006	

* 811P02140 .16 1.05 .020 .007 .314.242 .16 .04.007.002.002.032.0003 .002.005.005
811P02170 .16 1.06 .013 .005 .330.228 .18 .03.006.002.003.044.0003 .002.006.006

I certify that the above results are a true and correct copy of actual results contained in records maintained by ArceIorMittal Burns Harbor and are in full compliance with the requirements of the specification cited above. This test report cannot be altered and must be transmitted intact with any subsequent third party test reports, if required.

BHPLTRPT.TIF

SUPV. QUALITY ASSURANCE

D. W. ELWOOD PER WNK

INSPECTION DEPARTMENT

REVIEWED

WITNESSED

DATE: 6/26/12

VERIFIED BY

MAY 18 2011

EEC QC DEPT

S. Jatterson

Reviewed / Accepted
I.Q.S. #3

William Branaugh

NUCOR
PLATE MILL

P.O. Box 279
Winton, NC 27986
(252) 356-3700

Mill Test Report

Page 2



Issuing Date : 04/18/2011 BIL No. : 290884 Our Order No. : 898404 Cust Order No. : MUS-233153
Vehicle No: LW 62100 Sold To: METALS USA - SOUTH CENTRAL Ship To: METALS USA - PLATES AND SHAPES
Specification : 0.3750" x 96.000" x 480.000" 2800 N 43RD STREET EAST TRACK 747
ASTM A516 70-10/ASME SA516 70 PVQ 2010 Normalized Test MUSKOGEE, OK 74403 MUSKOGEE, OK 74401
Coupons at 1850 F

Marking :

X-7930-71B, 63, 120

Heat No	C	Mn	P	S	Si	Cu	Ni	Cr	Mo	Al(tot)	V	Nb	Ti	N	Ca	B	Sn	CEQ	PCM
1502456	0.19	1.05	0.020	0.000	0.22	0.23	0.08	0.10	0.02	0.030	0.006	0.001	0.002		0.0007	0.0001	0.010	0.41	0.27
Tensile Test																			
Plate Serial No	Pieces	Tons	Dir.	Yield	(psi)	Elongation % in 2"	Elongation % in 8"	Charpy Impacts											
								Dir.	1	(psi)	shear	2	(psi)	shear	3	(psi)	shear	Ave.	Size
1502456-03	6	14.70	T	54,000	81,000	22.2	24.0												

Part #9, 10, 11

VERIFIED BY

JUN 20 2011

EEC QC DEPT

INSPECTION DEPARTMENT

REVIEWED

WITNESSED DATE: 6/1/12

Reviewed / Accepted

I.Q.S. # 3

William Brennaugh VP

NACE MR0175 ANNEX 2.1.2 COMPLIANT

Test coupons only, normalized 60 minutes per inch of thickness at 1650 F ± 25 F. Hold 30 minutes minimum. ;

Manufactured to fully killed fine grain practice by Electric Arc Furnace. Welding or weld repair was not performed on this material. We hereby certify that the contents of this report are accurate and correct. All test results and operations performed by the material manufacturer are in compliance with the applicable specifications, including customer specifications.

Mercury has not been used in the direct manufacturing of this material. Produced as continuous cast discrete plate as-rolled, unless otherwise noted in Specification.

Yield by 0.5EU method unless otherwise specified. Ceq = C+(Mn/6)+(Cr+Mo+V/5)+(Cu+Ni/15)

Pcm = C+(Si/30)+(Mn/20)+(Cu/20)+(Nb/10)+(V/10)+(Ti/10)+58

Melted and manufactured in the USA. ISO 9001:2008 certified (#008083) by SRI Quality System Registrar (#0085-09). PED 97/23/EC 712 Annex 1, Para. 4.3 Compliant.

DIN 50049 3.1.8/EN 10204 3.1B(2004), DIN EN 10204 3.1(2006) compliant. For ABS grades only. Quality Assurance certificate 05-MMP-QA-546

T.A. Depretis

T. A. Depretis, Metallurgist

04/28/2011 10:32:37 AM

STOCK LIFTING LUGS

Load Number	Tally	Mill Order Number	P.O. Number	Part Number	Certificate Number	Date
389976	00000000417856	N-106993-003	32981		L333877-1	07/23/2011 04:48
Grade						
Order Description: A516 70, 0.5000 IN x 96.000 IN x 480.000 IN Quality Plan Description: A/SA516-70: ASTM A516-70-10/ASME SA516-70 2009 ADDENDA						
Customer:						
Sold TO: STEEL SERVICE COMPANY CLAREMORE OK						
Ship TO: STEEL SERVICE COMPANY CATOOSA OK						

Shipped Item	Heat/Slab Number	Certified By	C	Mn	P	S	Si	Cu	Ni	Cr	Mo	Ch	V	Al	Ti	N2	B	Ca	Sn	Ce
1G1767D	8117537-03 ***	8117537	0.23	1.11	0.010	0.007	0.20	0.20	0.07	0.07	0.011	0.000	0.002	0.037	0.001	0.007	0.0001	0.0031	0.007	0.45
1G1767E	8117537-03 ***	8117537	0.23	1.11	0.010	0.007	0.20	0.20	0.07	0.07	0.011	0.000	0.002	0.037	0.001	0.007	0.0001	0.0031	0.007	0.45

Shipped Item	Certified By	Heat Number	Yield ksi	Tensile ksi	X/T %	ELONGATION %			Bend OK?	Hard HB	Charpy Impacts (ft-lbf)			Shear %			Test Temp
						2" / 8"	3	Avg			1	2	3	Avg			
															Size mm	1	
1G1767D	SLG1767BTT	8117537 ***	54.5	72.7	75.0	33.7											
1G1767D	SLG1767FTT	8117537 ***	55.5	76.3	72.7	34.2											
1G1767D	SLG1767MTT	8117537 ***	52.5	72.7	72.2	33.4											
1G1767E	SLG1767BTT	8117537 ***	54.5	72.7	75.0	33.7											
1G1767E	SLG1767FTT	8117537 ***	55.5	76.3	72.7	34.2											
1G1767E	SLG1767MTT	8117537 ***	52.5	72.7	72.2	33.4											

Cut to 6 7/8" lg.

Name PIONEER

PO# 767386

Count 1

Size 1/2 X 96 X 240 A516-70

Heat# B117537-03

PIONEER STEEL INC.

DATE 2.21.12 QTY 100

PO# 1874

PART# 2000

BY

Items: 2 PCS; 6 Weight: 39205 LBS

Mercury has not come in contact with this product during the manufacturing process not has any mercury been used by the manufacturing process. Certified in accordance with EN 10204 3.1. No weld repair has been performed on this material. ISO 9001:2008 Registered, PED Certified

We hereby certify that the product described above passed all of the tests required by the specifications.

VERIFIED BY

April Pitts - QA Engineer

INSPECTION DEPARTMENT

REVIEWED

WITNESSED DATE: 6/26/12

11-23-2012

EEG QC DEPT

J. Patterson

Reviewed / Accepted

I.Q.S. #3

William Breunlich

Benteler Stahl/Rohr GmbH
Postfach 13 40
33043 Paderborn
Deutschland
Tel.: +49.5254.81-0 Fax: +49.5254.13666

BENTELER
Stahl/Rohr

ABNAHMEPRÜFZEUGNIS EN 10204-3.1
INSPECTION CERTIFICATE EN 10204-3.1
CERTIFICAT DE RECEPTION EN 10204-3.1
EN 10204:2005-01

Benteler Stahl/Rohr GmbH - Postfach 1340 - 33043 Paderborn - Deutschland
Webco Industries, Inc.
9101 West 21st Street
SAND SPRINGS, OK 74063
USA

Blatt: 1 / 6
Page: 1 / 6

Dokument-Nr.: 41-488044/001P
Document No.:
No. du document:

Kunden-Bestell-Nr.:
Purchase Order No.:
No. de commande du client:

Benteler Auftrags-Nr.:
Benteler Order No.:
No. de commande Benteler:

Versandanzzeigen-Nr.:
Dispatch Note No.:
No. d'avis d'expédition:

Produkt: NAHTLOSE STAHLROHRE
Product: SEAMLESS STEEL TUBES
Produit: TUBES D'ACIER SANS SOUDURE

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

Prüf-Nr.:
Inspection No.:
No. du certificat:

Hersteller:
Manufacturer:
Producteur:

Herstellerzeichen:
Manufacturer's brand:
Marque du producteur:

Stempel des Abnahmebeauftragten:
Stamp of the inspection representative:
Timbre du contrôleur:

Stahlschmelzungsverfahren:
Steelmaking process:
Procédé d'élaboration de l'acier:

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

ASTM-A 179-1990a, ASME SA-179, ASME Section II Part A Edition 2007

CHECKED FEB 22 2010

R. Johnson

see attachment product marking

Normalized

Pos.	Stück	Maße	INSPECTION DEPARTMENT	Länge	Gewicht	Schmelzen-Nr.	Prüfdruck	Rohr-Nr.-Gruppe	Vielfachlängen
Item	Number	Dimensions	REVIEWED	Length	Weight	Heat No.	Test pressure	Tube number group	Multiple lengths
Poste	Nombre	Dimensions	WITNESSED	Longueur	Poids	No. de coulée	Pression d'épreuve	Série de no. des tubes	Longueurs multiples
0001	318	0.750" O.D. * 0.083" MW	29 FT 1 "	9247,90	5851	181070			
0002	385	0.750" O.D. * 0.083" MW	30 FT 1 "	11581,59	7291	181070			
0003	244	0.750" O.D. * 0.083" MW	31 FT 3 "	7625,00	4815	181070			

Reviewed / Accepted
I.Q.S. # 3

William Brannagh

Benteler Stahl/Rohr GmbH
Postfach 13 40
33043 Paderborn
Deutschland
Tel.: +49.5254.81-0 Fax: +49.5254.13666

BENTELER

Stahl/Rohr

ABNAHMEPRÜFZEUGNIS EN 10204-3.1
INSPECTION CERTIFICATE EN 10204-3.1
CERTIFICAT DE RECEPTION EN 10204-3.1

Blatt: 3 / 6
Page: Page:
Page: Page:

Prüf-Nr.: 41-488044/001/P
Inspection No.:
No. du certificat:

Dokument-Nr.:
Document No.:
No. du document:

Schmelzenanalyse [%] / Heat analysis [%] / Analyse sur coulée [%]

Pos.	Schmelzen-Nr.	C	SI	MIN	P	S
Item	Heat No.					
Poste	No. de coulée					
0013	549318	0,100	0,150	0,46	0,013	0,003

Prüfergebnisse / Test results / Résultats des essais

Die Rohre sind auf Dichtheit geprüft durch:
The tubes have been submitted to a leak tightness test by:
Les tubes ont passé un contrôle d'étanchéité par:

Hydrostatic test: eddy current testing instead of hydrostatic test
PASSED

Die Rohre wurden zerstörungsfrei geprüft:
The tubes are non destructive tested:
Les tubes ont passé un essai non destructif:

ET-test: acc. to ASME SA-450, ASTM-A 450; acc. to ASTM-E 309; Imperfections
PASSED

Augsichtskontrolle:
Visual inspection:
Examen visuel:

PASSED

Aufweitversuch:
Drift expanding/flare test:
Essai d'évasement:

PASSED

Maßkontrolle:
Dimensions examination:
Vérification des dimensions:

PASSED

Ringtaillversuch:
Flattening test:
Essai d'aplatissement:

PASSED

Ergebnisse der mechanischen Prüfung / Results of mechanical testing / Résultats des essais mécaniques

Die Probenahme erfolgte an Vielfachlängen.
The sampling was carried out on multiple lengths.
L'échantillonnage était réalisé aux longueurs multiples.

Härteprüfung / Hardness test / Essai de dureté

Pos.	Proben-Nr.	Schmelzen-Nr.	Härte
Item	Specimen No.	Heat No.	Hardness
Poste	No. de l'éprouv.	No. de coulée	Dureté
Anforderungen			
Requirements			
Exigences			
0001	000001	181070	HRC
0001	000002	181070	HRC
			HB
			HV
			HRB
			HBW
			MAX 72
			064
			065

WITNESSED DATE: 7/24/13

INSPECTION DEPARTMENT

REVIEWED

Reviewed / Accepted I.Q.S. #3

William Brownagh

Part #14

Benteler Stahl/Rohr GmbH
Postfach 13 40
33043 Paderborn
Deutschland
Tel.: +49.5254.81-0 Fax: +49.5254.13666

BENTELER

Stahl/Rohr

ABNAHMEPRÜFZEUGNIS EN 10204-3.1

INSPECTION CERTIFICATE EN 10204-3.1

CERTIFICAT DE RECEPTION EN 10204-3.1

Härteprüfung / Hardness test / Essai de dureté

Dokument-Nr.:
Document No.:
No. du document:

Prüf-Nr.:
Inspection No.:
No. du certificat:

Blatt: 4 / 6
Page:

Pos.	Proben-Nr.	Schmelzen-Nr.	Härte
Item	Specimen No.	Heat No.	Hardness
Poste	No. de l'éprouv.	No. de coulée	Dureté

Anforderungen
Requirements
Exigences

HRC	HB	HV	HRB	HBW
-----	----	----	-----	-----

MAX 72

0001	000003	181070				065		
0001	000004	181070				063		
0002	000001	181070				064		
0002	000002	181070				065		
0002	000003	181070				065		
0002	000004	181070				063		
0003	000001	181070				064		
0003	000002	181070				065		
0003	000003	181070				065		
0003	000004	181070				063		
0004	000001	181069				064		
0004	000002	181069				064		
0005	000001	181069				064		
0005	000002	181069				065		
0006	000001	181073				063		
0006	000002	181073				064		
0006	000003	181073				063		
0006	000004	181073				063		
0007	000001	181073				063		
0007	000002	181073				063		
0007	000003	181073				064		
0007	000004	181073				063		
0008	000001	181073				063		

INSPECTION DEPARTMENT

REVIEWED

WITNESSED

DATE: 6/26/12

Reviewed / Accepted

I.Q.S. # 3

William Broughton

Part # 14

Benteler Stahl/Rohr GmbH
Postfach 13 40
33043 Paderborn
Deutschland
Tel.: +49.5254.81-0 Fax: +49.5254.13666

BENTELER
Stahl/Rohr

ABNAHMEPRÜFZEUGNIS EN 10204-3.1

INSPECTION CERTIFICATE EN 10204-3.1
CERTIFICAT DE RECEPTION EN 10204-3.1

Härteprüfung / Hardness test / Essai de dureté

Dokument-Nr.: 41-488044/001/P
Document No.:
No. du document:

Prüf-Nr.:
Inspection No.:
No. du certificat:

Blatt: 5 / 6
Page:

Pos.	Proben-Nr.	Schmelzen-Nr.	Härte
Item	Specimen No.	Heat No.	Hardness
Poste	No. de l'éprouv.	No. de coulée	Dureté

Anforderungen

Requirements
Exigences

HRC	HB	HV	HRB	HBW
-----	----	----	-----	-----

MAX 72

0008	000002	181073		064
------	--------	--------	--	-----

0008	000003	181073		064
------	--------	--------	--	-----

0008	000004	181073		065
------	--------	--------	--	-----

0008	000005	181073		063
------	--------	--------	--	-----

0008	000006	181073		063
------	--------	--------	--	-----

0009	000001	548853		064
------	--------	--------	--	-----

0009	000002	548853		065
------	--------	--------	--	-----

0009	000003	548853		065
------	--------	--------	--	-----

0009	000004	548853		064
------	--------	--------	--	-----

0010	000001	548853		064
------	--------	--------	--	-----

0010	000002	548853		065
------	--------	--------	--	-----

0011	000001	548853		064
------	--------	--------	--	-----

0011	000002	548853		065
------	--------	--------	--	-----

0012	000001	548853		064
------	--------	--------	--	-----

0012	000002	548853		065
------	--------	--------	--	-----

0013	000001	549318		065
------	--------	--------	--	-----

0013	000002	549318		064
------	--------	--------	--	-----

Vermerk / Remark / Remarque

Certificate remarks: Steel and tubes manufactured by Benteler Stahl / Rohr

INSPECTION DEPARTMENT
REVIEWED

WITNESSED ☐ DATE: 6/24/12

Reviewed / Accepted
I.Q.S. #3
William Brunaugh

Part #14

Benteler Stahl/Rohr GmbH
Postfach 13 40
33043 Paderborn
Deutschland
Tel.: +49 5254.81-0 Fax: +49 5254.13666

BENTELER

Stahl/Rohr

ABNAHMEPRÜFZEUGNIS EN 10204-3.1

INSPECTION CERTIFICATE EN 10204-3.1

CERTIFICAT DE RECEPTION EN 10204-3.1

Beiblatt Produktkennzeichnung / Attachment product marking / Supplément marquage du produit

Pos.	Produktkennzeichnung
Item	Produktkennzeichnung
Poste	Marquage du produit

0001, 0002, 0003, 0004, 0005, 0006, 0007, 0008, 0011, 0012

FS: BENTELER A179-SA179 HEAT-NO. DIMENSIONS TUBES-LENGTH FEET 2008 WA MADE IN GERMANY

0009, 0010

FS: BENTELER A179-SA179 HEAT-NO. DIMENSIONS TUBES-LENGTH FEET 2108 WA MADE IN GERMANY

FS: BENTELER A179-SA179 HEAT-NO. DIMENSIONS TUBES-LENGTH FEET 2408 WA MADE IN GERMANY

AEZ = Ätzlinienbeschriftung, Etching ink marking, Gravure à l'encre FK = Farbmarkenzeichnung, colour marking, marquage par couleur FS = Feilschablonierung, palm stencilling, marquage par peinture FSD = Farbschablonenrucker, Colour jet printer, Impprimante à jet d'encre de c
LS = Längsschablonierung, longitudinal stencilling, marquage longitudinal par peinture PKE = Etikettenmarkenzeichnung, tag marking, marquage sur étiquette PS = Prägestempel, die stamp, marquage par poinçonnage TS = Titensatzmarkenzeichnung, ink jet spray marking.

Verkäufer(in) / Salesman / woman in charge / Personne chargée : Mr Buerger, Tel.: 05254/81-4266, Fax: 4299

INSPECTION DEPARTMENT

REVIEWED ☒ FRED WHITE

WITNESSED ☐ DATE: 6/24/02

Reviewed / Accepted

I.Q.S. # 3

William Brannagh

WB

Part #14

Paderborn Schloß Neuhaus, 24.06.2008, TEL.: 05254.81-1767 FAX: 05254.81-1752

Abnahmebeauftragter

Inspection representative

Contrôleur

ALWIN PANKRATZ / TEM

Es wird bestätigt, daß die gelieferten Erzeugnisse den techn. Lieferbedingungen des Auftrages entsprechen. Dieses Dokument wurde mittels EDV erstellt und ist ohne Unterschrift rechtsgültig.
We certify that the supplied products comply with the order specification. This document was prepared by means of electronic data processing and is valid without signature.

Nous attestons que les produits livrés sont conformes aux stipulations de la commande. Ce document a été établi par traitement électronique de l'information et est valide sans signature.

TUBES INC.

Part #14

900 E. PECAN
SAND SPRINGS, OK 74063
918-245-5100

MANUFACTURER'S CERTIFICATE OF COMPLIANCE IN ACCORDANCE WITH EN 10204 3.1

CUSTOMER: ENERGY EXCHANGER COMPANY

CUSTOMER ORDER NO: 1200 TAG: X7930

OUR ORDER NO: T-44125-20

PRODUCT DESCRIPTION: SA179 CARBON STEEL U-BENDS
266 PCS 3/4" OD X .083 MW X V/L

CUSTOMER FURNISHED MATERIAL.

ALL U-BENDS WERE STRESS RELIEF ANNEALED @ 1150 +/- 25°F PLUS 12" PAST TANGENT
IN ACCORDANCE WITH SA-556 AND PURCHASE ORDER REQUIREMENTS. ✓

WE CERTIFY THAT THIS MATERIAL HAS BEEN MANUFACTURED, INSPECTED, AND TESTED IN
ACCORDANCE WITH THE SPECIFICATIONS TO WHICH IT WAS ORDERED, AND THAT THE ABOVE
INFORMATION IS CORRECT AS CONTAINED IN THE RECORDS OF THIS CORPORATION.

B. Turner 5/17/11

BRIAN TURNER - QUALITY
CERTIFICATION COORDINATOR

VERIFIED BY

MAY 24 2011

EEC QC DEPT

X. Jetterson

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 6/21/12

Reviewed / Accepted
I.Q.S. # 3

Officer / Technician

MM187157

DATE: 01/12/12

W. M. HEITGRAS COMPANY
P.O. BOX 2044
1316 N. OSAGE DRIVE
TULSA, OKLAHOMA 74101
(918) 583-3131

Part #15

CERTIFIED MATERIAL TEST REPORT

ENERGY EXCHANGERS
1844 N. GARNETT RD.
TULSA OK 74116

LOT # 108465
HEAT # 108465
STOCK # B7S112C912
1-1/8-8 X 9-1/8 ASTM A-193 B-7
CUS PO# 1744
ORDER # 28168

SPECIFICATIONS:

ASTM A193 B7 ALL THREAD ROD

X-7930.41

VENDOR: VULCAN THREADED PRODUCTS, INC.

QTY SOLD

48

- CHEMICAL COMPOSITION -

C %	MN %	P %	S %	SI %	NI %	CR %
00.4000	00.9000	00.0150	00.0260	00.2400	00.1030	00.8410
MO %	CU %	CO %	V %	AL %	FE %	TA %
00.1630	00.2400		00.0070	00.0010		
TI %	ZN %	SE %	CB %	W %	N %	SN %
						00.0080

- CHARPY IMPACT -

FIRST: 0 SECOND: 0 THIRD: 0 AVERAGE: 0

- MECHANICAL PROPERTIES -

TENSILE STRENGTH: 134,200 Psi
YIELD : 119,000
ELON : 20.00
RA : 60.00

HARDNESS : 27 HRC
PROOF STRESS: 0 Psi

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 1/24/12

COMMENTS:

MELTED & MFG IN THE USA
TEMPERING TEMP 1430 F
META 92/S1/S3

VERIFIED BY

JAN 17 2012

EEC QC DEPT

Reviewed / Accepted
I.Q.S. #3

William Bronaugh

W. M. HEITGRAS COMPANY

QUALITY CONTROL MANAGER

Part #16

DATE: 05/31/11

W. M. HEITGRAS COMPANY
P.O. BOX 2044
1316 N. OSAGE DRIVE
TULSA, OKLAHOMA 74101
(918) 583-3131

CERTIFIED MATERIAL TEST REPORT

X-7930-42

ENERGY EXCHANGERS
1944 N. GARNETT RD.
TULSA OK 74116

LOT # MR851
HEAT # B09364
STOCK # H2HHN112-S
1-1/8-8 ASTM A-194 2-H HEAVY
CUS PO# 1242
ORDER # 276291
TAG # STOCK

SPECIFICATIONS:

ASTM A-194 2H HEAVY HEX NUT

STOCK

VENDOR: UNYTITE, INC.

QTY SOLD

700

- CHEMICAL COMPOSITION -

C %	MN %	P %	S %	SI %	NI %	CR %
00.4600	00.7100	00.0110	00.0190	00.2300	00.0100	00.0600
MO %	CU %	CO %	V %	AL %	FE %	TA %
00.0100						
TI %	ZN %	SE %	CB %	W %	N %	SN %

- CHARPY IMPACT -

FIRST: 0 SECOND: 0 THIRD: 0 AVERAGE: 0

- MECHANICAL PROPERTIES -

TENSILE STRENGTH: 0 Psi
YIELD : 0
ELON : 0.00
RA : 0.00

HARDNESS : 28.9HRC
PROOF STRESS: 60.00 Psi
INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE: 6/26/12

COMMENTS:

HRB 102.3 HARDNESS
TEMPERING 1031 F/45M W.C.
HEAT TREAT T:MIN. 850 F
COUNTRY OF ORIGIN: U.S.A.

W.M. HEITGRAS COMPANY

VERIFIED BY
MAY 31 2011

Reviewed / Accepted
I.Q.S. #3

William Bronaugh
W

EEC QC DEPT

L. Jetterson

QUALITY CONTROL MANAGER

09/19/2011 From: AMERICAN ALLOY STEEL

To: ENERGY EXCHANGERS

P.O.# :1346

S.O.# :396462

AA PL#5109135

Item :1 (1 PC) 3/8" X 96" X 164"

TAG:

X-7930-50+51

Part # 17

ArcelorMittal Burns Harbor Plate

SHIPMENT NO. 803-08925		DATE SHIPPED 06-09-11	CAR OR VEHICLE NO. IHB-MCCOO-BNSF	IHB 018465	PAGE 8
AMERICAN ALLOY STEEL INC PO BOX 40469 HOUSTON TX 77040-0469		AMERICAN ALLOY STEEL INC BNSF TR# 7226 MILE 66.4 LN SEG 492 6230 N HOUSTON ROSSLYN RD HOUSTON TX			

S O L D T O	N O T E	SERIAL NUMBER	PAT NO.	HEAT NUMBER	NO. PCS.	SIZE AND QUANTITY				YIELD POINT	TENSILE STRENGTH	ELONG	RED.
						THICKNESS	WIDTH OR DIA.	LENGTH	WEIGHT				
						INCHES	INCHES	INCHES	POUNDS	PSI	PSI	IN	%

QUALITY STEEL MELTED & MANUFACTURED IN THE U. S. A. ✓

PLATES - ASME SA516 GR 70 PVQ 2010 EDITION,
ASME SA516 GR 65 PVQ 2010 EDITION,
ASME SA516 GR 60 PVQ 2010 EDITION,
CH-V SA2085 PLT L 15/12 FT LBS AT
-50F --- PLT NORM & COOL IN STILL
AIR --- TEST CERTS ARE PREPARED IN
ACCORD WITH PROCEDURES OUTLINED IN
EN 10204:2004 TYPE 3.1

NO WELD REPAIR WAS PERFORMED ON BELOW PLATE(S)

CO# 85354 GH 361-7984

PLATES HEAT TREATED ✓

TEST SPECIMENS ATTACHED & YIELD STRENGTH @ .5% EUL													
J031961	813862790	2	.375	96	360	7350	54300	77200	8	24			
			N	1650	DEG F	-	21	MIN					
J031960	821T00580	3	.375	96	360	11025	50200	74200	8	24			
			N	1650	DEG F	-	21	MIN					

BHN 153 TO 159 ✓
CERTIFIED BY
AMERICAN ALLOY STEEL
BY LMS DATE 9-19-11

Certified a true copy of the
original, retained in our file.
AMERICAN ALLOY STEEL
Reviewed By:

D67/12/11

O-QUENCH TEMPERATURE	T-TEMPERATURE	N-NORMALIZE TEMPERATURE
----------------------	---------------	-------------------------

SERIAL NUMBER	PAT NO.	HEAT NUMBER	HARD BHN BHN	BEND	CHARPY IMPACT														
					THICKNESS INCHES	TYPE	SIZE	DIR	TEST TEMP F	ENERGY FT LBS			SHEAR(%)			LAT. EXP			MILS
J031961		813862790			.375	V	3/4	L	-50	68	64	66							
J031960		821T00580			.375	V	3/4	L	-50	79	91	90							

INSPECTION DEPARTMENT
REVIEWED

HEAT NUMBER	CHEMICAL ANALYSIS																REVIEWED	DATE
	C	Mn	P	S	Si	Cu	Ni	Cr	Mo	V	Ti	Al	B	Co	N	Sn	GRAIN SIZE	
813862790	.17	1.06	.017	.003	.345	.229	.18	.03	.005	.002	.002	.037	.0002	.002	.004	.007		

* 821T00580	.17	1.03	.014	.005	.320	.217	.18	.03	.008	.002	.002	.030	.0002	.002	.005	.002		
-------------	-----	------	------	------	------	------	-----	-----	------	------	------	------	-------	------	------	------	--	--

VERIFIED BY

I certify that the above results are a true and correct copy of actual results contained in records maintained by ArcelorMittal Burns Harbor and are in full compliance with the requirements of the specification cited above. This test report cannot be altered and must be transmitted intact with any subsequent third party test reports, if required.

BHPLTRPT.TIF

SEP 21 2011

SUPV. QUALITY ASSURANCE

D. W. ELWOOD PER WNK

EEC QC DEPT

Reviewed / Accepted
I.Q.S. #3

William Breunhaugh

L. Jatterson

AMERICAN ALLOY
PLATE# 5109135

MM187157

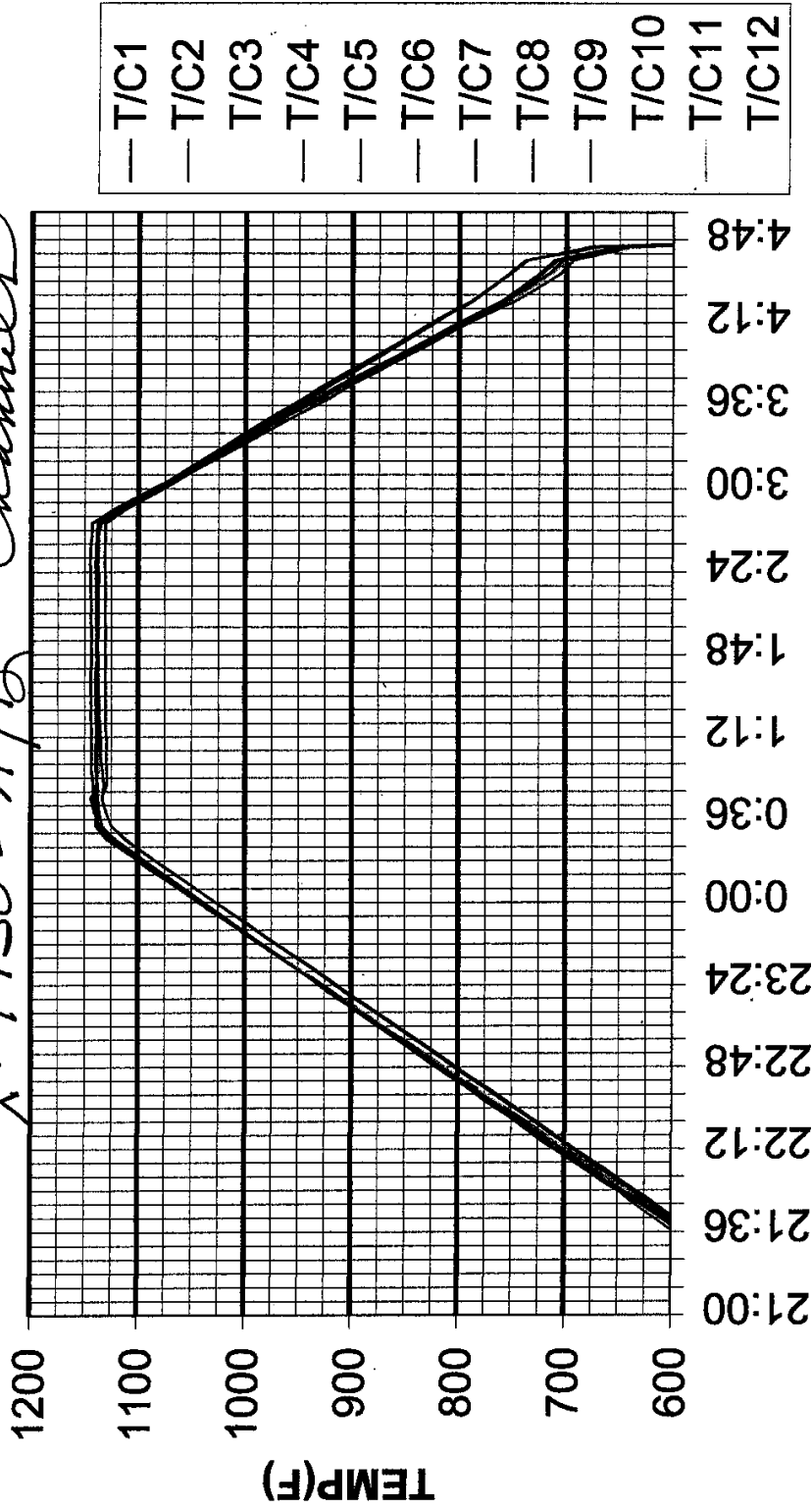
SECTION 5

6/12/12

ENERGY EXCHANGERS
JOB#54276
PO#PX 9535

BODYCOTE THERMAL PROCESSING FCE# 2001

X-7930-A/B Channels



INSPECTION REPORT

REVIEWED
CALIBRATION DATE 5/10/12
CALIBRATION DUE DATE 8/10/12

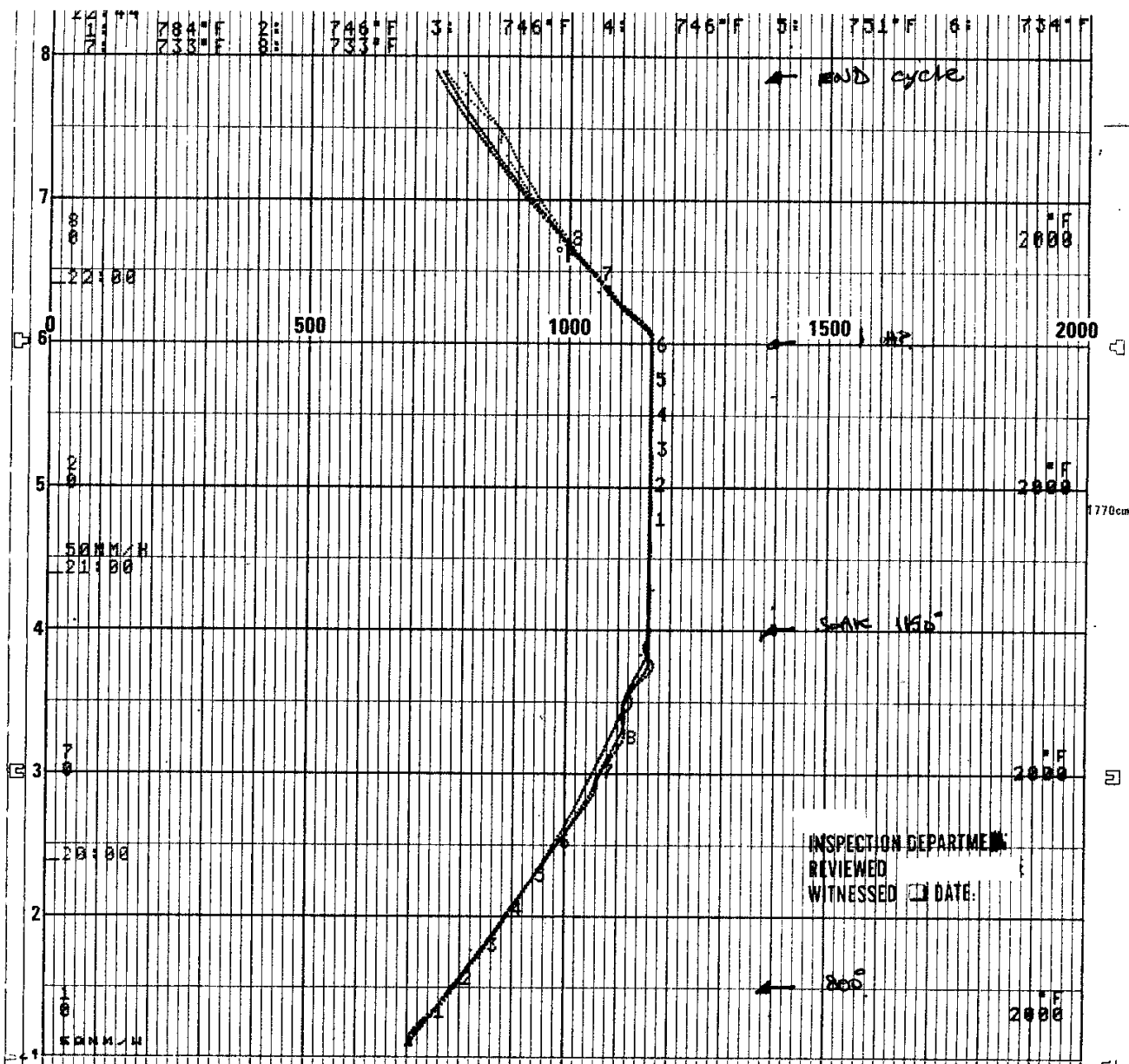
Reviewed / Accepted

I.Q.S. # 3

William B. B. 22-12

SIGNED BY CHRIS HELTON

Chris Helton



OSR

Houston (281) 422-7206
Toll Free: (888) 750-1222

Customer: Energy Ex

Location: TUSA ok

Job No: 02-2607

Date: 6-20-12

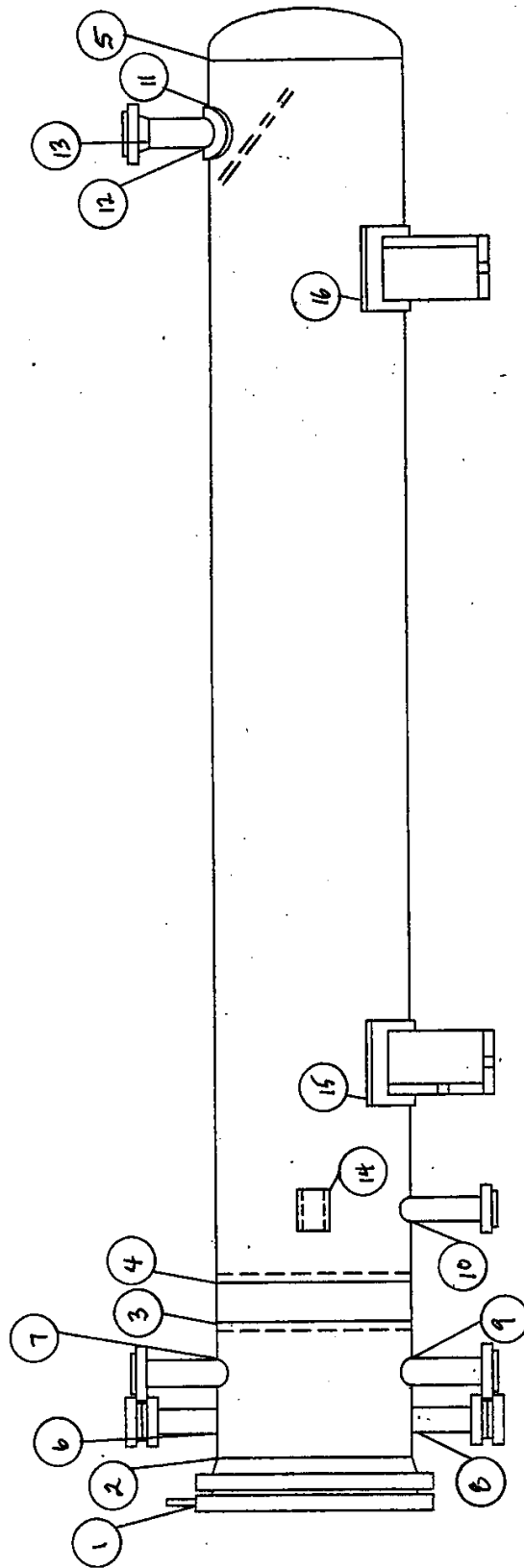
Chart Speed: 500 100 Hr

Technician: Y. BASSINE

HTS or Chart ID: 11484

Rec. No.	Weld No.	Weld Size	Schedule	Material
1-2				
3-4	x	7930-A		
5-6	x	7930-B		
7-8				
CLAN. 10 TUBESHEET WELD				

Reviewed / Accepted
I.Q.S. #3
William Brinkley
WJ 6/21/12



Reviewed / Accepted
I.Q.S. # 3
William Brennaugh

NDE/WELD MAP

X.7930A

ENERGY EXCHANGER COMPANY

CUSTOMER: SOUTHERN COMPANY SERV. P.O.#: 17496-0001

TAG: HX 1027

ENERGY JOB # X-7930 A

NDI/WELD INDEX

[illegible]

JOB # X-7930A

17496-0001

CHANNEL

SPOT

uw 51

SA 516-70

MATERIAL THICKNESS

22" K 3/4"

Q.C. WELDMENT

CODE/STANDARD:

ASME SEC. VIII, DIV. 1, A-

RADIOGRAPHIC DATA

1. RT DATE 6-7-12

2. MATERIAL EXAMINED:

() WELDMENT

() **CASTING**

() OTHER_

3. METHODS:

(4) SINGLE EXPOSURE

() MULTIPLE EXPOSURE

() DOUBLE WALL TECHNIQUE

() SINGLE WALL TECHNIQ

() DOUBLE WALL VIEWING

☐ SINGLE WALL VIEWING

() SINGLE FILM LOADING

4. IQI (PENETRAMETER) DATA:

DESIGNATION 2.4

SENSITIVITY LEVEL 2-4

LOCATION (FS) ~~(SS)~~

5. FILM DATA:

FILM TYPE 80

FILM DENSITY MAX

FILM DENSITY M.I.

6. SOURCE DATA:

ISOTOPE 192 SIZE 0.106

CURIES 89 E.T.: 29

S.O.D. 11 S.S.O.F. 5

RADIOGRAPHER

INTERPRETER

CUSTOMER INSPECTOR

readersheet(A99).doc

INSPECTION DEPARTMENT

REVIEWED

WITNESSED 1 DATE: _____

Reviewed / Accepted

I.Q.S. # 3

William Bronaugh

JOB # X-7930 A

174960001

CH

SPOT

SA 516 70

MATERIAL THICKNESS 22 x 3/4

Q.C. WELDMENT

CODE/STANDARD: ASME SEC. VIII, DIV. 1, A-

RADIOGRAPHIC DATA

1. RT DATE 6-12-12

(☒) WELDMENT
() CASTING
() OTHER _____

- ☐ SINGLE EXPOSURE
- ☐ MULTIPLE EXPOSURE
- ☐ DOUBLE WALL TECHNIQUE
- ☒ SINGLE WALL TECHNIQUE
- ☐ DOUBLE WALL VIEWING
- ☒ SINGLE WALL VIEWING
- ☒ SINGLE FILM LOADING
- ☐ DOUBLE FILM LOADING

DESIGNATION G.O 14

SENSITIVITY LEVEL 0.016

LOCATION (FS) (SS)

FILM TYPE fuji 100

FILM DENSITY MAX. 2-4

FILM DENSITY MIN. 2-4

ISOTOPE II 92 SIZE 0.149

CURIES 94 E.T. 120

S.O.D. 11/1 S.S.O.F. 3/4

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE:

RADIOGRAPHER S. Howard

INTERPRETER Sam W. III 193332

DATE REVIEWED 6-13-12

CUSTOMER INSPECTOR

~~Reviewed / Accepted~~
I.Q.S. # 3

DATE REVIEWED 6/8/12

William Brenaugh

DATE: 6-21-12

CERTIFICATION OF EXAMINATION
BY
MAGNETIC PARTICLE (DRY POWDER METHOD)
(Procedure MT-1 Rev. 6)

P.O. # 17496-0001

TAG # HX 1027

ENERGY JOB # X-7930 A

MT OF THE FOLLOWING:

LIFTING LUG WELDS

ALL TEMP ATTACHMENTS AND

ALL STRIKES

ALL NOZ BACK CUTS

ALL INT. + EXT CH WELDS

BEFORE + AFTER PWHT

This certification is made to document that all Magnetic Particle Examinations have been performed on _____ in accordance with the requirements of ASME Section VIII, Division I, Appendix VI, ASME Section V, Article 7, customer specifications and Energy Exchanger Company drawings.

TEST INSTRUMENT: ESC-Y400 / ESC MS-27D

PARTICLE TYPE & COLOR: DRY / GRAY Lot: 17746

MATERIAL AND THICKNESS: SA-106B X 3/8

LIGHTING: 100 FT CANDLES MIN. @ SURFACE

ENERGY EXCHANGER COMPANY



Brent Wilson
Quality Control Manager
ASNT NDT Level III, #193332
CWI # 10082731

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE:



Reviewed / Accepted
I.Q.S. #3
William Bronaugh

DATE: 5-29-12

CERTIFICATION OF EXAMINATION
BY
LIQUID PENETRANT - WATER WASHABLE
(Procedure PT-1 Rev. 6)

P.O. # 17496 - 0001

TAG # HX 1027

ENERGY JOB # X-7930 A

PT TUBE TO TUBESHEET
STRENGTH WELDS BEFORE
AND AFTER ROLLING

This certification is made to document that all Liquid Penetrant Examinations have been performed on X-7930 A in accordance with the requirements of ASME Section VIII, Division I, Appendix VIII, ASME Section V, Article 6, customer specifications and Energy Exchanger Company drawings.

PENETRANT: ARDROX 906

REMOVER: WATER

DEVELOPER: ARDROX 9D1B

MATERIAL AND THICKNESS: SA-266-6R 4N X 3"

LIGHTING: 100 FT CANDLES MIN. @ SURFACE

ENERGY EXCHANGER COMPANY



Brent Wilson
Quality Control Manager
ASNT NDT Level III, #193332
CWI #10082731

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE:



Reviewed / Accepted
I.Q.S. # 3

William Brennaugh

Energy Exchanger Company

BRINELL HARDNESS REPORT

JOB NO: X-7930 A

[illegible]

Reviewed / Accepted

~~I.Q.S. #3~~

William Brenaugh

INSPECTION DEPARTMENT

REVIEWED

WITNESSED ☐ DATE:

SECTION 6

DATE: 6-20-12

CERTIFICATE OF WELD/SUPPORT PAD AIR TEST

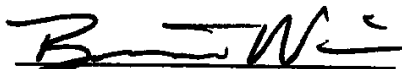
P.O. NO: 17496-0001

TAG NO: HX1027

ENERGY JOB NO: X-7930 A

This is to certify all weld/support pads on the above referenced equipment were air tested @ 15 P.S.I. and found to be satisfactory.

ENERGY EXCHANGER COMPANY



Brent Wilson
Quality Control Manager

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☒ DATE:

Reviewed / Accepted
I.Q.S. #8

William Brennaugh 6/22/12

DATE: 5-29-12

CERTIFICATE OF TUBE TO TUBESHEET AIR TEST

P.O.# 17496-0001

TAG# HX1027

ENERGY JOB # X-7930 A

This is to certify that all tube to tubesheet welds on the above referenced equipment were air tested @ 15 P.S.I. and found to be satisfactory.

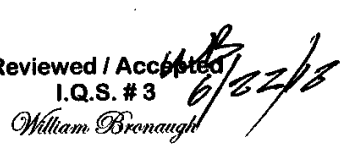
ENERGY EXCHANGER COMPANY

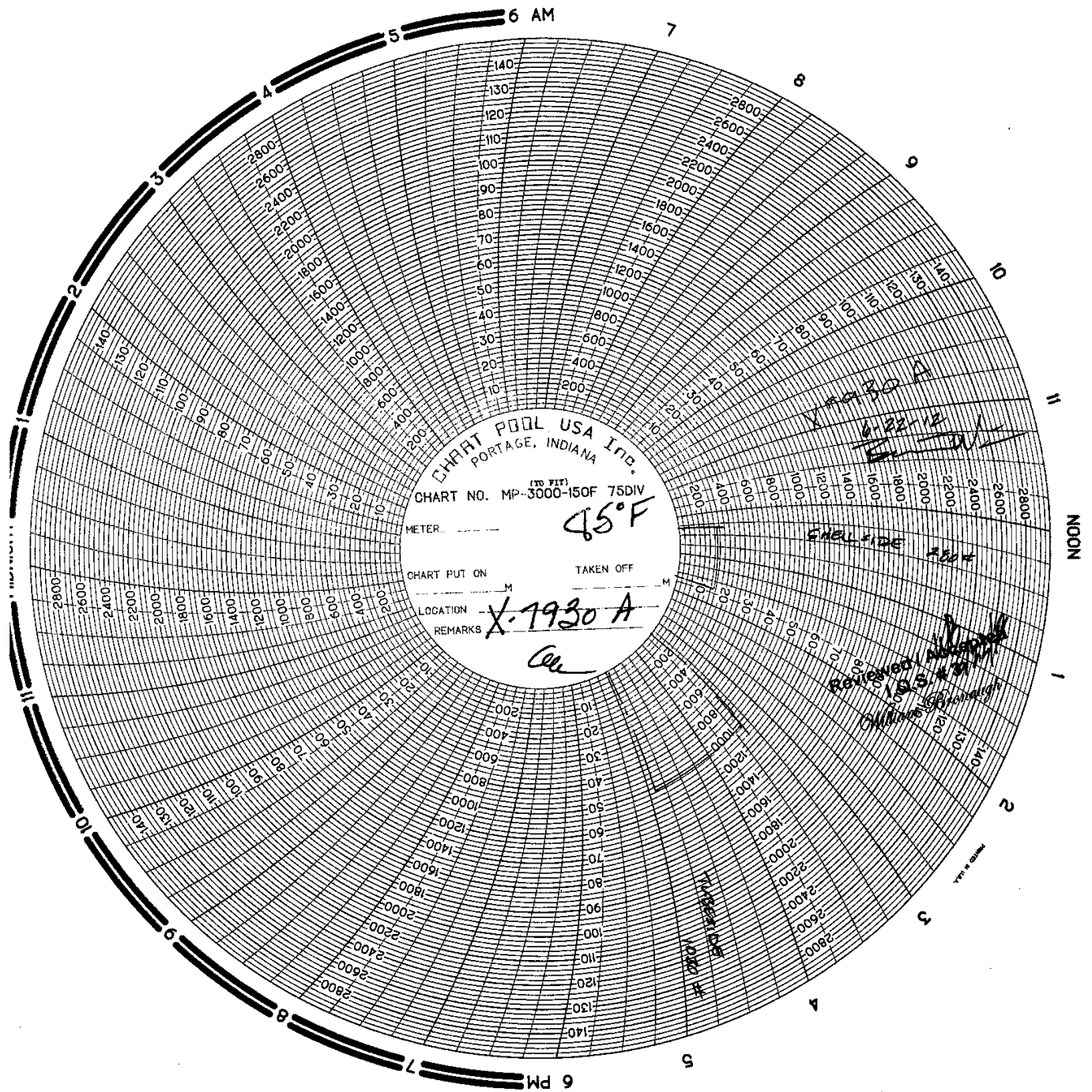


Brent Wilson
Quality Control Manager

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☒ DATE:

Reviewed / Accepted
I.Q.S. # 3


William Bronaugh



INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☒ DATE:

DATE: 6-21-12

CERTIFICATE OF HYDROSTATIC TEST

P.O.# 17496 0001

TAG# Hx 1027

ENERGY JOB # X- 7930 A

This is to certify the above referenced equipment was
hydro tested at the following pressures:

280 PSIG SHELL SIDE

1030 PSIG TUBE SIDE

Bubble Test OK

ENERGY EXCHANGER COMPANY

INSPECTION DEPARTMENT
REVIEWED
WITNESSED ☐ DATE:



Brent Wilson
Quality Control Manager

/lt

WB
6/22/12
Reviewed/ Accepted
I.Q.S. #3
William Bronaugh

Date: 6-26-12

CERTIFICATE OF NITROGEN PURGE

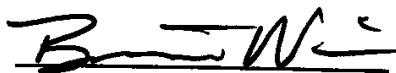
P.O. NO: 17496-0001

TAG NO: HX 1027

ENERGY JOB NO: X-7930A

This is to certify the above referenced equipment was purged
with 15 PSI dry nitrogen after hydro test.

ENERGY EXCHANGER COMPANY



Brent Wilson

Quality Control Manager

Reviewed / Accepted
I.Q.S. #3

William Bronaugh 

ENERGY EXCHANGER COMPANY

PAINT CHECK LIST

Contractor: EATON INDUSTRIAL COATINGS

Unit Serial No: X7830 A Customer Specification No: _____

Paint Required: 4-5 mils ^{CARBONINE} 450 Primer; _____ mils _____ Intermediate;
4-5 mils ^{CARBONINE} 450 Finish

Satisfactory Date

Testex PRESS-O-FILM™ HT
 www.testexape.com
 X-Coarse
 1.5 to 4.5 mil
 38 to 115 µm
 Made in USA

2.9
 (C+XC)/2

✓ WE	6/22/12	
✓ WE	6/20/12	
✓ WE		
✓ WE		

- Paint Shelf Life
 - Materials in accordance with Project Specifications & Drawings

- Notify Energy Exchanger Company

- Weather Conditions:
93 temperature; 54% humidity; 90 substrate; 74 dew point,
 EEC verify _____

- Surface Prep:
 (Req'd) SSPC-SP- 10 2-3 mils; (Actual) SSPC-SP- 10 2.7 mils

✓ WE	6/22/12	
---------	---------	--

- Surface Contamination
- Surface Imperfections
- Paint Contractor Re-check above
- Storage, Mixing, Application
- Masked Surfaces
- Check Compressed Air for Contamination
- Wet Film Thickness:
 (Req'd) _____ (Actual) _____
- Dry Film Thickness:
 (Req'd) 8-10 (Actual) 9-11
- Tie Down/Shipping Preparation

✓ WE	6/22/12	
✓ WE		
✓ WE		
✓ WE		
✓ WE		
✓ WE		
✓ WE		

✓ WE		
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✓ WE		
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2nd COAT
 TEMP 98
 S. TEMP 95
 Humidity 56%
 Dew Point 78

Reviewed / Accepted
 I.Q.S. #3
 William Bronaugh

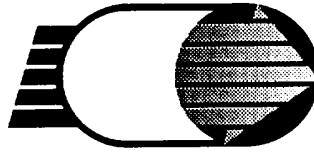
SECTION 7

ENERGY EXCHANGER COMPANY
SPARE PARTS LISTS

- * 1) PRICES ARE F.C.A. ENERGY SHOPS, TULSA, OK.
- * 2) SHIPPING TERMS ARE PREPAY AND CHARGE.
- * 3) PRICE ARE VALID FOR TWELVE (12) MONTHS.
- * 4) UNIT PRICES ARE PER SET OF SPARE GASKETS.

**** 1) ENERGY EXCHANGER COMPANY RECOMMENDS ONE SET OF SPARE GASKETS PER EXCHANGER PER YEAR OF OPERATION.**

Energy Exchanger Company



Installation, Operation and Maintenance Manual for **SHELL AND TUBE HEAT EXCHANGERS**

A Member of the
Tubular Exchanger
Manufacturers Association



Energy Industrial Park/1844 North Garnett/Tulsa, Oklahoma 74116-1698
918 437-3000 / FAX 918 437-7144

INSTALLATION, OPERATION & MAINTENANCE MANUAL — Shell & Tube Heat Exchangers

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MM187157

FOREWORD

Included in this manual are Tables and Figures which are reprinted in their entirety from the Standards of the Tubular Exchanger Manufacturers Association Seventh Edition (1988). Pages containing such material contain a citation to that publication.

Additionally, there are extensive extracts of text reprinted from the 7th Edition TEMA Standards. Pages containing such excerpts contain a footnote to that effect.

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GENERAL INSTRUCTIONS FOR INSTALLATION, OPERATION AND MAINTENANCE OF SHELL AND TUBE HEAT EXCHANGERS

SAFETY CONSIDERATIONS

LIFTING DEVICES

When eyebolts, lugs, clips or other devices are installed by the manufacturer, it is intended that these lifting devices are to lift only the empty components to which they are attached and not the assembled heat exchanger, unless explicitly specified otherwise.

Proper rigging must be used in lifting assembled heat exchangers. Exchangers are usually much heavier than pressure vessels of comparable dimensions; therefore, weights should be carefully evaluated. Where available, determinations should include reference to manufacturers drawings, added components, bill of lading, etc. Special care must be exercised in handling exchangers with expansion joints.

ROUTINE PRECAUTIONARY PROCEDURES

A heat exchanger is a multi-chamber pressure vessel designed at specific limits of pressure, temperature and fluid flow conditions as shown on the exchanger specification sheet and heat exchanger nameplate(s). The process system, which includes the heat exchanger, must be safeguarded so that the heat exchanger design conditions and operating limits are not exceeded. All operating and maintenance personnel should be made aware of specific limitations including pressures and temperatures, flow rates, start-up/shut-down procedures and cleaning procedures.

Do not remove channel covers, shell covers, floating head covers, bonnets or connecting piping until all pressure has been relieved and both shell and tube sides are completely drained. Exceptions are permissible when design permits independent pressure testing of shell or tube sides.

Plugged tubes and double tubesheets, unless vented, may remain pressurized after shell and tube sides are depressurized. Caution may be exercised in loosening of tube plugs or opening of vents to avoid sudden release of pressure or harmful fluids.

Many heat exchangers circulate fluids which are toxic, lethal or flammable and dangerous to the human system. These fluids could cause problems if bolted or threaded joints are not maintained in leak-tight condition under operating or no-flow ambient conditions. Proper precautions, such as effective draining and purging, must be taken in handling and decontamination when exchangers are opened for any reason. It is essential that the user advise maintenance or repair personnel, including outside contractors, when toxic, lethal, or flammable conditions exist.

When heat exchangers are cleaned, it is important that full characteristics of the circulating fluids, fouling material, and the cleaning agent be known and care exercised in handling them. Use eye protection, a respirator, or other appropriate protective devices.

Do not blow out heat exchangers with air when the process fluids or the cleaning fluids being handled are flammable or reactive.

SECTION 1 HEAT EXCHANGER NOMENCLATURE

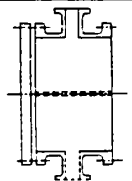
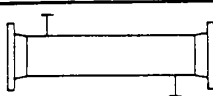
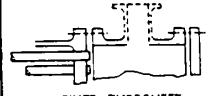
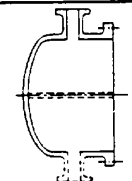
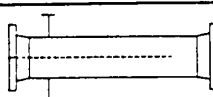
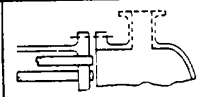
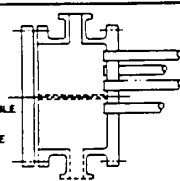
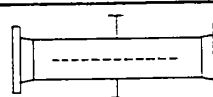
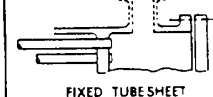
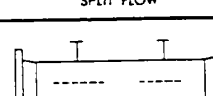
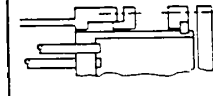
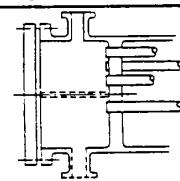
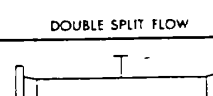
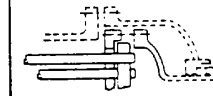
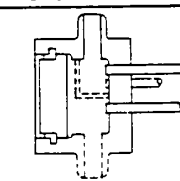
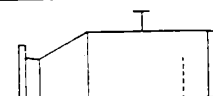
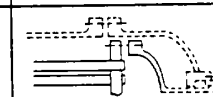
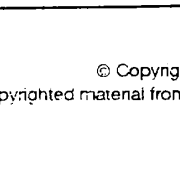
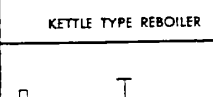
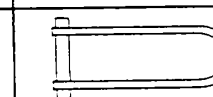
N-1 TYPE DESIGNATION-RECOMMENDED PRACTICE

It is recommended that heat exchanger type be designated by letters as described below.

N-1.1 TYPE

Type designation shall be by letters describing stationary head, shell (omitted for bundles only), and rear head, in that order, as indicated in Figure N-1.1.

Figure N-1.1

FRONT END STATIONARY HEAD TYPES		SHELL TYPES		REAR END HEAD TYPES	
A		E		L	
	CHANNEL AND REMOVABLE COVER		ONE PASS SHELL		FIXED TUBESHEET LIKE "A" STATIONARY HEAD
					
	BONNET (INTEGRAL COVER)		TWO PASS SHELL WITH LONGITUDINAL BAFFLE		FIXED TUBESHEET LIKE "B" STATIONARY HEAD
					
B	REMOVABLE TUBE BUNDLE ONLY	H		P	
	CHANNEL INTEGRAL WITH TUBE- SHEET AND REMOVABLE COVER		DOUBLE SPLIT FLOW		OUTSIDE PACKED FLOATING HEAD
					
	CHANNEL INTEGRAL WITH TUBE- SHEET AND REMOVABLE COVER		DIVIDED FLOW		FLOATING HEAD WITH BACKING DEVICE
					
C	SPECIAL HIGH PRESSURE CLOSURE		KETTLE TYPE REBOILER		PULL THROUGH FLOATING HEAD
		X		U	
			CROSS FLOW		U-TUBE BUNDLE
					
					EXTERNALLY SEALED FLOATING TUBESHEET

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SECTION 1 HEAT EXCHANGER NOMENCLATURE

N-2 NOMENCLATURE OF HEAT EXCHANGER COMPONENTS

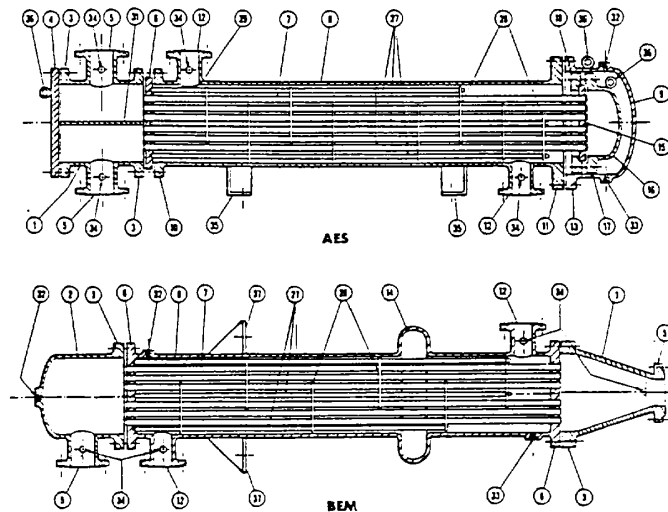
For the purpose of establishing standard terminology, Figure N-2 illustrates various types of heat exchangers. Typical parts and connections, for illustrative purposes only, are numbered for identification in Table N-2. (See Note)

Table N-2

1. Stationary Head — Channel	20. Slip-on Backing Flange
2. Stationary Head — Bonnet	21. Floating Head Cover — External
3. Stationary Head Flange — Channel or Bonnet	22. Floating Tubesheet Skirt
4. Channel Cover	23. Packing Box
5. Stationary Head Nozzle	24. Packing
6. Stationary Tubesheet	25. Packing Gland
7. Tubes	26. Lantern Ring
8. Shell	27. Tierods and Spacers
9. Shell Cover	28. Transverse Baffles or Support Plates
10. Shell Flange — Stationary Head End	29. Impingement Plate
11. Shell Flange — Rear Head End	30. Longitudinal Baffle
12. Shell Nozzle	31. Pass Partition
13. Shell Cover Flange	32. Vent Connection
14. Expansion Joint	33. Drain Connection
15. Floating Tubesheet	34. Instrument Connection
16. Floating Head Cover	35. Support Saddle
17. Floating Head Flange	36. Lifting Lug
18. Floating Head Backing Device	37. Support Bracket
19. Split Shear Ring	38. Weir
	39. Liquid Level Connection

NOTE: Manufacturers may identify corresponding parts using numbers differing from the above.

Figure N-2

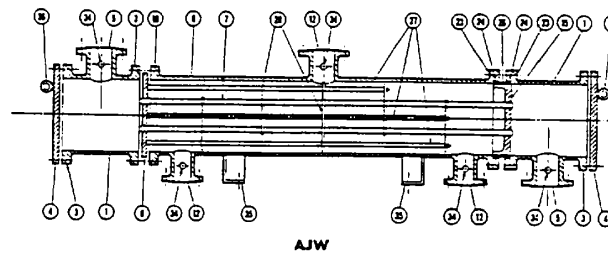
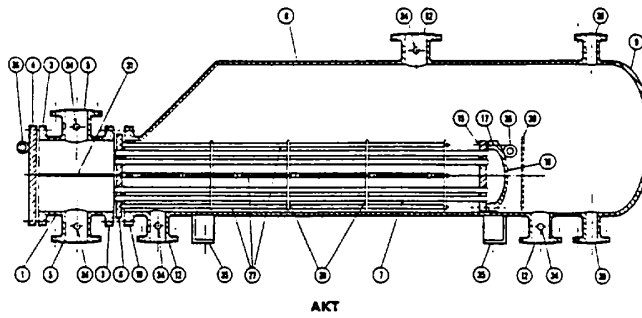
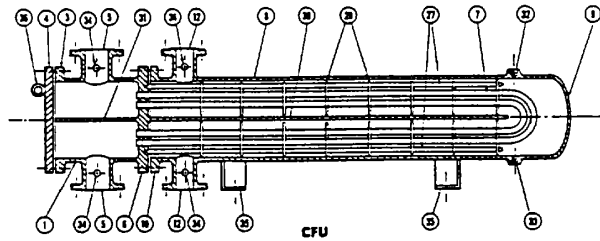
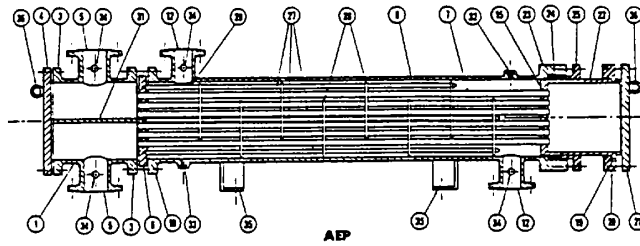


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SECTION 1

HEAT EXCHANGER NOMENCLATURE

Figure N-2 (Continued)



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SECTION 2

HEAT EXCHANGER IDENTIFICATION AND DEFINITIONS

D-2.1 EXCHANGER IDENTIFICATION

D-2.11 COMPLETE EXCHANGER

Manufacturers normally assign a serial number which is unique and permanently identifies each exchanger. Inquiries to the manufacturer should reference this number when it is shown on the nameplate and manufacturer's drawings. Additional useful information normally shown includes size, type, and item number.

D-2.12 EXCHANGER PARTS

Exchanger parts should be identified by the exchanger serial number and by the name and part number corresponding to those shown in Section 1, Table N-2, or as shown on the manufacturer's drawings.

D-2.2 DEFINITIONS

D-2.21 EXCHANGER UNIT

One or more exchangers designed for a specific service.

D-2.22 ITEM NUMBER

The purchaser's identification number for an exchanger unit.

D-2.23 NORMAL OPERATING CONDITIONS

The thermal and hydraulic performance requirements generally specified for designing the heat exchanger.

D-2.24 UPSET CONDITIONS

A departure from specified operating conditions.

D-2.25 PULSATING FLUID CONDITIONS

Conditions of flow generally characterized by rapid fluctuations in pressure and flow rate resulting from sources outside of the heat exchanger such as: pumps, compressors, blowers, etc.

D-2.26 START-UP CONDITIONS

The conditions of operation which exist from the time that flow of either or both process streams is initiated to the time that steady-state operating conditions are achieved.

D-2.27 SHUT-DOWN CONDITIONS

The conditions of operation which exist from the time of steady-state operating conditions to the time that flow of both process streams has ceased.

D-2.28 CODE

All references to Code herein mean the ASME Boiler and Pressure Vessel Code, Section VIII, Division 1, Pressure Vessels.

SECTION 3

INSTALLATION OF HEAT EXCHANGERS

E-3 INSTALLATION

E-3.1 INSTALLATION PLANNING

E-3.11 CLEARANCE FOR DISMANTLING

For straight tube exchangers fitted with removable bundles, provide sufficient clearance at the stationary head end to permit removal of the bundle from the shell and provide adequate space beyond the rear head end to permit removal of the shell cover and/or floating head cover.

For fixed tubesheet exchangers, provide sufficient clearance at one end to permit withdrawal and replacement of the tubes and enough space beyond the head at the opposite end to permit removal of the bonnet or channel cover.

For U-tube heat exchangers, provide sufficient clearance at the stationary head end to permit withdrawal of the tube bundle, or at the opposite end to permit removal of the shell.

E-3.12 FOUNDATIONS

Foundations must be adequate so that exchangers will not settle and impose excessive strains on the exchanger. Foundation bolts should be set to allow for setting inaccuracies. In concrete footings, pipe sleeves at least one size larger than bolt diameter slipped over the bolt and cast in place are best for this purpose, as they allow the bolt center to be adjusted after the foundation has set.

E-3.13 PIPING

E-3.131 THERMAL EXPANSION

It is essential that adequate provisions be made in the connecting piping to allow for thermal expansion without imposing unspecified piping loads on the exchanger. This is particularly important for single pass internal floating head designs, outside packed floating heads, and fixed tubesheet types with shell expansion joints. Unless precautions are taken, leakage or damage may result.

E-3.132 PULSATION AND VIBRATION

In all installations, care must be taken to eliminate or minimize transmission of fluid pulsations and mechanical vibrations to the heat exchangers.

E-3.14 CLEANING

Convenient means should be provided for cleaning the unit as suggested under "Maintenance." (Section 5)

E-3.15 LEVELING

Exchangers must be installed so that pipe connections are made without forcing, disassembling or loosening of flanged assemblies.

E-3.16 STACKED HEAT EXCHANGERS

The manufacturer normally stacks exchangers prior to completion of fabrication to insure proper alignment of interconnecting nozzles. Shims separating the intermediate shell supports are normally used. Therefore, it is important that shims, if used, match the thicknesses and locations used by the manufacturer.

E-3.17 CONNECTION PROTECTORS

Remove shipping covers and plugs immediately prior to installation. Before connecting to piping, inspect all openings in the heat exchanger for foreign material. The entire system should be clean and free of foreign objects before starting operation. Do not expose heat exchanger internals to moisture or harmful contaminants.

E-3.18 PIPE CONNECTIONS

Pipe connections must be in accordance with the manufacturer's dimensional outline drawing.

E-3.19 FOUNDATION BOLTS

Foundation bolts should be loosened at one end of unit to allow free expansion of shells. Slotted holes in supports are provided for this purpose.

- E-3.20 If the heat exchanger is equipped with a bellows type expansion joint, the expansion joint must be adequately protected during shipping and setting. Shipping supports must be removed in accordance with instructions.

E-3.3 HEAT EXCHANGER STORAGE

Heat exchangers normally are not protected for storage. If storage is necessary, a covered location at uniform temperature is preferable and provisions must be made to protect the heat exchanger interior from moisture, freezing, or harmful contaminants.

SECTION 4

OPERATION OF HEAT EXCHANGERS

E-4. OPERATION

E-4.1 PERFORMANCE OF HEAT EXCHANGERS

Satisfactory performance and service life can be expected only from heat exchangers which are properly installed, operated in accordance with design conditions, and receive preventive maintenance and cleaning on an appropriate schedule. These requirements are the responsibility of the user.

E-4.11 PERFORMANCE FAILURES

The failure of heat exchanger equipment to perform satisfactorily may be caused by one or more factors, such as:

- (1) Excessive fouling.
- (2) Air or gas binding resulting from improper piping installation or lack of suitable vents.
- (3) Operating conditions differing from design conditions.
- (4) Maldistribution of flow in the unit.
- (5) Excessive clearances between the baffles and shell and/or tubes, due to corrosion.
- (6) Improper thermal design.
- (7) Flooding resulting from inadequate drainage of condensate.

E-4.2 OPERATION OF HEAT EXCHANGERS

E-4.21 OPERATING PROCEDURES — NORMAL

Before placing any exchanger in operation, reference should be made to the exchanger drawings, specification sheet(s), and name plate(s) for any special instructions. Local safety and health regulations must be considered. Improper start-up or shut-down sequences, particularly of fixed tubesheet units, may cause leaking of tube-to-tubesheet and/or bolted flanged joints.

E-4.22 START-UP OPERATION

Most exchangers with removable tube bundles may be placed in service by first establishing circulation of the cold medium, followed by the gradual introduction of the hot medium. During start-up all vent valves should be opened and left open until all passages have been purged of air and are completely filled with fluid. For fixed tubesheet exchangers, fluids must be introduced in a manner to minimize differential expansion between the shell and tubes. (Refer E-4.24)

E-4.23 SHUT-DOWN OPERATION

For exchangers with removable bundles, the units may be shut down by first gradually stopping the flow of the hot medium and then stopping the flow of the cold medium. If it is necessary to stop the flow of cold medium, the circulation of hot medium through the exchanger should also be stopped. For fixed tubesheet exchangers the unit must be shut down in a manner to minimize differential expansion between shell and tubes, (Refer E-4.24). When shutting down the system, all units should be drained completely when there is the possibility of freezing or corrosion damage. To guard against water hammer, condensate should be drained from steam heaters and similar apparatus during start-up or shut-down. To reduce water retention after drainage, the tube side of water cooled exchangers should be blown out with air.

E-4.24 START-UP AND SHUT-DOWN PROCEDURES FOR FIXED TUBESHEET EXCHANGERS

When start-up and shut-down instructions are furnished, they must be followed. When specific instructions are not supplied, the recommended procedure is to start, or stop, the circulation of both shell and tube side fluids gradually and at the same time.

E-4.3 OPERATING LIMITATIONS

E-4.31 NORMAL OPERATING CONDITIONS

Equipment must not be operated at conditions more severe than those specified on the heat exchanger specification sheet, and/or name plates. A change in service or deviation from the specified operating conditions may require that a mechanical design check be made in order to avoid possible damage to the heat exchanger.

E-4.32 SUPPLEMENTAL NAME PLATE DATA

The manufacturer may supply supplemental data where it is pertinent to the operation or testing of the exchanger. This may include information pertaining to differential design and test pressure conditions, restrictions on operating conditions for fixed tubesheet type exchangers, or other restrictive conditions applicable to the design and/or operation of the unit or its components. Such information may be noted on the standard name plate or on a supplemental plate attached to the exchanger at the name plate location.

E-4.33 FLOW RATE

Heat exchangers are not to be operated at flow rates greater than those shown on the heat exchanger specification sheet. Excessive flow rates can cause vibration and/or erosion and severely damage the heat exchanger.

E-4.34 HYDRAULIC HAMMER

Exchangers should not be subjected to pulsating, slugging, or unstable flow conditions which may impair performance or result in destructive hydraulic hammer. Adequate condensate drainage is essential for steam heaters and similar apparatus.

E-4.35 TEMPERATURE SHOCKS

Exchangers normally should not be subjected to abrupt temperature fluctuations. Hot fluid must not be suddenly introduced when the unit is cold, nor cold fluid when the unit is hot.

E-4.36 FLUID TEMPERATURE LIMITS

E-4.361 Heat exchangers are not to be operated at fluid temperatures more severe than those shown on the heat exchanger specification sheet.

E-4.362 For fixed tubesheet exchangers fluid inlet temperatures may be severely limited when there is no fluid on the opposite side. Operation with fluid circulation on one side only should be avoided, unless specifically provided for in the design of the heat exchanger.

E-4.4 BOLTED JOINTS

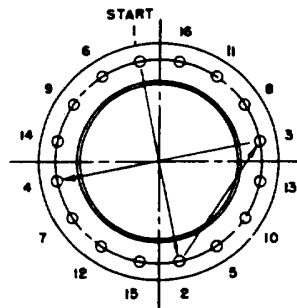
E-4.41 RECOMMENDATIONS FOR RETIGHTENING

Heat exchangers are pressure tested before leaving the manufacturer's shop in accordance with ASME Code requirements. However, normal yielding of gasket joints may occur in the interval between testing in the manufacturer's shop and installation at the job site. Therefore, all external bolted joints may require retightening after installation and, if necessary, after the exchanger has reached operating temperature.

E-4.42 RECOMMENDED BOLT TIGHTENING PROCEDURE

It is important that all bolted joints be tightened uniformly and in a diametrically staggered pattern as illustrated in Figure E-4.42 except for special high pressure closures when the instructions of the manufacturer should be followed.

Figure E-4.42



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SECTION 5

MAINTENANCE OF HEAT EXCHANGERS

E-5. MAINTENANCE

E-5.1 INSPECTION OF UNIT

At regular intervals and as frequently as experience indicates, an examination should be made of the interior and exterior condition of the unit. Neglect in keeping all tubes clean may result in complete stoppage of flow through some tubes which could cause severe thermal strains, leaking tube joints, or structural damage to other components. Sacrificial anodes, when provided, should be inspected to determine whether they should be cleaned or replaced.

E-5.11 INDICATIONS OF FOULING

Exchangers subject to fouling or scaling should be cleaned periodically. A light sludge or scale coating on the tube greatly reduces its efficiency. A marked increase in pressure drop and/or reduction in performance usually indicates cleaning is necessary. The unit should first be checked for air or vapor binding to confirm that this is not the cause for the reduction in performance. Since the difficulty of cleaning increases rapidly as the scale thickness or deposit increases, the intervals between cleanings should not be excessive.

E-5.12 PREVENTIVE MAINTENANCE

Additional important reasons for inspections include:

- (1) Corrosion and erosion may weaken various parts of an exchanger and may eventually cause mechanical failure, or impaired performance.
- (2) Determination of fouling and corrosion rates for prediction of service life and scheduling down-time.
- (3) Implementation of preventive maintenance procedures which reduce rates of fouling and general deterioration, or eliminate leaks.

E-5.13 ACCESS TO TUBES

Before disassembly, the user must assure himself that the unit has been depressurized, vented and drained, neutralized and/or purged of hazardous materials.

To inspect the inside of the tubes and also make them accessible for cleaning, the following procedures should be used:

- (1) Stationary Head End
 - (a) Type A, C, & D, remove cover only.
 - (b) Type B, remove bonnet.
- (2) Rear Head End
 - (a) Type L, N, & P, remove cover only.
 - (b) Type M, remove bonnet.
 - (c) Type S & T, remove shell cover and floating head cover.
 - (d) Type W, remove channel cover or bonnet.

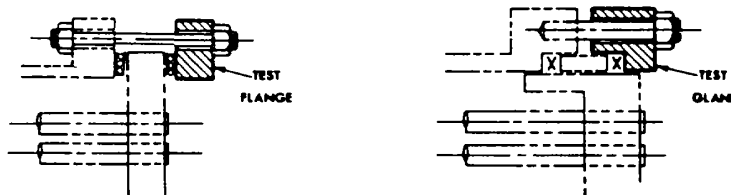
E-5.14 LOCATING LEAKS IN TUBES

The following procedures may be used to locate perforated or split tubes and leaking joints between tubes and tubesheets. In most cases, the entire front face of each tubesheet will be accessible for inspection. The point where water escapes indicates a defective tube or tube-to-tubesheet joint.

- (1) Units with removable channel cover:
Remove channel cover and apply hydraulic pressure in the shell.
- (2) Units with bonnet type head:
 - (a) On fixed tubesheet units where tubesheets are an integral part of the shell, remove bonnet and apply hydraulic pressure in the shell.
 - (b) On fixed tubesheet units where tubesheets are not an integral part of the shell and on units with removable bundles, remove bonnet, re-bolt tubesheet to shell or install test flange or gland, whichever is applicable, and apply hydraulic pressure in the shell.
See Figure E-5.14-1 for typical test flange and test gland.

CAUTION: Bolting directly to the edges of the tubesheets may result in overstress unless it was considered in the design of the tubesheets.

Figure E-5.14-1

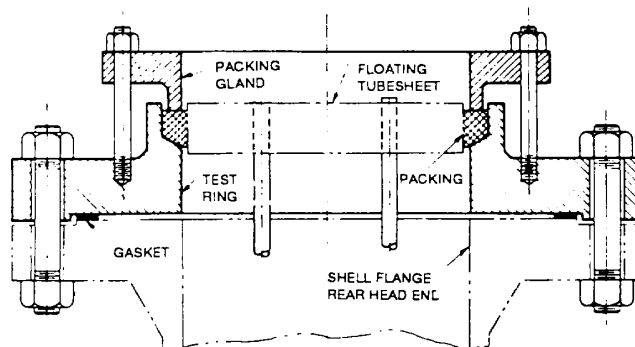


- (3) Units with type S or T floating head:
Remove channel cover or bonnet, shell cover and floating head cover. Install test ring and bolt in place with gasket and packing. Apply hydraulic pressure in the shell. A typical test ring is shown in Figure E-5.14-2. When a test ring is not available it is possible to locate leaks in the floating head end by removing the shell cover and applying hydraulic pressure in the tubes. Leaking tube joints may then be located by sighting through the tube lanes.

NOTE: Care must be exercised when testing partially assembled exchangers to prevent over extension of expansion joints or overloading of tubes and/or tube-to-tubesheet joints.

Hydrostatic test should be performed so that the temperature of the metal is at least 30°F above the minimum design metal temperature, MDMT.

Figure E-5.14-2



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E-5.2 TUBE BUNDLE REMOVAL

Bundles must be withdrawn from the stationary end as noted on the drawing. All parts such as glands, retainer rings, split shear rings and closure packing must be removed before attempting to remove bundle. Threaded eyebolts may be attached to the stationary tubesheet when tapped holes have been provided for this purpose. When eyebolt tappings are not provided, rods may be passed through two or more tubes and attached to a steel bearing plate over the floating tubesheet. Provide a protective spacer between the bearing plate and tubesheet to protect the tube ends.

E-5.21 HANDLING TUBE BUNDLES

Tube bundles should not be handled with hooks or other devices which might damage the tubes. Bundles should be supported on cradles or skids. Horizontal tube bundles should be lifted by means of suitable slings. Baffles can be bent and damaged by dragging a bundle over a rough surface. All gasket and packing contact surfaces should be protected from accidental damage since these areas are generally difficult to repair.

E-5.3 CLEANING TUBE BUNDLES

E-5.31 CLEANING METHODS

The heat transfer surfaces of heat exchangers should be kept reasonably clean to assure satisfactory performance. Convenient means for cleaning should be made available.

Heat exchangers may be cleaned by either chemical or mechanical methods. The method selected must be the choice of the operator of the plant and will depend on the type of deposit and the facilities available in the plant. Following are several cleaning procedures that may be considered:

- (1) Circulating hot wash oil or light distillate through tubes or shell at high velocity may effectively remove sludge or similar soft deposits.
- (2) Some salt deposits may be washed out by circulating hot fresh water.
- (3) Commercial cleaning compounds are available for removing sludge or scale provided hot wash oil or water is not available or does not give satisfactory results.
- (4) High pressure water jet cleaning.
- (5) Scrapers, rotating wire brushes, and other mechanical means for removing hard scale, coke, or other deposits.
- (6) Employ services of a qualified organization that provides cleaning services. These organizations will check the nature of the deposits to be removed, furnish proper solvents and/or acid solutions containing inhibitors, and provide equipment and personnel for a complete cleaning job.

E-5.32 CLEANING PRECAUTIONS

- (1) Tubes should not be cleaned by blowing steam through individual tubes since this heats the tube and may result in severe expansion strain, deformation of the tube, or loosening of the tube-to-tube sheet joint.
- (2) When mechanically cleaning a tube bundle, care should be exercised to avoid damaging the tubes.
- (3) Cleaning compounds must be compatible with the metallurgy of the exchanger.
- (4) Cleaning procedures, especially those which circulate hot fluids through the tubes, can cause significant temperature differentials between the shell and tubes. Such cleaning procedures can cause damage to fixed tubesheet heat exchangers and should be avoided unless specifically provided for in the design of the heat exchanger.

E-5.4 GASKET REPLACEMENT

Gasket and gasket surfaces should be thoroughly cleaned and should be free of scratches and other defects. Gaskets should be properly positioned before attempting to retighten bolts. It is recommended that when a heat exchanger is dismantled for any cause, it be reassembled with new gaskets. This will tend to prevent future leaks and/or damage to the gasket seating surfaces of the heat exchanger. Composition gaskets become dried out and brittle so that they do not always provide an effective seal when reused. Metal or metal jacketed gaskets, when compressed initially, flow to match their contact surfaces. In so doing they are work hardened and, if reused, may provide an imperfect seal or result in deformation and damage to the gasket contact surfaces of the exchanger.

Bolted joints and flanges are designed for use with the particular type of gasket specified. Substitution of a gasket of different construction or improper dimensions may result in leakage and damage to gasket surfaces. Therefore, any gasket substitutions should be of compatible design.

Any leakage at a gasketed joint should be rectified and not permitted to persist as it may result in damage to the gasket surfaces.

When metal jacketed filled type gaskets are used with a tongue and groove joint without a nubbin, the gasket should be installed so that the tongue bears on the seamless side of the gasket jacket. When a nubbin is used, the nubbin should bear on the seamless side.

E-5.5 SPARE AND REPLACEMENT PARTS

The procurement of spare or replacement parts from the manufacturer will be facilitated if the correct name for the part, as shown in Section 1, Table N-2, of this manual is given, together with the serial number, type, size, and other information from the nameplate. Replacement parts should be purchased from the original manufacturer.

E-5.6 EXPANDED TUBE JOINTS

E-5.6.1 TUBE HOLE FINISH

Tube hole finish affects the mechanical strength and leak tightness of an expanded tube-to-tubesheet joint. In general:

- (1) A rough tube hole provides more mechanical strength than a smooth tube hole. This is influenced by a complex relationship of modulus of elasticity, yield strength, and hardness of the materials being used.
- (2) A smooth tube hole does not provide the mechanical strength that a rough tube hole does, but it can provide a pressure tight joint at a lower level of tube wall reduction.
- (3) Very light wall tubes require a smoother tube hole finish than heavier wall tubes.
- (4) Significant longitudinal scratches can provide leak paths through an expanded tube-to-tubesheet joint and should therefore be removed.

E-5.6.2 TUBE WALL REDUCTION

The optimum tube wall reduction for an expanded tube-to-tubesheet joint depends on a number of factors, some of which are:

- (1) Tube hole finish.
- (2) The presence or absence of the tube hole serrations (grooves).
- (3) The tube hole size and tolerance.
- (4) Tubesheet ligament width and its relation to tube diameter and thickness.

- (5) Tube wall thickness.
- (6) Tube hardness and change in hardness during cold working.
- (7) Tube O.D. tolerance.
- (8) Type of expander used.
- (9) Type of torque control or final tube thickness control.
- (10) Function of tube joint, i.e., strength in resistance to pulling out, minimum cold work for corrosion purposes, freedom from leaks, ease of replacement, etc.
- (11) Length of expanded joint.
- (12) Compatibility of tube and tubesheet materials.

E-5.63 TUBE EXPANDING

A suitable tube expander should be used to tighten a leaking tube joint. Care should be taken to insure that tubes are not over expanded. Do not re-expand tubes which are not leaking. Do not expand tubes beyond 1/8" from the back face of the tubesheet.

E-5.64 TYPICAL COMPUTATION OF TUBE WALL REDUCTION

EXAMPLE OF DETERMINING THE EXPANDED TUBE INSIDE DIAMETER FOR A SPECIFIED AMOUNT OF WALL REDUCTION

GIVEN: TUBE DIAMETER = 0.750
 TUBE HOLE DIAMETER = 0.760
 TUBE WALL THICKNESS = 0.065
 SPECIFIED WALL REDUCTION = 5%

SOLUTION: WALL REDUCTION = $0.065 \times 0.05 = 0.00325$
 FINAL WALL THICKNESS = $0.065 - 0.00325 = 0.06175$
 FINAL EXPANDED TUBE I.D. = $0.760 - 2(0.06175) = 0.6365$

CAUTION: *THE USE OF NOMINAL DIMENSIONS, WITHOUT ATTENTION TO PERMISSIBLE TOLERANCES CAN LEAD TO INCORRECT CONCLUSIONS.*

*EXPANDING PROCEDURES SHOULD BE BASED ON MEASURED DIMENSIONS,
NOT NOMINAL DIMENSIONS.*

E-5.65 PLUGGING TUBES IN TUBE BUNDLES

In U-tube heat exchangers, and other exchangers of special design, it may not be feasible to remove and replace defective tubes. Defective tubes may be plugged using commercially available tapered plugs with ferrules or tapered only plugs which may or may not be seal welded. Excessive tube plugging may result in reduced thermal performance, higher pressure drop, and/or mechanical damage.

E-5.7 WELDED TUBE JOINTS

Welding procedure and testing techniques for either seal welded or strength welded tube joints normally are by agreement between manufacturer and purchaser and therefore should be considered prior to repairs to welded tube joints or tube replacements.

E-5.8 END FLANGES AND BOLTING

The purpose of this section is to alert the users, and provide basic data for consideration in assembly and maintenance of bolted flanged joints. Controlling the torque applied in tightening threaded bolts is the most economical and commonly used method for the control of initial tension. There are several factors which affect the relationship between torque and tension of threaded bolts. A few of the factors are the type of lubricant and/or plating, if any, used on the threads and the materials from which the bolt and nut are manufactured.

In assembling gasketed joints it is essential that the gasket first be seated uniformly by initial tightening of studs using a staggered quarterly pattern. After the gasket is seated, torquing may be completed stepwise to the final desired value, following a staggered or sequential pattern.

The following may be used as references and aids when assembling bolted flanged joints:

1. Recommended assembly and maintenance of flanged joints as shown in the Crane Company Catalog #60, Engineering Data Section.
2. Torque Control, Sixth Edition, Sturtevant Company.
3. ASME Code, Appendix S.

E-5.9 SPECIAL HIGH PRESSURE CLOSURES

The instructions of the heat exchanger manufacturer should be followed when provided.

E-5.10 REPAIRS, ALTERATION, RERATING, AND REPLACEMENT PARTS.

In order to maintain the Code integrity of the vessel, any repairs by welding, subsequent heat treating, alterations, replacement pressure parts, or rerating must be done in accordance with the National Board Inspection Code.

Potentially toxic or harmful contaminants must be neutralized prior to repairs.

Following repair by welding, post weld heat treatment may be a requirement for preservation of resistance to corrosion.